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Photoinduced Electron Transfer from Organic Semiconductors onto Redox Mediators for CO_2 Reduction

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Abstract

In this work the photoinduced electron transfer from organic semiconductors onto redox mediator catalysts for CO_2 reduction has been investigated. In the beginning, the work focuses on the identification, characterization and test of suitable catalyst materials. For this purpose, rhenium compounds with 2,2'-bipyridine bis(arylimino) acenaphthene ligands and pyridinium were tested for molecular homogenous catalysis.

Infrared, ultraviolet-visible (UV-Vis) and nuclear magnetic resonance (NMR) spectroscopy were used for initial characterization of the catalyst substances. Since the interpretation of infrared spectra was difficult for large molecules based on measured data only, additionally infrared absorption spectra obtained by quantum mechanical density functional theory (DFT) calculations were successfully used to correlate characteristic features in the measured spectra to their molecular origin. It was found that experimentally observed data and quantum chemical predictions for the infrared spectra of the novel compounds are in good agreement. Additionally, quantum mechanical calculations were carried out for the determination of molecular orbital frontier energy levels and correlated to UV-Vis absorption and cyclic voltammetry measurements.

Extensive cyclic voltammetry measurements and bulk controlled-potential electrolysis experiments were performed using a N₂- and CO₂-saturated electrolyte solution. Together with a detailed product analysis via infrared spectroscopy, gas and ion chromatography the results allowed electrochemical characterizations of the novel catalysts regarding their suitability for electrochemical CO₂ reduction.

Once suitable catalysts were identified, the materials were immobilized on the electrode surface by electro-polymerization of the catalyst (5,5'-bisphenylethynyl-2,2'-bipyridyl)Re(CO)₃Cl itself or by incorporation of (2,2'-bipyridyl)Re(CO)₃Cl into a polypyrrole matrix, thereby changing from homogeneous to heterogeneous catalysis. In an entirely new approach the catalyst (2,2'-bipyridyl)Re(CO)₃Cl was covalently attached to poly(3-hexylthiophene).

Finally, the combination of suitable catalysts with organic semiconductor materials was investigated for photoinduced energy and charge transfer from the donor semiconductor polymer to the catalyst acceptor. Poly(N-vinylcarbazole) (PVK) was used as absorber material acting as efficient redox photosensitizer in combination with $(2,2'-bipyridyl)Re(CO)_3Cl$ as catalyst acceptor.

Photoluminescence quenching experiments in solid film mixtures and in a solid-liquid interface between polymer and catalyst revealed strong luminescence quenching by the catalyst material due to a resonant energy transfer.

This work shows, that the combination of organic semiconductors with catalyst redox mediators offers a promising approach for electro- and photocatalytic CO_2 reduction.

Kurzfassung

Die vorliegende Arbeit beschäftigt sich mit dem photoinduzierten Ladungstransfer zwischen organischen Halbleitern und Katalysator-Redox-Mediatoren mit dem Ziel der chemischen Reduktion von CO_2 . Geeignete Katalysator-Moleküle konnten identifiziert und charakterisiert werden. Anhand vielversprechender Ergebnisse wurden Rhenium enthaltende Übergansmetallkomplexe mit 2,2'-bipyridin und bis(arylimino) acenaphten Liganden genauer auf deren Eigenschaften zur homogenen Katalyse getestet.

Für die anfängliche Charakterisierung der Katalysatoren wurden Infrarot-, UV-Vis- und Kern-Resonanz- (NMR)-Spektroskopie Messungen durchgeführt. Weiters wurden Infrarotabsorptionsspektren anhand quantenmechanischer Berechnungen mittels Dichte-Funktional-Theorie (DFT) erfolgreich berechnet und charakteristische Absorptionsbanden konnten den entsprechenden Molekülschwingungen zugeordnet werden. Die gemessenen und berechneten Spektren weisen eine gute Übereinstimmung auf.

Zusätzlich wurden quantenmechanische Berechnungen für die Bestimmung der jeweiligen Molekülorbitale verwendet und die Ergebnisse der Berechnungen mittels experimentellen UV-Vis- und Cyclovoltammetrie-Messungen verglichen. Intensive Cyclovoltammetrie- und Elektrolyseexperimente in N₂- und CO₂-gesättigten Elektrolytlösungen wurden in Zusammenhang mit einer detaillierten Analyse der Reduktionsprodukte durchgeführt. Hierfür wurden Infrarotspektroskopie, Gas- und Ionenchromatographie verwendet. Die neuen Katalysatoren konnten hinsichtlich deren potentiellen Verwendbarkeit zur CO₂ Reduktion somit detailliert charakterisiert werden.

Nachdem passende Katalysatoren gefunden worden waren, konnten diese auf der Elektrodenoberfläche durch Elektropolymerisation des Katalysators $(5,5'-bisphenylethynyl-2,2'-bipyridyl)Re(CO)_3Cl$ selbst oder durch Einbettung von $(2,2'-bipyridyl)Re(CO)_3Cl$ in eine Polypyrrol-Matrix immobilisiert werden. Dies ermöglichte den Übergang von einer homogenen zu einer heterogenen Katalyse. In einem komplett neuen Ansatz wurde der Katalysator $(2,2'-bipyridyl)Re(CO)_3Cl$ kovalent an Poly(3-Hexylthiophen) gebunden.

Abschließend wurde der photoinduzierte Energie- und Ladungstransfer durch Kombination eines Polymerhalbleiters als Donor und eines Katalysators als Akzeptor untersucht. Poly(Nvinylcarbazol) (PVK) als effektiver Photosensibilisator wurde in Kombination mit dem als Akzeptor fungierendem $(2,2'-bipyridyl)Re(CO)_3Cl$ getestet. Experimente zur Löschung der Photolumineszenz in Feststoffmischungen und in Fest-Flüssig-Grenzschichten zwischen Polymer und Katalysator zeigten eine starke Lumineszenz-Löschung aufgrund eines resonanten Energietransfers.

Zusammenfassend konnte in dieser Arbeit gezeigt werden, dass die Kombination von organischen Halbleitern mit Katalysator-Redox-Mediatoren eine aussichtsreiche Methode zur elektro- und photokatalytischen CO_2 -Reduktion darstellt.

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Chapter 1

Introduction

1.1 Energy and environment

The current energy supply of human society is mainly based on fossil fuels like coal, oil and gas which are related to several problems. The reserves are decreasing and their final depletion seems to be just a matter of time.[1] In addition, combustion of fossil fuels leads to the emission of CO_2 , which is considered as a main greenhouse gas.[2] Figure 1.1(a) and 1.1(b) show measurements of the atmospheric carbon dioxide concentration at Mauna Loa, Hawaii. The presented data reveals an increase from initially 300 parts per million (ppm) to more than 400 ppm current level over the last decades.[3] Figure 1.1(b) shows a detail monthly view of the data represented in Figure 1.1(a) where the annual fluctuations in CO_2 concentration according to the seasonal vegetation changes in the northern and southern hemispheres are apparent. The possible consequences of the man made greenhouse effect (increased temperatures) and the depletion of fossil fuels on oncoming generations depict that there is a need for environmentally friendly and sustainable energy systems.[4]

Several approaches have been made to replace fossil fuels by sustainable techniques like solar and wind energy, hydroelectric power, energy from biomass, etc. Up to now none of these were able to fully replace fossil fuels. From all available renewable energy resources, solar energy will be the only known source that provides sufficient energy to meet the increasing energy demand of humanity. The total solar energy absorbed by Earth's atmosphere, oceans and land masses is approximately 3,850,000 exajoules (EJ) per year. Even with photovoltaic technology available today only 1% of the area of global deserts would be sufficient to produce the entire annual human primary energy consumption as electric power.[5]

Renewable energy sources, like solar radiation, are most abundant in remote locations and have huge fluctuations over short (daily variations) and long timescales (seasonal changes). Therefore cost effective energy storage and transport is just as important as energy generation. This could in theory be achieved by the use of battery systems, but at



Figure 1.1: (a) Atmospheric carbon dioxide concentration measured at Mauna Loa, Hawaii over the last decades. (b) Detail monthly view of the data represented in Figure (a) showing the atmospheric carbon dioxide concentration and its seasonal fluctuations as measured at Mauna Loa, Hawaii for the last four years.[3]

present batteries are far too expensive and transport of electricity over long distances via cables involves significant losses.[6]

One of the most efficient ways to store energy regarding to energy density and transportability is, as nature has demonstrated over millions of years, chemical energy storage in hydrocarbons. The energy density of gasoline is around 46 MJ/kg (12.8 kWh/kg), which is significantly higher compared to modern batteries, like for example a Li-ion battery, with an energy density of around 540 kJ/kg (150 Wh/kg).[7] Therefore, direct and efficient conversion of solar energy to hydrocarbons would be a major breakthrough on the way towards a sustainable energy supply for humanity.



Figure 1.2: The schematic representation of energy as a vector in space and time.

Figure 1.2 illustrates the idea of energy as a vector in space and time, where both components have to be fulfilled to meet human demands now and in the future.

1.2 The end of cheap fossil fuels

The human demand for energy is growing steadily. This is anticipated to be even more pressing since the global population and economies are increasing rapidly too. Succeeding current trends it is predicable that the world energy demand is following. During the last 25 years alone, world energy consumption has increased by about 60 %.[8]

Oil is still the most important energy source for mankind. This becomes apparent if we take into account that each US citizen for example is consuming about 11 liter of oil per person per day.[9] Taking global oil consumption into account, experts expect an increase of about 50% by 2030. This will become progressively problematic since the easiest oil to extract has by now been produced and new reserves are difficult to find.[1] Humanity has tried to keep pace with increasing consumption, but the rapid increase in crude oil extraction by the modern industrialized society within the last century is anticipated to come to a maximum in the near future. This point at which global oil production will reach a final peak and then decline is well known in literature as "peak oil" and has been around for decades. Some scientists argue that this point in time has already passed and oil production will decline in the near future. Although statistics show that oil reserves are apparently increasing, the total percentage which is available for extraction is steadily decreasing. If the United States, as the biggest oil consumer in the world, are taken as an example, production as a percentage of reserves has declined from 9 % in 1980 to 6 % by 2012. On a global scale the production at existing oil fields is continuously declining at rates of about 4.5 % to 6.7 %per year. [10, 11, 12]

Taking this data into account leads to the conclusion that although humanity will not run out of oil soon, but of oil that can be produced easily and cheaply. Figure 1.3 shows the oil production from 1998 to 2011 and the corresponding Brent crude oil price in US dollar per barrel. It can be seen that the oil production followed the oil demand until 2005 and then leveled off although the oil price continued to increase.[10, 13]



Figure 1.3: Oil production from 1998 to 2011 and corresponding Brent crude oil price in US dollar per barrel. The oil production followed the oil demand until 2005 and then leveled off although the oil price continued to increase. (Graph reproduced from reference [10] and the data therein is taken from reference [13].)

Although the US Energy Information Administration optimistically planed with a 30 % increase in oil production between now and 2030, it is stated that all of that increase is in the form of unidentified projects. This unidentified projects is oil yet to be discovered.[13] Murray and King pointed out in their article of 2012,[10] that even if production at existing fields miraculously stopped declining, such an increase would require 22 million barrels per day of new oil production by 2030. Taking however current declines of 5 % per year into account they calculated that this would need a discovery and utilization of new fields yielding more than 64 million barrels per day. This amount is equivalent to todays total oil production. The authors further concluded that this is very unlikely to happen.

It is clear that the scarcity of oil will heavily affect the global economy, which is so closely tied to physical resources and a rapidly growing world economy will require large increases in energy supplies over the next few years. Following this argumentation it is interesting and important to notice that the approaches needed for tackling the economic impacts of resource scarcity and climate change described in the previous chapter are the same and obvious. Human society has to move away from the dependence on fossil-fuel energy sources. Learning a lesson from history it tells that the implications of climate change have driven only slow policy responses. On the other hand economic consequences tend to drive shorter-term action. It is known from past records that when there are oil price spikes, the economy begins to respond within a year or less.

A solution to this multiple problem space, whether it is climate or economy driven, can only be done by increasing efficiency of transportation, residential, commercial, and industrial uses and thereby decouple energy consumption and economic growth.[8] Furthermore global energy supply has to move away from fossil fuels like coal, oil and gas to renewable energy sources. To make this transition possible, the capture and utilization of carbon dioxide from earths atmosphere and its transformation to a carbon neutral energy carrier, is of utmost importance.

1.3 Carbon capture and utilization

Possible processes for carbon dioxide (CO₂) recycling were formerly described in the literature and include the capture of CO₂ from air, release of pure CO₂ and finally fuel synthesis.[14, 15] For fuel synthesis CO₂ has to be chemically reduced. This can be done either directly (electrochemically or photochemically) or in an indirect way using for example hydrogen gas as a reducing agent. In both methods a catalyst is usually needed. Whereas the indirect reduction with hydrogen is a well-known process, the direct reduction methods are still a topic of basic research and also the focus of this thesis.

 CO_2 reduction processes have already been implemented with good efficiencies through various strategies. Two interesting approaches were outlined by Stucki et. al [14] and Specht et. al. [15] Both attempts used metal hydroxide based solutions, either a calcium hydroxide (Ca(OH)₂) or a alkali hydroxide (NaOH, KOH) solution for CO₂ capturing in an absorption liquid and acidification methods for the CO_2 release. The pure CO_2 gas has then to be reduced with the aid of a reducing agent, here hydrogen gas, in a high temperature thermo-chemical reactor. The main disadvantages of this approach are the high energy and engineering intensive process steps. As proposed by Olah [16], another way to reduce (CO_2) would be the use of a regenerative electrochemical cell system based on the fuel cell concept. Such a regenerative fuel cell would be able to operate in two modes, namely forward and reverse. In forward mode, the fuel cell generates electricity by oxidizing hydrocarbon fuels such as methane or methanol. In reverse mode, the fuel cell produces these hydrocarbon fuels by the reduction of CO_2 . Although the fundamental principles of these two processes are known, no efficient selective reduction of CO_2 to higher hydrocarbons has been achieved by now. Furthermore this method will not answer the question where the electricity for fuel production should come from.

Methods for direct electrochemical activation of carbon dioxide have long been studied and significant progress has been made over the past decade.[17, 18, 19, 20] The electrochemical reduction of CO₂ usually requires a high potential of about -1.9 Vvs. NHE for a one electron activation process. This high potential is partly explained by the necessary large inner-shell rearrangements upon electron transfer and the corresponding bending of the molecule upon one electron activation resulting in an O-C-O angle of 133°.[21, 22] By performing the CO₂ reduction in a multi-electron process, however, this transformation can be facilitated. As a consequence of this multi-electron and proton transfer, the required reduction potentials are lowered significantly. This is reflected by the change in the equilibrium redox potentials between reaction 1.1 and 1.2 where the redox potential changes from -1.90 V to -0.65 V vs. NHE respectively.[23] Furthermore the equilibrium potential of the CO₂ reduction progressively shifts to more positive values as the number of electrons and protons participating in the reduction process increase, comparing different net reactions 1.3 to 1.8.

$$CO_2 + e^- \rightleftharpoons CO_2^{\bullet-}$$
 (1.1)

$$2CO_2 + 2e^- \rightleftharpoons CO + CO_3^{2-} \tag{1.2}$$

$$CO_2 + 2H^+ + 2e^- \rightleftharpoons HCOOH$$
 (1.3)

$$CO_2 + 2H^+ + 2e^- \rightleftharpoons CO + H_2O \tag{1.4}$$

$$CO_2 + 4H^+ + 4e^- \rightleftharpoons C + 2H_2O \tag{1.5}$$

$$CO_2 + 4H^+ + 4e^- \rightleftharpoons HCHO + H_2O \tag{1.6}$$

$$CO_2 + 6H^+ + 6e^- \rightleftharpoons CH_3OH + H_2O \tag{1.7}$$

$$CO_2 + 8H^+ + 8e^- \rightleftharpoons CH_4 + 2H_2O \tag{1.8}$$

Although the equilibrium reduction potentials for a proton coupled multi-electron CO_2 reduction appear to be tolerably low, in reality however, the actual reduction potentials on bare metal electrodes are much higher than the Nernst potential due to barrier induced over potentials. In order to decrease the actual redox potential needed for the CO_2 -reduction process, suitable catalysts are required.



Figure 1.4: The schematic proposal of mimicking photosynthesis by providing a photo induced electron transfer from an organic semiconductor onto a redox mediator catalyst for CO_2 reduction in an electrolyte containing system.

An interesting achievement in this direction was reported by Delacourt et. al.[24], who described syngas conversion into methanol using an electrochemical cell similar to PEM fuel cells. This group achieved 45 % energy efficiency at 10 mA cm⁻², but unfortunately the efficiency was decreasing with higher current densities (30 % at 100 mA cm⁻²). The homogeneous catalysis of carbon dioxide assimilating fuel generation based on water splitting represents another interesting approach in solar fuel research.[25, 26] These artificial photosynthetic systems are inspired by the overall function of the natural enzymatic reactions, where the industrially important role of hydrogen gas as a two-electron reductant for CO₂-fixation is replaced by organic redox cofactors such as NADH, acting as hydride transfer reagents. In all kinds of technical scenarios following this direction, this leads to the fundamental problem of catalytic cofactor regeneration, i. e. a reversible NAD⁺ to NADH conversion to supply electrons and protons for a multistep carbon dioxide conversion into energy rich compounds.[27, 28, 29]

At present most of the best studied catalysts are metal complexes with bipyridine ligands, where the catalyst center consists of transition metals based on rhenium (Re), rhodium (Rh) or ruthenium (Ru). Despite their high current efficiencies and high selectivity, problems in the field of artificial solar fuel production by these catalysts are manifold. Although these molecular catalyst compounds can be used to stabilize intermediate steps of the CO₂ reduction process and thus lower the required overpotential, achieving a simultaneous multiple electron and proton transfer as indicated by the described reactions 1.3 to 1.8 is kinetically extremely difficult to realize and over potentials of most reported catalyst systems are still significantly high. Furthermore, systems based on these catalyst materials, as reported up to now, suffer from low stability and low turnover frequency. In recent yeas Bocarsly et. al. [30] reported on the catalytic reduction of CO₂ to methonol by Pyridinium (the protonated form of Pyridine). Although this system demonstrates only a very low rate of reaction due to a complicated mechanism, which is not jet fully understood, the approach seems to very

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promising regarding earth abundant catalyst materials and proton rich products.

In the presented thesis the aim is to investigate a new approach for the reduction of carbon dioxide (CO_2) to various desirable products. The intention is to establish a system providing a photo induced electron transfer from an organic semiconductor onto a redox mediator for CO_2 reduction. This can be achieved by using an organic semiconducting material, as it is known today in the field of organic photovoltaic, in contact with an electrolyte solution that contains a catalyst, which is specific for a multi electron CO_2 reduction. Such a system would mimic photosynthesis which is demonstrated successfully by nature over million of years. In Figure 1.4 a schematic proposal for this process is shown.

Although several steps will be investigated and described in detail, which are necessary to achieve such a system, the main part of this thesis will focus on catalyst research for CO_2 reduction. Once the right materials are specified, spectroelectrochemical methods, such as in situ Fourier transform infrared spectroscopy (FTIR) and current density-voltage characteristics of the catalyst or polymer electrolyte interface, will be investigated to describe the physics behind this processes. At the end a brief outlook on future challenges with respect to CO_2 reduction is presented, together with possible suggestions how this problems could be addressed by the scientific community. In a more elaborate view on CO_2 reduction to date (compare chapter 9) current achievements in the field of direct CO_2 reduction are brought into context of energy supply and related costs.

1.4 Organic semiconductors for CO₂ reduction

A very promising approach in the last decade was the combination of catalysts with inorganic semiconductor materials. In a recent work Kubiak et. al. showed light-assisted co-generation of CO and H₂ from CO₂ and H₂O with a p-type silicon working electrode. The experiments were preformed in an acetonitrile/water mixture, exhibiting high Faradic efficiency at low homogeneous catalyst concentration.[18, 31] Bocarsly and coworkers [32] reported selective reduction of CO₂ to methanol by combining p-GaP semiconductor electrode and pyridine as catalyst material. This attempt of a kinetically difficult $6e^-$ aqueous photo reduction of CO₂ to methanol allows astonishingly low reduction potentials below the standard reduction potential of -0.52 Vvs SCE.

In this work the approach is different in a way that an organic semiconductor is used as light absorbing donor material in combination with an acceptor catalyst, as for example Pyridinium or (2,2)-bipyridyl)Re(CO)₃Cl, for the actual CO₂ reduction. The advantage lies in the unique properties of organic semiconductors as they are flexible, light weight, biodegradable and bio-compatible, abundant and hold hence the promising perspective to be cheap in production. Figure 1.5 shows the general idea of a photoinduced charge transfer from a biased organic semiconductor onto a catalyst redox mediator for CO₂ reduction.

The schematic drawing in Figure 1.5 shows an organic p-type semiconductor, as for ex-



Figure 1.5: Suggested mechanism for photoinduced charge transfer from a biased organic p-type semiconductor onto a catalyst redox mediator for CO_2 reduction.

ample poly(3-hexylthiophene) (P3HT) on indium tin oxide (ITO), which serves as a transparent conducting electrode (TCE). The whole system is in contact with an electrolyte solution forming a Schottky type of contact.[33] The electrolyte solution contains a catalyst acceptor molecule as for example pyridinium or (2,2)-bipyridyl)Re(CO)₃Cl. Upon light irradiation an electron-hole pair is generated in the organic semiconductor. The electron-hole pair generated can not be treated as individual charge carriers since the positive hole (h^+) and the negative electron (e^-) are initially still bound in the material by their Coulomb attraction.[34] The electron-hole pair, also known as exciton, moves as a quasi particle in the bulk of the material until the two charge carriers recombine or hit an interface where the driving force is strong enough for both charges to separate. In the ideal case the exciton will reach the semiconductor-electrolyte interface where the electron transfers to the catalyst acceptor molecule and the hole, now free to move in the bulk material, travels back to the biased ITO contact where it recombines with an electron. The catalyst material loaded with the negative charge is then capable of transferring this charge to the substrate, namely CO₂, and reducing it to the desired product.

Chapter 2

Experimental techniques

2.1 Electrochemistry

2.1.1 Cyclic voltammetry experiments

Cyclic voltammetry is a useful technique to determine the redox properties of the soluble compounds such as 1-1 to 2-3. It allows indirect studies about the catalytic activity for CO_2 reduction to CO and NADH regeneration. In the presented studies a one-compartment cell was used for cyclic voltammetry experiments, either with a Pt or glassy carbon working electrode, a Pt counter electrode and a Ag/AgCl quasi reference electrode calibrated with ferrocene/ferrocenium (Fc/Fc^+) as an internal reference in organic solvents. In water based systems a standard calomel real reference electrode was used. For CO_2 reduction experiments, the cyclic voltammogram of the metal complexes under N₂ saturation was compared to the spectrum in the presence of carbon dioxide. Electrochemical experiments with organic solvents (e.g. acetonitrile) for CO_2 reduction were performed with 0.1 M tetrabutylammonium hexafluorophosphate (TBAPF₆) as supporting electrolyte, and in water based systems with a 0.1M KCl as supporting electrolyte. It was found that purging of the system with N_2 or CO_2 respectively, for about 15 min under stirring, is sufficient to achieve gas saturation of the electrolyte solution. The catalyst concentration in a cyclic voltammogram experiments was typically 1 mM and the CO_2 concentration was assumed to be at gas saturation of 0.28 M in acetonitrile.[35]

Scheme 2.1(a) shows a schematic picture of the one-compartment cell for cyclic voltammetry experiments during CO_2 purging (A) and during the voltammetry experiment (B). The one-compartment cell used for electrochemistry experiments typically contained about 14 ml of electrolyte solution and 10 ml gas phase. Cyclic voltammetry experiments were usually performed using a JAISSLE Potentiostat-Galvanostat IMP 88 PC.

Optical cyclic volltammetry experiments for photo-electrochemistry with organic semi-



(a) One-compartment cell schematic

(b) Foto of the one-compartment cell

Figure 2.1: (a) One-compartment cell for cyclic voltammetry experiments during CO_2 purging (A) and during cyclic voltammetry measurement (B). Cells containing working electrode (WE), reference electrode (RE) and counter electrode (CE). (b) Foto of a typical one compartment cell with a three electrode setup contacted by crocodile clamps, Ag/AgCl real reference electrode in a 3 M KCl solution and in- and outlets for gas purging.



(a) Quartz cuvette schematic

(b) Foto of the quartz cuvette setup

Figure 2.2: (a)Quartz cuvette for cyclic voltammetry experiments with organic semi conducting electrodes. Cells containing working electrode (WE), reference electrode (RE) and counter electrode (CE). (b) Foto of the Quartz cuvette electochemical setup inside the glove box under white light illumination of a 35 W spot lamp.

2.1. ELECTROCHEMISTRY

conductors as working electrode were preformed in a quartz cuvette cell. A schematic representation of such a quartz cuvette for cyclic voltammetry experiments with organic semi conducting electrodes is depicted in scheme 2.2. These cells contain a transparent working electrode (WE), reference electrode (RE) and a counter electrode (CE). As light source a 35 W halogen spot lamp was used with white light irradiation. The distance between the cuvette and the light source was 7 cm if not stated otherwise.



Figure 2.3: Typical example of a cyclic Voltammograms of 1-1 in CO₂ saturated electrolyte solution as measured during the experiment versus the Ag/AgCl quasi reference electrode potential (black lines with squares and recalculated according to $E_{1/2 \ Fc/Fc+}$ to the NHE potential (red line with circles). Measurements are taken at a scan rate of 100 mVs⁻¹ in acetonitrile with TBAPF₆ (0.1 M), Pt working electrode, Pt counter electrode, and a catalyst concentration of 1 mM.

Experiments with a quasi reference electrode (QRE) have to be calibrated with ferrocene / ferrocenium (Fc/Fc⁺) as an internal reference. The half-wave potential $E_{1/2 Fc/Fc+}$ for Fc/Fc⁺ was measured at eg. 375 mVvs.Ag/AgCl quasi reference electrode potential for the experiment shown in Figure 2.3. The recorded current-potential curve (black line with squares) is then recalculated according to the $E_{1/2 Fc/Fc+}$ to the corresponding normal hydrogen electrode (NHE) potential (red line with circles). For the recalculation to NHE potential the $E_{1/2Fc/Fc+}$ vs. NHE potential offset was taken at 640 mV as suggested by Bazan et al. [36].

2.1.2 Controlled potential electrolysis

Controlled potential electrolysis experiments were generally performed in a gas tight onecompartment or H-cell with a Pt working electrode, a Pt counter electrode and a Ag/AgCl quasi reference electrode. Figure 2.4 shows a scheme of a typical H-cell setup used in the controlled potential experiments. Although a one-compartment cell is easier to handle in terms of setup building and sealing it has the big disadvantage that reduction products

CHAPTER 2. EXPERIMENTAL TECHNIQUES

formed at the working electrode might be re-oxidised on the counter electrode. This problem can be avoided using an H-cell with separated anode and cathode part by a glass frit. However, since the expected product with the transition metal type of catalysts, in aprotic solvents like acetonitrile, is CO and the solubility of CO in a given solvent is typically in the order off 100 times less than for CO_2 , it is expected that little to no CO will remain in solution. In fact the experiments performed with CO evolving catalysts did not show any difference concerning CO yield between the one compartment cell electrolysis experiment and the H-cell experiments.



Figure 2.4: (a) H-cell setup with separated anode and cathode compartment for controlled potential electrolysis. Cells containing working electrode (WE), reference electrode (RE) and counter electrode (CE). (b)

Foto of a typical H-cell used for CO₂ electrolysis experiments.

Figure 2.5 shows a typical current density vs. time plot for CO_2 -electrolysis experiment with compound 1-3 as performed in a one compartment cell. It can be seen that the reductive current initially dropped significantly and afterwards stayed constant with a small decay reflecting the declining concentration of CO_2 substrate in solution over the electrolysis time. Additionally, a plot of current density vs. $1/\text{time}^{1/2}$, as shown in Figure 2.5(b), can give useful information on the kinetics of the process. For example Fick's second law of diffusion shows that a linearity in the current vs. $1/\text{time}^{1/2}$ plot suggests both, a fast electron transfer rate and a time-independent surface concentration of the reactant (in this case CO_2) within the electrolysis time, compare Equation 2.1.[37]

$$j = nF\left(\frac{D}{\pi}\right)^{1/2} \frac{c^0 - c^s}{t^{1/2}}$$
(2.1)

Where j is the current density, n is the number of electrons, F is the Faraday constant, D is the diffusion coefficient, c^0 is the bulk concentration, c^s is the electrode surface concentration and t is the measurement time.

The slope of the line also allows calculating the diffusion coefficient D if the bulk and

electrode surface concentrations are known. The equation cannot be applied for very short time scales, since the initial concentration gradient is very high and the current as such is not limited by diffusion, but by the electron transfer process, compare Figure 2.5(a).[38]



Figure 2.5: Typical current density vs. time plot for potentionstatic CO₂-electrolysis experiment of Re(5,5'bisphenylethynyl-2,2'bipyridyl)(CO)₃Cl (1-3) at constant -1950 mVvs.NHE, performed in acetonitrile solution saturated with CO₂ and an electrolysis time of 3000 s (a) and the same data plotted as current density vs. $1/\text{time}^{1/2}$ (b).

As a direct proof of the catalytic CO_2 -reduction capability of the rhenium catalysts, headspace gas samples are taken and analysed with regard to the CO-concentration using GC and FTIR measurements. The application of transmission IR gas measurements, compared to standard GC analysis, has several advantages. IR measurement has a very short measurement time, high reproducibility, works at ambient temperatures and pressures, shows no vulnerability to interact with a mobile or stationary phase and the gas sample will not come in contact with the detector system. Details to this method used for CO measurements are described in the subsection *Optical spectroscopy methods* and have also been reported in a published paper.[39]

Knowing the amount of products formed and the charges passed through the electrochemical system, the Faradaic efficiency (η_F) can then be calculated according to Equation 2.2.

$$\eta_F = \frac{n_e \times n_P}{n_{etot}} \tag{2.2}$$

Where n_P is the amount of products formed, n_e is the number of electrons needed for each product (compare reactions 1.1 to 1.8) and n_{etot} is the total number of electrons put into the system during the electrolysis experiment, usually optained by integration of the current time curve as plotted in Figure 2.5(a). For the Faradaic efficiency of CO formation Equation 2.2 can be rewritten into Equation 2.3

$$\eta_{FCo} = \frac{2 \times (n_{COgas} + n_{COsol})}{n_{etot}}$$
(2.3)

where n_{COgas} is the amount of CO molecules formed in the gas phase, n_{COsol} is the amount of CO molecules in the electrolyte solution and 2 denotes the two electrons required for the CO₂ reduction to CO (according to the reaction 1.2).

The number of molecules of CO in the gas phase is usually obtained by GC and FTIR analysis, while the number of molecules of CO dissolved in the electrolyte solution is more difficult to obtain. In the experiments presented herein the number was estimated using Henry's Law following Equation 2.4.

$$p_i = k_H \times c \tag{2.4}$$

The Henry constant k_H is taken with (2507 atm mol_{solvent} mol_{CO}), derived from data of Castillo et al.,[40] p_i is the partial pressure of the solute CO and c is the concentration of CO in solution. The number of electrons consumed in the CO₂ electrolysis was determined by integration of the current-time curve of the electrolysis experiment.

With this approach, typical Faradaic efficiency for transition metal catalysts for the reduction of CO_2 to CO, by e.g. the compound 1-3, of about 43 % was deduced and ranks equally with the efficiencies that have been measured for compound 1-1.[39] Literature values of reported Faradaic efficiencies of similar or modified compounds reach values up to 100 %.[41, 42, 43] Furthermore, it has been shown that under these conditions (ACN:TBAPF₆) also small amounts of formate and oxalate can be formed, however with typical Faradaic efficiencies below 1 %.[41]

It should be stated that control experiments, e.g. without catalyst materials present under otherwise identical conditions, are important to verify the technique and should not yield detectable amounts of product formation.

2.1.3 Electropolymerisation

Electropolymerisation of the rhenium catalyst film in chapter 7 was done in potentiodynamic mode in a one-compartment cell also used for cyclic voltammetry experiments, either with a Pt or glassy carbon working electrode, a Pt counter electrode and a Ag/AgCl quasi reference electrode. For the formation of the rhenium catalyst film the catalyst monomer 1-3 was polymerized by repeatedly scanning to negative -1600 mVvs. NHE on a Pt working electrode at 50 mVs^{-1} in nitrogen-saturated acetonitrile solution containing 0.1 M TBAPF₆ and a monomer catalyst concentration of 2 mM.

Electropolymerisation of the polypyrrolle film in chapter 7 including the catalyst monomer 1-1 solution was done by potentiodynamic film formation of a pure polypyrrole film without compound 1-1 present. Pyrrole was electropolymerized on a Pt foil serving as supporting working electrode for the polypyrrole film. Pyrrole was used as received. 625 μ l of pyrrole were added to 18 ml of acetonitrile with TBAPF₆ (0.1 M) as supporting electrolyte to receive a monomer concentration of 0.5 M. The electropolymerisation was performed by sweeping the potential between 1053 mV and -647 mVvs. NHE over 70 cycles with a scan rate of 100 mVs⁻¹.

In a subsequent similar experiment compound 1-1 was dissolved in the pyrrole monomer electrolyte solution with a concentration of 2 mM and used for electro polymerization. After electropolymerization at constant current of 0.1 mA the formed film was removed from the system and washed with pure acetonitrile solution to remove any initial monomer and catalyst material not incorporated into the polymer matrix. Then the polymer film was used as working electrode for heterogeneous CO_2 reduction.

The potentiodynamic electropolymerization of thiophene compounds in chapter 8 was performed in different solvents. 0.1 M thiophene to polythiophene (8-1) was polymerized in ACN solution containing 0.1 M TBAPF₆ as supporting electrolyte. The cyclic voltammograms were recorded at a scan rate of 100 mVs⁻¹ inside the glove box using a Pt working electrode (WE), a Pt counter electrode (CE) and a Ag/AgCl quasi reference electrode. Potentiodynamic electropolymerization of 0.056 M 3-hexylthiophene to poly (3-hexylthiophene) (8-2) was performed in propylene carbonate solution containing 0.1 M TBAPF₆ as supporting electrolyte. The potentiodynamic electropolymerization of approx. 0.015 M Re(4-methyl-4'-(7-thienylheptyl)-2,2'-bypyridene(CO)₃Cl to fac-(2,2'-bipyridyl)Re(CO)₃Cl functionalized poly (3-hexylthiophene) (8-3) was done in in BFEE solution.

2.2 Spectroscopic methods

2.2.1 UV-Vis absorption and PL spectroscopy

UV-vis absorption measurements for the monomer catalysts were performed in a 1 cm quartz glass cuvettes at 298 K with a Cary 3G UV-visible spectrophotometer. Light absorption of the rhenium catalyst film on a Pt working electrode was characterized using an Ocean Optics fibre spectrometer and an ISP-R integrating sphere. The difference in the diffuse reflectance spectra of the non-transparent electrode was compared to a white light standard.



Figure 2.6: Illustration of the general UV-Vis spectrometer setup consisting of a deuterium (D2) and tungsten light source, monochromator, the beam selector, sample compartment and the detector.

Transmission measurements for the PL quenching experiments described in chapter 8 were taken on a Perkin Elmer LAMBDA 1050 double monochromator spectrometer (source doubling mirror) between 400-700 nm in 2 nm steps, with a slit width of 2 nm and a detector response time of 0.2 second. When required, signal to noise was optimized by attenuating the reference beam with internal attenuators. A schematic illustration of the spectrometer is depicted in Figure 2.6.

The LAMBDA 1050 uses automatic 2 A and 3 A attenuation and can be similarly amplified. For all spectra, autozero (100 % and 0 %) correction scans were taken (baseline correction). The spectrometer is equipped with a deuterium (D2) lamp as the UV and a tungsten lamp as the visible and near infrared (NIR) source. The energy is dispersed into specific wavelengths by the use of a reflective gratin. The source change is set to 320 nm, the common beam mask (CBM) is set to 100 %.



Figure 2.7: Illustration of the general PL spectrometer setup consisting of a Xenon arc source, Czerny-Turner type gratings, sample compartment and the PTI PMT detector.

The LAMBDA 1050 utilizes a Photomultiplier R6872 and three detectors for energy detection from 175-3300 nm. A gridless PMT for detection in the UV/Vis, a Peltier cooled InGaAs detector for use in the 800-2600 nm region and a Peltier cooled PbS detector for the range from 2500-3300 nm.

Photoluminescence (PL) spectra were recorded on a PTI QuantaMaster 400 Spectrofluorometer with a continuous Xenon arc lamp (75 W) light source emission range from 185 nm to 680 nm, a Czerny-Turner type excitation monochromator (throughput 65 % at 300 nm) with a focal length of 300 mm, a excitation grating with 1200 line/mm (300 nm blaze), emission grating with 200 line/mm (400 nm blaze) and a multi-mode PTI PMT detector model 914, with a spectral response from 185 to 900 nm (Quantum Efficiency at 260 nm (Peak) 25.4 % typ.). A schematic illustration of the spectrometer is depicted in Figure 2.7.

2.2.2 FTIR absorption spectroscopy

FTIR measurements were performed on a BRUKER IFS 66/S FTIR spectrometer with 4 cm^{-1} spectral resolution. Scheme 2.8 shows a very general illustration of the FTIR setup consisting of a mid infrared (MIR) Glowbar light source, an interferometer with a KBr beam splitter, the sample chamber and the mercury cadmium telluride (MCT) and triglycine sulfate (DTGS) detector.

For Faradaic efficiency calculations, FTIR gas analysis was used as a complementary and independent technique to standard GC measurements for identifying the reduction products



Figure 2.8: Illustration of the general FTIR spectrometer setup consisting of a MIR light source, an interferometer, the sample chamber and the detector.

formed. For the FTIR measurements, a gas tight transmission cell (see Scheme 2.9) with ZnSe windows was designed to measure IR absorption in transmission mode. The spectra were recorded with and without 5 ml headspace sample after different times of electrolysis of the catalyst compounds in solution. For calibration of the systems, a defined amount of calibration gas (Linde) containing 11 % CO₂, 1.5 % CO and 600 ppm C_3H_8 in N₂ was used.

This method has, compared to standard GC analysis, several advantages. The IR measurement has a very short measurement time, high reproducibility, works at ambient temperatures and pressures, shows no vulnerability to interact with a mobile or stationary phase and the gas sample will not come in contact with the detector system.



Figure 2.9: Illustration of the gas tight transmission cell with ZnSe windows built for IR difference absorption spectrum measurement in transmission mode, where I_0 denotes the intensity of the incomeing IR beam and I the intensity of the IR radiation after the sample.

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Figure 2.10 shows a typical IR difference absorption spectrum in transmission mode. The two peaks centred around $2143 \,\mathrm{cm}^{-1}$ correspond to the infrared active rotational-vibrations of the P and R branch of gaseous CO. For further details on the infrared active vibrations of various molecules see reference [44]. The absorption increase at $2350 \,\mathrm{cm}^{-1}$ and the two double peaks centred around $3650 \,\mathrm{cm}^{-1}$ correspond to the infrared active vibrations of CO₂.



(a) IR difference absorption spectra



(b) Foto of IR transmission gas cell

Figure 2.10: (a) IR difference absorption spectrum in transmission mode, with and without 5 ml headspace sample after 50 minutes electrolysis experiment of compound 1-3 in solution. (b) Foto of the IR transmission gas cell with two ZnSe windows as it is mounted in the IR spectrometer compartment.

The area under the peak can be determined by integration. Figure 2.11 shows the calibration of the system by difference absorption spectra in transmission mode, with different volumes of a calibration gas mixture (11 % CO₂, 1.5 % CO and 600 ppm C_3H_8 in N₂). It was found that the peak area is linearly depending on the concentration of CO in the system (see Figure 2.11). With this setup, it was possible to determine the CO gas concentration

in an initially N_2 -filled transmission cell as low as 500 ppm.

2.2.3 ATR-FTIR absorption spectroscopy

Infrared measurements in attenuated total reflection (ATR) mode were performed on a BRUKER IFS 66/S FTIR spectrometer at room temperature, using a mercury-cadmium telluride (MCT) detector cooled with liquid nitrogen prior the measurements. For all ATR-FTIR measurements ZnSe crystal was used as reflection element, which was pre-cleaned by polishing with diamond paste (1 and $0.25 \ \mu$ m) and additional rinsing in a reflux system with acetone. For electropolymerisation, a thin (10 nm) layer of Pt was sputtered onto the ZnSe crystal, serving as a transparent working electrode (WE).

Scheme 2.12 shows the schematic of a ATR-FTIR ZnSe crystal as reflection element. Since ZnSe is not conducting, for spectroelectrochemistry measurements, a thin (10 nm) layer of Pt was sputtered onto the ZnSe crystal, which served as a transparent WE.

For the electropolymerization of compound 1-3 the polymer growth process was investigated with an ex-situ ATR-FTIR technique. For this measurement, the ZnSe reflection element covered with a thin (10 nm) sputtered film of platinum was used as working electrode, and a 150 nm layer of the rhenium catalyst film was potentiostatically electropolymerized on the Pt-surface of the modified ZnSe ATR crystal. The experiment was performed in a one compartment electrochemical cell as depicted in Scheme 2.13(A).

The electrolyte solution contained 0.1 M TBAPF₆, initial monomer1-3 concentration of 2 mM in acetonitrile. For the film formation, the electrochemical cell was connected to the potentiostat and a constant potential of -1550 mVvs.NHE was applied for 500 seconds. After electropolymerization, the ZnSe/Pt electrode with the 150 nm thick catalyst film was washed with pure acetonitrile and dried under N₂ atmosphere. Then the crystal was mounted into an ATR-FTIR setup between two PTFE spacers (as depicted in Scheme 2.13(B)) and the ATR-FTIR difference absorption spectra between a pure ZnSe/Pt electrode and the ZnSe/Pt electrode with the catalyst film were recorded. (The corresponding spectra are shown and discussed in chapter 7.)

2.3 Analytical methods for product analysis

For a direct proof of the catalytic CO_2 reduction capability of the catalyst materials, product analytics is a very important point. In most cases of the CO forming catalytic compounds 1-1 to 2-3, headspace gas samples were taken and analysed regarding the CO concentration by either GC or FTIR headspace gas sampling. For the FTIR absorption measurements a special gas tight IR transparent measurement cell containing two ZnSe windows was developed in our laboratory as already described (for a schematic drawing see Scheme 2.9). Additionally to the



(b) Peak area of the spectra in (a)

Figure 2.11: (a) IR difference absorption spectra in transmission mode, with different volumes of a N₂ calibration gas mixture (11 % CO₂, 1.5 % CO and 600 ppm C₃H₈ in N₂). (The two peaks centred around 2143 cm⁻¹ correspond to the infrared active vibration of CO, the peak at 2350 cm^{-1} to the vibrations of CO₂.). (b) Peak area of IR difference absorption peaks centred around 2143 cm⁻¹ in transmission mode at different CO volumes (black squares) and linear interpolation between peak areas (black dotted line).





(b) Foto of an ATR-FTIR ZnSe crystal

Figure 2.12: (a) Schematic of a ATR-FTIR ZnSe crystal as reflection element. For spectroelectrochemistry measurements, a thin (10 nm) layer of Pt was sputtered onto the ZnSe crystal, which served as a transparent WE. (b) Foto of an ATR-FTIR ZnSe crystal with a thin (10 nm) layer of sputtered Pt and conductive silver paste on top for back contact



Figure 2.13: A) One-compartment cell with a ZnSe reflection element covered with a thin (10 nm) sputtered layer of Pt (gray) as the WE for the electropolymerization of the catalyst polymer (2, violet). B) Schematic of the mounted ATR-FTIR crystal with the polymer film (violet) inside the spectrometer.

FTIR measurements gas chromatography was the main technique for product determination.

2.3.1 Gas chromatography

Gas chromatography (GC) analysis for CO was conducted on a Thermo Trace GC equipped with a TCD detector and a Phenomenex PLTT 5A column (30 m, 0.53 mm ID, 25 μ m film). The carrier gas was helium at 3 ml min⁻¹, the GC was programmed from 45 °C for 5 min to 300 °C for 1 min with a heating rate of 30 °C min⁻¹. The injector was operated at 300 °C with a split ratio of 1:10 and the detector at 200 °C with 27 ml min⁻¹ make up gas. 1 mL sample was injected with a gastight syringe directly from the reaction vessel.



(a) One-compartment cell

(b) ATR-FTIR setup

Figure 2.14: (a) Picture of the PTFE cell for ATR-FTIR spectroelectrochemistry with tubes for electrolyte in- and outlet and the Pt counter electrode visible in the back of the cell (b) Foto of the ATR-FTIR setup mounted in the FTIR spectrometer with the three electrode setup and the ZnSe ATR crystal.

Figure 2.15(a) shows a typical GC analysis of a headspace sample (200 μ l) after a 25 minutes electrolysis experiment with compound 1-3 in a single-compartment cell containing CO₂ saturated acetonitrile solution with TBAPF₆ (0.1 M), a Pt working electrode, a Pt counter electrode, and a catalyst concentration of 1 mM. The chromatogram is shown in the time frame of 0 to 550 s. In this measurement three peaks are present corresponding to O₂ and N₂ at around 60 s, CO at around 90 s and CO₂ at 500 s retention time. Figure 2.15(b) shows liquid GC calibration measurements for various concentrations of methanol in water with an injection volume of 1 μ l. The retention time for the methanol peak maximum is typically at 2.07 min. The inset shows the linear polynomial fit of the calibration peak area according to y = intercept + slope $\cdot x$, with a slope of 0.015 with an error of 3.404⁻⁴ and the intercept at 0.01 with an error of 0.009. The calibration measurement shows excellent linearity in the concentration range from 1 to 50 ppm of methanol with a mean square value (R²) of 0.99891 and a Pearson R of 0.99945.

2.3.2 Ion chromatography

Ion chromatography (IC) measurements for the detection of formate, acetate, carbonate and oxalate were done on a Dionix ICS 5000 equipped with a conductivity detector and a separated pre- (AG19, CAP, $0.4 \ge 50$ mm) and main-column (AS19, CAP, $0.4 \ge 250$ mm). The eluent source was a Dionix EGC-KOH (capillary). Measurement time was 27 min. with 45 mM target concentration and a reduced concentration of 10 mM (6 min). Eluent generation for 10min (10mM) with increasing the concentration (ramp 3 mM/min) for 15 min to 45 mM (3 min). The sample (1 ml) was injected with a 2 or 5 ml plastic syringe (Braun) using a PES 0.45 μ m Roth filter.



(b) Liquid Gas Chromatography

Figure 2.15: (a) GC analysis of a headspace sample (200 μ l) after a 25 minutes electrolysis experiment with compound 1-3 in a single-compartment cell containing CO₂ saturated acetonitrile solution with TBAPF₆ (0.1 M), Pt working electrode, Pt counter electrode, and a catalyst concentration of 1 mM. (b) Liquid GC calibration measurements for various concentrations of methanol in water. The retention time for the methanol peak maximum is typically at 2.07 min. Inset: Linear fit of the calibration peak area.

2.4 Homogeneous photocatalysis

Photocatalytic reactions were performed in a 10 ml quartz cell filled with 6 ml of a mixture of dimethylformamide and triethanolamine (DMF:TEOA = 5:1/v:v) containing a catalyst concentration of 2.6 mM under CO₂ saturation. The solution was stirred during the experiment and a 360 nm low pass cutoff filter was used. The irradiation time was 18 h under 26900 lux with an Osram 400 W Xenophot xenon lamp. The irradiated cell cross section area was 3.14 cm^2 . Gas samples were taken with a gas tight syringe and transferred to eighter FTIR gas analysis (for a schematic drawing see Scheme 6.2, in chapter 6) or GC analysis.

2.5 Catalyst materials

Scheme 2.16 shows the schematics of four rhenium(I) tricarbonyl chloride complexes with different diimine ligand systems, that is $(2,2'-bipy.)Re(CO)_3Cl$ (1-1), $(4,4'-dicarboxyl-2,2'-bipy.)Re(CO)_3Cl$ (1-2), $(5,5'-bisphen.-2,2'-bipy.)Re(CO)_3Cl$ (1-3) and [5,5'-bis (LL)-2,2'-bipy.]Re(CO)_3Cl (1-4) where LL for compound 1-4 is (2,6-bis-octyloxy-4-formyl) phenylethinyl) used for CO₂ reduction throughout the thesis. Scheme 2.16(b) shows the schematics of three different Re(BIAN-R)(CO)_3Cl compounds (2-1 to 2-3) that have been used as novel materials for the aim of CO₂ reduction in chapter 5. The compounds have been synthesized according to literature procedure. [45]



(a) Rhenium compounds with bipyridyl ligands



(b) Rhenium compounds with (BIAN-R) ligands

Figure 2.16: (a) Schematic chemical structures of different rhenium bipyridyl compounds (2,2)-bipyridyl)Re(CO)₃Cl (1-1), (4,4)-dicarboxyl-2,2'-bipyridyl)Re(CO)₃Cl (1-2), (5,5)-bisphenylethynyl-2,2'-bipyridyl)Re(CO)₃Cl (1-3) and [5,5)-bis ((2,6-bis-octyloxy-4-formyl)phenylethinyl)-2,2'-bipyridyl]Re(CO)₃Cl (1-4) for CO₂ reduction. (b) Schematic chemical structures of three different rhenium compounds with bis(arylimino)acenaphthene derivatives (BIAN-R) ligands (2-1), (2-2) and (2-3) for CO₂ reduction.
Chapter 3

Photophysical results

The photocatalytic efficiency of different diimino rhenium carbonyl complexes for the reduction of carbon dioxide to CO is strongly dependent on the electronic structure and the redox properties of these compounds. As stated by Takeda et al.[46] the lowest electronic excited states of bipyridine-based rhenium diimime carbonyl complexes, mainly of ³MLCT* and ${}^{3}\pi\pi^{*}$ character, are frequently quite close in energy and may also be mixed with each other. Focusing on photochemical CO₂ reduction, almost all applicable catalysts have in common, that their lowest excited state is of the ³MLCT* character with a relatively long lifetime in the 10-100 ns range.[46] This state can be quenched reductively by suitable sacrificial electron donors such as triethanolamine (TEOA or TEA) to generate a one-electronreduced (OER) species. These OER molecules can form adducts with CO₂, the structure of which is not yet fully clear. There are various proposed intermediates by different research groups.[47, 48, 49] In most of the suggested catalytic pathways, one of the OER-CO₂ adducts reacts with a second OER radical in order to obtain CO as a reaction product and retrieve the initial catalyst.

The nature of the bipyridyl ligand influences the energetic levels of the possible electronic transitions upon excitation with UV and visible light. A simplified scheme of the most common electronic structure for similar rhenium carbonyl complexes is shown in Scheme 3.1.[46] The prototype compound Re(bpy)(CO)₃Cl (1-1) is taken as a basic template for the following descriptions. It's UV-visible absorbance spectrum in toluene is shown in Figure 3.3 (black line with squares). It shows two distinct maxima at 300 and 400 nm and the room temperature photoluminescence (red line with triangles) at an excitation wavelength of $\lambda_{exc} = 380$ nm shows a broad emission from 450 to 750 nm with a maximum at 550 nm.

The absorbance spectra of the rhenium bipydridyl complexes 1-1 to 1-4 exhibit strong electronic ${}^{1}\pi\pi^{*}$ intraligand transitions of the diimine ligands in the higher energetic region, usually at wavelengths shorter than 330 nm and MLCT signatures at lower energies.[50, 51, 45, 52] Additional weaker UV-bands of IL origin can be observed for compounds 1-3 and 1-4 in the 300 - 320 nm spectral region. These bands suggest energetic splitting of approximately 2200 cm^{-1} due to coupling to phenylethynyl C-C vibrational modes.[50] The absorbance and



Figure 3.1: Schematic energy diagram of the lowest-lying excited states of complexes 1-1 to 1-4.[46]

emission data in various solvents for compounds 1-1 to 1-4 are summarized in Table 5.1.

Besides substituent effects on the spectra, what is most remarkable and also well known about the absorbance of the described compounds is the fact that the ¹MLCT transition is strongly dependent on solvent effects; [53, 50, 54] this can also be seen in Figure 3.2 comparing the spectra of compound 1-3 in dichloromethane to the spectrum recorded in acetonitrile. In the more polar solvents such as methanol or acetonitrile the lowest lying ¹MLCT absorbance is shifted to the red by 30 nm compared to less polar solvents like toluene or dichloromethane. Furthermore the carboxyl substituted compound 1-2 shows a strong red shift of the MLCT of about 2770 cm⁻¹ as compared to complex 1-1, due to the electron withdrawing effect of the carboxyl groups.

Compound	Solvent	Absorbance	Emission
		$[\lambda_{max}]$	$[\lambda_{max}]$
$(2,2'-bipy.) \text{Re}(\text{CO})_3 \text{Cl} (1-1)$	Toluene	299, 403	550
$(2,2'-bipy.) \text{Re}(\text{CO})_3 \text{Cl} (1-1)$	Methanol	369	
(4,4)-dicarb2,2)-bipy.)Re(CO) ₃ Cl (1-2)	Methanol	394	
(5,5'-bisphen2,2'-bipy.)Re(CO) ₃ Cl (1-3)	Dichloromethane	245, 290, 390	442,689
$(5,5'-bisphen2,2'-bipy.) Re(CO)_3 Cl (1-3)$	Acetonitrile	360	
$([5,5]-bis (LL)-2,2]-bipy.]Re(CO)_3Cl (1-4)$	Toluene	430	428,695
$([5,5]-bis (LL)-2,2]-bipy.]Re(CO)_{3}Cl (1-4)$	Dichloromethane	427	
$([5,5]-bis (LL)-2,2]-bipy.]Re(CO)_{3}Cl (1-4)$	Methanol	411	

Table 3.1: Summary of photophysical data of rhenium tetracarbonyl diimino complexes 1-1 to 1-4. The abbreviation LL for compound 1-4 is (2,6-bis-octyloxy-4-formyl)phenylethinyl)

The photophysics of the rhenium complex 1-3 is dominated by the presence of the reducing rhenium(I) tricarbonyl chloride donor fragment, which leads to a luminescent lowest-



Figure 3.2: UV-visible absorption spectra of the rheniumcarbonyl-complexes 1-1 to 1-4 in different solvents. In more polar solvents such as methanol (MeOH) or acetonitrile (ACN) the lowest lying ¹MLCT absorbance is shifted to the red by 30 nm compared to less polar solvents like toluene or dichloromethane (DCM).



Figure 3.3: (a) UV-visible absorption (black line with squares) with two maxima at 300 and 400 nm and photoluminescence (red line with triangles) spectra of rhenium carbonyl complex 1-1 in toluene at room temperature and $\lambda_{exc} = 380$ nm. (b) UV-visible absorption (black line with squares) and emission spectra at $\lambda_{exc} = 388$ nm (red line with triangles) of the rhenium carbonyl complex 1-3 in dichloromethane at room temperature. The ³MLCT emission spectra is indicated by a maximum at around 650 nm and additional shoulders at 590 and 700 nm.

energy triplet excited state of the metal-to-ligand charge transfer type. In some cases, such as with compounds 1-3 and 1-4, the emission quantum yield is very low ($\phi \leq 0.001$). The broad ³MLCT emission of 1-3 in dichloromethane solution is also covering a typical wide spectral region including orange and red light exhibiting a maximum at around 650 nm and showing additional shoulders at 590 and 700 nm (Figure 3.3(b)). Interestingly, upon UV-light excitation at the absorption peak maximum of 1-3, the compound also shows an additional structured blue green intraligand emission with maxima at 443 and 465 nm, which is not completely quenched by the lower-lying MLCT states (Figure 3.3(b)).[50] This is not the case for the non-substituted parent compound (2,2'-bipyridyl)Re(CO)₃Cl (1-1) (Figure 3.3(a)) and was found to be caused by the additional phenylethinyl groups of the diimine ligand of 1-3.

Comparable dual luminescence behavior has also been reported for similar multichromophore systems investigated by Schanze and coworkers.[52] Additionally compound 1-4, the absorbance and luminescence spectra exhibits similar spectroscopic properties as catalyst 1-3. This is not surprising, considering that 1-3 and 1-4 are structurally related. The IL luminescent transition of 1-4 lies in the range between 400-500 nm in this case, whereas the ³MLCT emission is observed in the region higher than 600 nm.[45]

Chapter 4

Quantum chemical calculations

Computational quantum chemical calculations has developed over the last few decades as a versatile part of science, that generates calculated data which supplements experimental obtained data and helps to determine on the structures, properties and reactions of atoms and molecules. Sometimes quantum chemical calculations allow the determination of properties that are difficult to get experimentally. The quantum mechanical calculations are based primarily on the development of quantum mechanics by the beginning of the 20th century. Nowadays powerful computer programs are used for calculation of electron and charge distributions, molecular geometry in ground and excited states, potential energy surfaces, rate constants for elementary reactions, details of the dynamics of molecular collisions and many other things. [55, 56] In this work quantum mechanical calculations were mainly used for the interpretation of experimental obtained data such as infrared absorption spectra and for the calculation of molecular orbital energy levels.

The method used was similar to the one reported in literature reference nr [50]. The calculations were carried out with Gaussian09.[57] All quantum-chemical calculations were carried out using a density functional theory (DFT) based method with the hybrid B3LYP functional.[58, 59, 60] The 6-31G(d) basis set was used through the calculations,[61, 62, 63] whereas for the complexed rhenium metal the LanL2DZ basis set [64, 65, 66, 67] was applied. The obtained geometries were verified to correspond to a real minimum by establishing an absence of imaginary IR frequencies.

4.1 Infrared absorption spectra

The technique of infrared spectroscopy is a very powerful tool in chemistry and physics. Electromagnetic radiation in the micrometer range, i.e. electromagnetic radiation with wavelengths in the order of 10^{-6} m, has enough energy to excite molecular vibration-rotation transitions.[68] Since molecules have different, characteristic vibration-rotation transitions due to the effective mass of the molecules and force constant of chemical bonds in the molecule, infrared spectroscopy allows for analytical characterization of a molecular substance. However, since the vibrational degree of freedom for non linear molecules scales with 3N-6, with N being the number of atoms in the molecule, one can imagine that infrared spectra get very complicated for larger molecules making the spectra difficult to interpret. For this reason calculated IR absorption spectra by quantum mechanical DFT calculations are successfully used to correlate characteristic features in the measured spectra to their molecular origin.



Figure 4.1: IR absorption spectra of $\text{Re}(2,2'-\text{bipyridyl})(\text{CO})_3\text{Cl}$ (1-1). Experimentally measured FTIR difference absorption spectra in KBr (black solid line with squares) and corresponding calculated IR absorption spectra by DFT without (red line) and with (blue dashed line) solvent effects taken into account.

Figure 4.1 shows for example the FTIR difference absorption spectra of compound 1-1 measured in KBr (black solid line with squares) and the corresponding calculated IR absorption spectra by ab initio DFT method (red and blue lines) with the software Gaussian09. It should be noted that $\text{Re}(2,2'-\text{bipyridyl})(\text{CO})_3\text{Cl}$ is here used as an example only. The reader will notice that within the thesis many IR-spectra of similar type of materials will be presented and discussed in detail.

The infrared spectrum of complexes of the (LL)Re(CO)₃Cl-type are dominated by their characteristic signals connected to the C \equiv O vibrations positioned at around 1900 cm⁻¹ and 2000 cm⁻¹ respectively.[42, 50] As the IR absorption bands of the C \equiv O vibrations are dominant in the spectra and reside in the frequency region where no other absorption bands exist, these bands are useful to probe the electronic exited states of these compounds. Additionally, these band frequencies are greatly influenced by the amount of the electron density on the central rhenium (I) atom, which is considered to be the driving force for catalytic CO₂ reduction.[46] Similar vibrations have been found in for example the related compound (5,5'-bisphenylethynyl-2,2'-bipyridyl)Re(CO)₃Cl.[39] The signal at 1650 cm⁻¹ is typical for the C=C stretching vibrations in the aromatic ligand system. The weak signals around 1500 cm^{-1} are characteristic C-H bending vibrations and those at 880, 800 and 720 cm⁻¹ are attributed to C-H rocking vibrations.[69]

As can be seen in Figure 4.1, experimentally observed data and quantum chemical predictions for the IR spectra of the novel compound are in good agreement. For the prediction of infrared spectra it is often necessary to scale the obtained calculated data by a constant factor to achieve good matching of calculated and measured spectra. It was found that calculated ab initio harmonic vibrational frequencies are typically larger than the fundamental vibrational frequencies observed experimentally. Theoretical analysis showed that one main reason of this disagreement is the neglect of anharmonicity effects in the theoretical treatment. Additional complication comes of incomplete incorporation of electron correlation and the fact that used basis sets are finite. Hartree-Fock (HF) theory for example, which is commonly used in DFT based calculations, generally tends to overestimate the calculated vibrational frequencies because of unsuitable dissociation behavior. This limitation can sometimes be overcome by the explicit inclusion of electron correlation. A detailed analysis of this effect with suggestions of different scaling factors can be found in reference [70].

4.2 Molecular orbital energy levels

In this section quantum mechanical calculations were carried out for the determination of molecular orbital frontier energy levels. Figure 4.2 depicts for example the energy levels of the last four occupied and first four unoccupied molecular orbitals (MO) of the compound $Re(2,2'-bipyridyl)(CO)_3Cl$ obtained from theoretical calculations at the DFT level.



Figure 4.2: Molecular orbital energy levels of $\text{Re}(2,2'-\text{bipyridyl})(\text{CO})_3\text{Cl}$ calculated by DFT for the frontier orbitals including HOMO-LUMO gap.

Similar calculations were carried out for other mocleculs of the complexes of the $(LL)Re(CO)_3Cl$ -type. Table 4.1 summarizes the values of quantum mechanical calculations of different rhenium compounds studied in the present work. As can be seen in Table 4.1, quantum mechanical calculations yield a HOMO energy level of about -5.50 eV and a LUMO energy level of about -2.95 eV eV for $(5,5'\text{-bisphenylethynyl-2,2'-bipyridyl})Re(CO)_3Cl$ resulting in a band gap of about 2.56 eV. Similar calculations for the simple $Re(2,2'\text{-bpy})(CO)_3Cl$, compare Figure 4.2, gave a lager band gap of 2.89 eV which is in agreement with the UV-Vis absorption measurements depicted in Figure 3.2 in the chapter 3. It should be notice however, that quantum mechanical calculations are based on many assumptions giving only an estimate of the real molecular properties at best.

Compound	HOMO-LUMO	HOMO	LUMO	Band Gap
	[Orbital nr.]	[eV]	[eV]	[eV]
$(2,2'-bipy.)Re(CO)_3Cl (1-1)$	78 - 79	-5.62	-2.73	2.89
(4,4'-tbut2,2'-bipy.)Re(CO) ₃ Cl	110 - 111	-5.45	-2.41	3.04
(4,4'-bisphen2,2'-bipy.)Re(CO) ₃ Cl	130 - 131	-5.62	-2.97	2.66
(5,5'-bisphen2,2'-bipy.)Re(CO) ₃ Cl	130 - 131	-5.51	-2.95	2.56

Table 4.1: Summary of quantum mechanical calculations of different rhenium compounds studied in the present work.

Many professional programs for quantum mechanical calculations such as Gaussian09 allow impressive visual representation of calculated data. Figure 4.3 shows the visual representation of molecular frontier orbitals of different rhenium compounds as obtained from theoretical calculations at the DFT level. The results obtained from DFT calculations are in particular interesting when compared with optical measurements. The assignment of the lowest-lying excited states of $\text{Re}(2,2'-\text{bipyridyl})(\text{CO})_3\text{Cl}$ and its related compounds in chapter 3 as intraligand (IL) and metal-to-ligand charge transfer (MLCT) type is in agreement with the results obtained from the DFT calculations and with previous studies of similar compounds reported in literature.[50] In the visual representation in Figure 4.3 it can be clearly seen, that the calculated highest occupied molecular orbital (HOMO) of the rhenium complex carries a significant metal d-orbital contribution from the $\text{Re}(\text{CO})_3\text{Cl}$ fragment, which determines the charge transfer character of the lowest excited states in this materials.





(a) (2,2'-bipy.)Re(CO)₃Cl HOMO

(b) (2,2)-bipy.)Re(CO)₃Cl LUMO



(c) (4,4'-tbut-2,2'-bipy.) $\operatorname{Re}(\operatorname{CO})_3\operatorname{Cl}$ HOMO



(d) (4,4'-tbut-2,2'-bipy.) $\operatorname{Re}(\operatorname{CO})_3\operatorname{Cl}$ LUMO



(e) (4,4'-bisphen.-2,2'-bipy.) $\operatorname{Re}(\operatorname{CO})_3\operatorname{Cl}$ HOMO



(f) (4,4'-bisphen.-2,2'-bipy.) $\operatorname{Re}(\operatorname{CO})_3\operatorname{Cl}$ LUMO



(g) (5,5'-bisphen.-2,2'-bipy.) Re(CO)_3Cl HOMO



(h) (5,5'-bisphen.-2,2'-bipy.) $\operatorname{Re}(\operatorname{CO})_3\operatorname{Cl}$ LUMO

Figure 4.3: Visual representation of molecular frontier orbitals of different rhenium compounds studied in the present work.

Chapter 5

Homogeneous electro catalysis

At present most of the best studied catalysts are metal complexes with bipyridine ligands, where the catalyst center consists of transition metals based on rhenium (Re), rhodium (Rh) or ruthenium (Ru). Despite their high current efficiencies and high selectivity, problems in the field of artificial solar fuel production by these catalysts are manifold. Although these molecular catalyst compounds can be used to stabilize intermediate steps of the CO_2 reduction process and thus lower the required overpotential, achieving a simultaneous multiple electron and proton transfer as indicated by the described reactions 1.3 to 1.8, is kinetically extremely difficult to realize and over potentials of most reported catalyst systems are still significantly high. In Figure 5.1 a schematic representation of a catalyzed and a non catalyzed reaction mechanism with respect to the energy niveau over the reaction coordinate is depicted.



Figure 5.1: Schematic representation of a catalyzed and a non catalyzed reaction mechanism with respect to the energy niveau over the reaction coordinate.

Furthermore, systems based on these catalyst materials, as reported up to now, suffer from low stability and low turnover frequency. In recent yeas Bocarsly et. al. [30] reported on the catalytic reduction of CO_2 to methonol by Pyridinium (the protonated form of Pyridine). Although this system demonstrates only a very low rate of reaction due to a complicated mechanism, which is not jet fully understood, the approach seems to very promising regarding earth abundant catalyst materials and proton rich products. The materials investigated in this chapter dealing with homogeneous electro catalysis are Rhenium diimine complexes with different ligand systems as well as the Pyridinium catalyst. In the following three sections *Rhenium compounds with bipyridine ligands*, *Rhenium compounds with bian ligands* and *Pyridinium as catalyst* the properties of these materials as homogeneous electro catalysts for CO_2 reduction will be investigated.

5.1 Rhenium compounds with 2,2'-bipyridine ligands

Concerning the generation of CO from carbon dioxide, metal complexes with bipyridine ligands are among the most promising candidates for homogeneous catalysis in terms of activities and lifetimes [19, 20]. Up to now, mainly rhenium- and ruthenium-based systems have been reported for their ability to electrochemically or photochemically accelerate the reduction of CO₂ to CO. Carbon monoxide itself can be used as a precursor compound for fuel synthesis processes, where CO and H₂ are mixed as syn-gas to form hydrocarbons such as methane or methanol [24, 71]. Figure 5.2 shows the schematic mechanism for the two electron CO_2 reduction of (2,2'-bipyridyl)Re(CO)₃Cl (1-1) and related compounds to CO and CO_3^{2-} as first proposed by Sullivan and Meyer et. al. in 1989.[72]



Figure 5.2: Schematic mechanism for the two electron CO_2 reduction of $(2,2'-bipyridyl)Re(CO)_3Cl$ (1-1) and related compounds to CO and CO_3^{2-} .

Scheme 5.3 in this section shows the schematics of four rhenium(I) tricarbonyl chloride complexes with different dimine ligand systems, that is $(2,2'-bipy.)Re(CO)_3Cl$ (1-1), $(4,4'-dicarboxyl-2,2'-bipy.)Re(CO)_3Cl$ (1-2), $(5,5'-bisphen.-2,2'-bipy.)Re(CO)_3Cl$ (1-3) and [5,5'-bis (LL)-2,2'-bipy.]Re(CO)_3Cl (1-4) where LL for compound 1-4 is (2,6-bis-octyloxy-4formyl)phenylethinyl) used for CO₂ reduction.

The (2,2'-bipyridyl) and (4,4'-dicarboxyl-2,2'-bipyridyl) ligand were purchased from commercial suppliers (Fluka, Aldrich). The multichromophoric diimine ligand (5,5'-bisphen-ylethynyl-2,2'-bipyridyl) was synthesized from 2,2'-bipyridine according to published routes

through the formation of 5,5'-dibromo-2,2'-bipyridine and additional Pd-catalyzed Sonogashira coupling of the dibromo-compound with phenylacetylene.[50, 73, 74] [5,5'-bis((2,6bis-octyloxy-4-formyl)phenylethinyl)-2,2'-bipyridyl] was obtained via coupling of 5,5'-dibromobipyridine with 1,5-dioctyloxy-4-ethinyl-benzaldehyde. Synthesis of the rhenium complexes was then achieved by further metallation with $\text{Re}(\text{CO})_5$ Cl in toluene as described in the literature.[53, 75, 76]



Figure 5.3: Schematic chemical structures of four different rhenium compounds $(2,2'-bipyridyl)Re(CO)_3Cl$ (1-1), $(4,4'-dicarboxyl-2,2'-bipyridyl)Re(CO)_3Cl$ (1-2), $(5,5'-bisphenylethynyl-2,2'-bipyridyl)Re(CO)_3Cl$ (1-3) and [5,5'-bis ((2,6-bis-octyloxy-4-formyl)phenylethinyl)-2,2'-bipyridyl]Re(CO)_3Cl (1-4) for CO₂ reduction.

Figure 5.4 shows the cyclic voltammograms of 1-1 in nitrogen saturated electrolyte solution on the reductive side (black line with circles) and in a seperate scan the oxidative side (blue line with circles). When the solution was saturated with N₂, compound 1-1 shows a one-electron quasi-reversible reduction wave with its maximum around -1200 mVvs. NHE followed by a one-electron irreversible reduction wave at more negative potential around -1530 mVvs. NHE. This characteristics for rhenium-bipyridine based catalysts are well known and were first reported in this contents by Lehn et al. in 1984.[77] The peak at -1200 mVvs. NHE of compound 1-1 can be attributed to a ligand based reduction and is reversible with its re-oxidation at around -1100 mVvs. NHE. The second reduction wave at -1530 mVvs. NHE can be assigned to a reduction at the metal centre and is not reversible. The oxidative scan (blue line with circles) is somehow interesting since it is usually not reported in most publications where people focus only on the reduction properties of these compounds. On the oxidative side two non reversible oxidation waves are measured. The first with a peak maximum at around 1500 mVvs. NHE and the second with its onset around 1800 mVvs. NHE. The nature of these peaks are speculative and would be a matter for further study. The other compounds presented in this section show a similar behaviour.



Figure 5.4: Cyclic Voltammograms of 1-1 in nitrogen saturated electrolyte solution on the reductive side (black line with circles) and oxidative side (blue line with circles). Measurements are taken at a scan rate of 100 mVs^{-1} in acetonitrile with TBAPF₆ (0.1 M), Pt working electrode, Pt counter electrode, and a catalyst concentration of 1 mM.

Figure 5.5(a) shows a comparison of cyclic voltammograms between compound 1-1 and compound 1-4. These measurements indicate the strong dependence of these compounds on the ligand system. For compound 1-4 the extended conjugated ligand results in a clear shift for the first reduction wave to a more positive potential. As a consequence, also the UV-vis absorption maximum (a MLCT band) is shifted to a longer wavelength as expected and can be seen in Figure 5.5(b). This behavior is important to tune the properties of these metal-organic compounds to improve their capability for electro- and photo- catalytic CO_2 reduction.

Figure 5.6 shows the cyclic voltammograms of 1-1 in nitrogen (black line with squares) and CO₂ (red line with circles) saturated electrolyte solution. When the solution was saturated with N₂, compound 1-1 shows the typical behaviour already described and shown in Figure 5.4. In CO₂-saturated solution (red line with circles), compound 1-1 shows a strong enhancement in current density at the second irreversible reduction wave at about -1750 mVvs. NHE. This enhancement in current is known to be the catalytic reduction of CO₂ to CO and is assumed to proceed in aprotic solvents according to reaction 1.2. The first quasi-reversible reduction wave at around -1200 mVvs. NHE does not show a significant increase in current density and is hence not participating in the catalytic reaction directly.

Figure 5.7 shows the same cyclic voltammograms as in Figure 5.6 namely the catalyst 1-1 in nitrogen (black line with squares) and CO_2 (red line with circles) saturated electrolyte



(b) UV-vis absorption spectra comparison

Figure 5.5: (a) Comparison of 1-1 (black line with squares) and 1-4 (blue line with triangles) in cyclic voltammograms and taken at $100 \,\mathrm{mVs^{-1}}$ in dimethylformamide with TBAPF₆ (0.1 M), Pt working electrode, Pt counter electrode, and a catalyst concentration of 0.5 mM. (b) Comparison of UV-vis absorption spectra of 1-1 (black line with squares) and 1-4 (blue line with triangles) recorded in methanol.



Figure 5.6: Cyclic Voltammograms of 1-1 in nitrogen (black line with squares) and CO_2 (red line with circles) saturated electrolyte solution. Scan with CO_2 saturation shows a large current enhancement due to a catalytic reduction of CO_2 to CO. Measurements are taken at a scan rate of $100 \,\mathrm{mVs^{-1}}$ in acetonitrile with TBAPF₆ (0.1 M), Pt working electrode, Pt counter electrode, and a catalyst concentration of 1 mM. A scan with no catalyst present under CO_2 (blue dotted line) shows negligible reductive current.

solution. Different to the previous measurement however, the working electrode was changed from a platinum to a glassy carbon electrode. Again compound 1-1 shows a strong enhancement in current density at the second irreversible reduction wave at about -1750 mVvs. NHE indicating that the catalytic activity of this and similar compounds is not due to the nature of the electrode in use. Additionally this is important due to the fact that CO, which is the main reduction product, is know to lead to a deactivation of the platinum electrode surface by irreversibly binding to and blocking the electrode surface layer.

Although well studied in the past, the catalytic cycle for electrochemical CO_2 reduction of compound 1-1 (and similar compounds presented herein) is still not fully understood. However, it is known that the catalytic mechanism needs an empty coordination site for CO_2 binding which is identified to proceed via the loss of the halide (Cl⁻). Some detailed studies on this mechanism have been carried out initially by Sullivan et al.[47] and Lehn et al.[78] in 1985 and 1986, respectively. A more recent study on this was carried out by Johnson et al. in 1996 reviewing several proposed mechanisms.[79]

Figure 5.8 shows the cyclic voltammograms of compound 1-2 measured in N₂ and CO₂ saturated acetonitrile solution, respectively. In comparison to compound 1-1, compound 1-2 does not show a clear and pronounced reversible one-electron quasi-reversible reduction wave around -1200 mVvs.NHE although the onset is still observable. A non-reversible wave can be observed at around -1500 mVvs.NHE which can be attributed to the additional carboxyl groups on the bipyridyl ligand. In contrast to previously published data,[42] the modified compound 1-2 showed some catalytic behaviour towards CO₂ reduction when the electrolyte solution was saturated with CO₂, as can be seen in Figure 5.8(a) (red line with



Figure 5.7: Cyclic voltammograms of 1-1 in nitrogen (black line with squares) and CO_2 (red line with circles) saturated electrolyte solution. Scan with CO_2 saturation shows a large current enhancement due to a catalytic reduction of CO_2 to CO. Measurements are taken at a scan rate of 100 mVs^{-1} in acetonitrile with TBAPF₆ (0.1 M), glassy carbon working electrode, Pt counter electrode, and a catalyst concentration of 1 mM. A scan with no catalyst present under CO_2 (blue dotted line) shows negligible reductive current.

circles). However, CO_2 potentiostatic bulk electrolysis at -2100 mVvs.NHE revealed that the compound seems to be unstable and loses its catalytic activity within several minutes of electrolysis time.

When the acetonitrile solution was saturated with CO_2 , also compound 1-3 showed a strong enhancement in the second reduction wave current density. In relative comparison a 6.5-fold increase at the second irreversible reduction wave under CO_2 at -1750 mVvs.NHEwas observed. Comparing this to compound 1-1, the relative increase in current density is higher for compound 1-3. A detailed study on compound 1-3 has been published.[39]

Figure 5.9(a) shows the cyclic voltammograms of compound 1-3 recorded under N₂- and CO₂-saturated acetonitrile solution. In contrast to compound 1-1, compound 1-3 does not show a clear separation between different reductive waves. Additionally, the onset of the reductive current occurred at a potential around -750 mVvs.NHE, which is about 330 mV more positive compared to compound 1-1 (Figure 5.7). This significant differences between compound 1-1 and 1-3 can be attributed to the addition of the bisphenylethynyl groups at the 5,5' position (the phenyl rest is para substituted with respect to the bipyridine ligand). When compound 1-3 was scanned repeatedly under N₂ - saturated conditions to very negative potentials (i.e. -1600 mVvs.NHE), a violet film formed on the Pt working electrode. The origin of this film formation and its potential towards CO₂ reduction was further investigated and will be described in great detail in the chapter *Heterogeneous electro catalysis*.

For a detailed comparison of the two compounds 1-1 and 1-3 see Figure 5.9(b). Here only the reductive current of compound 1-1 (red line with circles) compared to compound



(a) Cyclic Voltammograms of 1-2



(b) Cyclic Voltammograms of 1-4

Figure 5.8: (a) Cyclic Voltammograms of 1-2 in nitrogen (black line with squares) and CO_2 (red line with circles) saturated electrolyte solution. Scan with CO_2 saturation shows a large current enhancement due to a catalytic reduction of CO_2 to CO. Measurements are taken at a scan rate of $100 \,\mathrm{mVs^{-1}}$ in acetonitrile with TBAPF₆ (0.1 M), Pt working electrode, Pt counter electrode, and a catalyst concentration of 1 mM. A scan with no catalyst present under CO_2 (blue dotted line) shows negligible reductive current. (b) Cyclic Voltammograms of 1-4 in nitrogen (black line with squares) and CO_2 (red line with circles) saturated electrolyte solution. Scan with CO_2 saturation shows a large current enhancement due to a catalytic reduction of CO_2 to CO. Measurements are taken at the same conditions and concentrations as for compound 1-2.



(b) Compound 1-1 compared to compound 1-3

Figure 5.9: (a) Cyclic Voltammograms of 1-3 in nitrogen (black line with squares) and CO₂ (red line with circles) saturated electrolyte solution. Scan with CO₂ saturation shows a large current enhancement due to a catalytic reduction of CO₂ to CO. Measurements are taken at a scan rate of $100 \,\mathrm{mVs^{-1}}$ in acetonitrile with TBAPF₆ (0.1 M), Pt working electrode, Pt counter electrode, and a catalyst concentration of 1 mM. A scan with no catalyst present under CO₂ (blue dotted line) shows negligible reductive current. (b) Reductive current of compound 1-1 (red line with circles) compared to compound 1-3 (black line with squares) under CO₂ in saturated electrolyte solution. The second reduction wave of compound 1-3 occurs at ca. 300 mV more positive potential compared to compound 1-1.

1-3 (black line with squares) under CO_2 in saturated electrolyte solution are shown. One can clearly see, that the second reduction wave of compound 1-3 occurs at ca. 300 mV more positive potential compared to compound 1-1.

Different to the compound materials 1-1 to 1-3, compound 1-4 was poorly soluble in acetonitrile. Therefore, cyclic voltammograms were measured in dimethylformamid (DMF). Figure 5.8(b) shows the corresponding cyclic voltammograms of compound 1-4 recorded in N₂- and CO₂-saturated DMF solution. Due to the extended ligand of this compound, the redox characteristics are much more diverse compared to above presented measurements of the more simple compounds 1-1 to 1-3. Within the potential of 0 to -1800 mVvs.NHE, 4 distinct reversible reduction peaks can be found with their half-wave potential (E_{1/2}) at - 635, -1020, -1250 and -1500 mVvs.NHE. Since it is generally known for rhenium compounds with bipyridine ligands that a metal-center based reduction shows an irreversible behaviour, these peaks might be attributed to a ligand based reduction. Further studies would be necessary to fully clarify their true nature. Different to the other compounds 1-1 to 1-3 the cyclic voltammogram of compound 1-4 did not reveal catalytic current enhancement within the measured potential range when the electrolyte solution was saturated with CO₂. The recorded current enhancement can be attributed to the additional background current as can be seen from the scan with no catalyst present (blue dotted line).

Figure 5.6 and 5.7 show a crossing of cathodic and anodic currents at around -1300 mV vs NHE under CO₂. This trace crossing observed for compound 1-1 indicates the occurrence of a chain process where a species, which is easier reduced than the initial compound, is continuously produced and reduced at the electrode until the trace crossing disappears. This phenomenon has been previously observed and quantitatively interpreted for cyclic voltammetry measurements of electrocatalytic reduction processes.[80, 81, 82]

For the catalyst compound 1-1 one possible explanation for this trace crossing is the formation of a dimer species in lack of sufficient CO_2 present which then can be further reduced to a dimer-anion.[47, 83, 79] These predictions agree with the experimental observations that trace crossing is enhanced with increasing catalyst concentration, compare Figure 5.10(a), and with lower scan rates, compare Figure 5.10(b).

The speed of the CO_2 reduction reaction is an important measure for the capability of a homogeneous catalyst. Comparison between various compounds is generally given by the rate constant k. To define k of the catalyst, usually rotating disk experiments are applied to determine the diffusion coefficient of the complex.[42] For this one can use the Levich equation to calculate the diffusion coefficient according to equation 5.1.[37]

$$i_L = (0.62)nFAD^{2/3}\omega^{1/2}\nu^{-1/6}C \tag{5.1}$$

Where i_L is the Levich current from the rotating disk experiment, n is the number of electrons, F is the Faraday constant, A is the electrode area, D is the diffusion coefficient, ω is the rotation rate, ν is the kinematic viscosity of the solution and C is the concentration of the analyte in solution.



(a) Compound 1-1 at different concentrations



(b) Compound 1-1 at different scan rates

Figure 5.10: (a) Cyclic voltammograms of 1-1 in CO_2 saturated electrolyte solution with different catalyst concentrations. Voltammograms are recorded at $100 \,\mathrm{mVs^{-1}}$ using a Pt working electrode, a Pt counter electrode and a Ag/AgCl quasi reference electrode. Trace crossing is enhanced with increasing catalyst concentration. (b) Cyclic voltammograms of 1-1 in CO_2 saturated electrolyte solution at different scan rates. Voltammograms are recorded using a Pt working electrode, a Pt counter electrode and a Ag/AgCl quasi reference with increasing catalyst concentration. Trace crossing is enhanced with electrolyte solution at different scan rates. Voltammograms are recorded using a Pt working electrode, a Pt counter electrode and a Ag/AgCl quasi reference electrode. Trace crossing is enhanced with decreasing scan rate.

The catalytic rate constant (k) can then be extracted from equation 5.2 which holds true for a reversible electron-transfer process followed by a fast catalytic reaction.[84]

$$i_C = nFA[cat]\sqrt{Dk[Q]^y} \tag{5.2}$$

Where i_C is the catalytic current, [cat] is the catalyst concentration, [Q] is the concentration of the substrate (in this case CO₂), y is the order of the substrate in the reaction in question and the other parameters are the same as in equation 5.1.

However, since rotating disk experiments are usually difficult to obtain, a combination of equation 5.2, for the catalytic current, and equation 5.3, for determining the peak current i_P of a compound with a reversible electron transfer and without any following reaction, can be elegantly used to obtain a good estimate for k simply from cyclic voltammetry measurements.

$$i_P = (0.466)n^{3/2}FA[cat]\sqrt{\frac{DF\nu}{RT}}$$
(5.3)

Where ν is the applied scan rate and the other abbreviations have their described meaning.[37] The ratio of i_C to i_P will then yield equation 5.4, where the diffusion coefficient cancels out and hence k can be estimated knowing i_C and i_P .[85]

$$\frac{i_C}{i_P} = \frac{1}{0.466} \sqrt{\frac{RT}{nF}} \sqrt{\frac{k[Q]^y}{\nu}}$$
(5.4)

The units of k depends on the order of reaction. The homogeneous CO_2 reduction to CO with the compounds 1-1 to 1-4 proceed via a second-order type of reaction resulting in a rate constant k with the units of $M^{-1}s^{-1}$ or $L \mod^{-1}s^{-1}$.[86]

Given the above equation 5.4, detailed analysis of the cyclic voltammogram data as presented in the Figures 5.6 to 5.9(a) allows to estimate the second order rate constant for the CO₂ reduction. Using for example the value of 2.1 for the ratio of i_C to i_P measured for compound 1-1 in equation 5.4 yields in a rate constant of about 60 M⁻¹s⁻¹ which is in good agreement to reported literature values.[42] Applying the same method to the other compounds 1-2 and 1-3 gives a rate constant of about 170 M⁻¹s⁻¹ for compound 1-2 and a rate constant of about 220 M⁻¹s⁻¹ for compound 1-3.

5.2 Rhenium compounds with bis (arylimino) acenaphthene

While for CO_2 reduction up to know mainly polypyridine derivatives have been used as 1,2dimines, related compounds with chelating imino groups that are not part of a heterocyclic aromatic system were largely neglected. A very attractive example for such a class of ligands are bis(arylimino)acenaphthene derivatives (BIAN-R), which can reversibly store up to four electrons upon reduction and could therefore introduce beneficial effects for accelerating the required multielectron transfer catalysis.[25, 87, 88, 89] In this section the successful application of Re(BIAN-R)(CO)₃Cl complexes as efficient new catalysts for the reduction of carbon dioxide is described.



Figure 5.11: Schematic chemical structures of three different rhenium compounds with bis(arylimino)acenaphthene derivatives (BIAN-R) ligands (2-1) (2-2) and (2-3) for CO₂ reduction.

Scheme 5.11 in this section shows the schematics of three different $\text{Re(BIAN-R)(CO)}_3\text{Cl}$ compounds (2-1 to 2-3) that have been used as novel materials for the aim of CO₂ reduction. To investigate the redox properties of these compounds 2-1 to 2-3 cyclic voltammograms were recorded using a one compartment cell consisting of a three electrode setup, working,

reference and counter electrode. Additionally voltammograms were recorded under CO_2 saturated electrolyte solution to investigate the activities of these compounds towards their capability for CO_2 reduction.



Figure 5.12: Cyclic voltammograms of 2-3 in nitrogen saturated electrolyte solution with two different scan rates of $50 \,\mathrm{mVs^{-1}}$ (blue line with triangles) and $100 \,\mathrm{mVs^{-1}}$ (black line with slashed triangles) respectively. Measurements are taken in acetonitrile with TBAPF₆ (0.1 M), Pt working electrode, Pt counter electrode, and a catalyst concentration of 1 mM.

Figure 5.12 shows the cyclic voltammograms of compound 2-3 measured in N₂ saturated acetonitrile solution for 50 and 100 mVs⁻¹, respectively. The compound displays four distinct reduction peaks at around -250, -500, -950 and -1300 mV(vs. NHE). The first two are reversible in nature while the last two are partly reversible. The reduction and oxidation of peak 1 and 2 around -250, -500 mV(vs. NHE) displays some characteristic features for a homogeneous, one electron transfer reaction. The peak maxima are separated by approximately 59 mV and the positions of the peak voltage do not change as a function of voltage scan rate. Furthermore the ratio of the peak currents is close to one. Additionally, the peak height scales with a square root dependence on the scan rate suggesting a diffusion controlled process with fast electron transfer as predicted by the Randles–Sevcik equation.[38] The behavior of the last two reduction peaks around -950 and -1300 mV(vs. NHE) is considerably different.

Figure 5.13(a) shows a comparison of the redox behavior of compound 2-3 between nitrogen and carbon dioxide saturated acetonitrile solution. In carbon dioxide saturated solution (Figure 5.13(a), red curve), compound 2-3 shows a strong enhancement in current density after the 4th irreversible reduction wave at about -1600 mV(vs.NHE) compared to the situation under N₂ saturation (Figure 5.13(a), black curve). This enhancement in current is proven to be the catalytic reduction of carbon dioxide to carbon monoxide and is assumed to proceed in aprotic solvents according to reaction 1.2 and in protic solvents



(b) Cyclic Voltammograms of 2-3

Figure 5.13: (a) Cyclic Voltammograms of 2-3 in nitrogen (black line with squares) and CO₂ (red line with circles) saturated electrolyte solution. Scan with CO₂ saturation shows a significant current enhancement due to a catalytic reduction of CO₂ to CO. Measurements are taken at a scan rate of 100 mVs⁻¹ in acetonitrile with TBAPF₆ (0.1 M), Pt working electrode, Pt counter electrode, and a catalyst concentration of 1 mM. A scan with no catalyst present under CO₂ (blue dotted line) shows negligible reductive current. (b) Cyclic voltammograms of 2-3 in CO₂ (red line with circles) saturated electrolyte solution and acetonitrile with 2% of H₂O added (blue line with squares). Scan with H₂O added shows a substantial higher reductive current due to an enhanced catalytic reduction of CO₂ to CO and additional H₂O reduction to H₂. Measurements are taken at a scan rate of 50 mVs⁻¹ in acetonitrile with TBAPF₆ (0.1 M), glassy carbon working electrode, Pt counter electrode, and a catalyst concentration of 1 mM.

according to reaction 1.4. The first four reduction waves at around -250, -500, -950 and -1300 mV(vs. NHE) do not show a significant increase in current density and are hence not participating in the catalytic reaction directly. The formation of the reduction product CO from CO₂ has been verified after constant potential electrolysis at -1800 mV(vs. NHE) by GC headspace analysis and additionally with an independent method of gas FTIR absorption measurement as shown in Figure 5.15.

Although well studied in the past for similar Re-based catalysts compounds presented herein, the catalytic cycle for electrochemical carbon dioxide reduction of our new compound 2-3 (and the similar compound 2-2) is still not fully understood and under current investigation. However, it is known that for Re-bipy based catalysts like $(2,2'-bipyridyl)Re(CO)_3Cl$ the catalytic mechanism needs an empty coordination site for carbon dioxide binding, which is identified to proceed via the loss of the halide (Cl^-) . For the Re-bipy based system detailed studies on this mechanism have been carried out initially by Sullivan et al.[47] and Lehn et al.[43] in 1985 and 1986, respectively. A more recent study on this was carried out by Johnson et al. in 1996 reviewing several proposed mechanisms.[79] Electrochemical studies and product gas analysis up to know suggest that the catalytic cycle of our new compound 2-3 (and 2-2) proceed in a similar way.

Figure 5.14(a) shows a comparison of the redox behavior of compound 2-2 between nitrogen and carbon dioxide saturated acetonitrile solution. In carbon dioxide saturated solution (5.14(a), red curve), compound 2-2 shows (similar to compound 2-3) a strong enhancement in current density after the 4th irreversible reduction wave at about -1600 mV(vs. NHE)compared to the situation under N₂ saturation (5.14(a), black curve). While otherwise complete similar in its redox behavior compared to compound 2-3 it is interesting to notice that for compound 2-2 the first reduction peak at around -250 mV(vs. NHE) vanishes under CO₂ saturated acetonitrile solution as can be seen in Figure 5.14(a) (red curve). The reason for this is not fully understood up to now.

Figure 5.14(b) shows a comparison of the redox behavior of compound 2-1 between nitrogen and carbon dioxide saturated acetonitrile solution. Different to the other compounds 2-3 and 2-2 presented herein, compound 2-1 does now show any catalytic current enhancement in a carbon dioxide saturated solution (Figure 5.14(b), red curve). Since the compound 2-1 is in structure completely similar to the other compounds 2-3 and 2-2 except its ligand structure on the phenyl rings, the difference in its redox behavior towards its capability of CO₂ reduction can be attributed to this difference on the ligand of the chelating imino groups that are not part of a heterocyclic aromatic system. This would suggest that for any similar type of compound the capability for CO₂ reduction is greatly influenced by its ligand structure.

Figure 5.13(b) shows a comparison of the redox behavior of compound 2-3 when 2 % of H₂O are added to a carbon dioxide saturated acetonitrile solution. In the pure carbon dioxide saturated solution (Figure 5.13(b), red curve), the behavior towards CO₂ reduction is similar to the situation presented in Figure 5.13(a). If water is added to the acetonitrile solution (Figure 5.13(b), blue curve) compound 2-3 shows a substantial further enhancement in current density after the 4th irreversible reduction wave at about -1600 mV(vs. NHE).



(b) Cyclic Voltammograms of 2-1

Figure 5.14: (a) Cyclic Voltammograms of 2-2 in nitrogen (black line with squares) and CO₂ (red line with circles) saturated electrolyte solution. Scan with CO₂ saturation shows a significant current enhancement due to a catalytic reduction of CO₂ to CO. Measurements are taken at a scan rate of $100 \,\mathrm{mVs^{-1}}$ in acetonitrile with TBAPF₆ (0.1 M), Pt working electrode, Pt counter electrode, and a catalyst concentration of 1 mM. A scan with no catalyst present under CO₂ (blue dotted line) shows negligible reductive current. (b) Cyclic Voltammograms of 2-1 in nitrogen (black line with squares) and CO₂ (red line with circles) saturated electrolyte solution. Scan with CO₂ saturation shows no significant current enhancement under CO₂ saturation. The measurement conditions and concentrations were otherwise the same as in (a)

This enhancement in the reductive current can be attributed to an enhanced catalytic activity towards CO_2 reduction to CO following reaction 1.4 and additionally to the reduction of H_2O to H_2 . The formation of both reduction products (CO and H_2) have been verified by GC headspace analysis.



Figure 5.15: Headspace gas analysis after potentiostatic CO_2 -electrolysis experiment of 2-3 at constant -1850 mV(vs.NHE) (a) GC measurements of the headspace gas for electrolysis experiment performed in acetonitrile solution saturated with CO_2 (red solid line) and acetonitrile solution saturated with CO_2 with 2% H₂O added (blue solid line). For comparison, the calibration gas containing 1 vol% of CO (black dashed line) and (b) FTIR difference absorption spectra in transmission mode of the headspace gas for electrolysis experiment performed in acetonitrile solution saturated with CO_2 . (The two peaks centered around 2143 cm⁻¹ correspond to the infrared active vibration of CO)

For a direct proof of the catalytic CO_2 reduction capability of compounds 2-3, headspace gas samples were taken and analyzed regarding the CO concentration by using GC and FTIR as an independent and complementary technique. Figure 5.15 shows the measurements of headspace gas analysis after a potentiostatic CO_2 -electrolysis experiment of 1mM 2-3 containing electrolyte solution at constant -1850 mV(vs. NHE). In Figure 5.15(a) GC measurements of the headspace gas after approximately 10000 seconds electrolysis experiment performed in acetonitrile solution saturated with CO_2 (red solid line) and acetonitrile solution saturated with CO_2 with 2 % H₂O added (blue solid line) are depicted. Additionally, for comparison, a measurement using a standard calibration gas containing 1 vol% of CO (black dashed line) is shown. In Figure 5.15(b) FTIR difference absorption spectra in transmission mode was used to analyze the headspace gas after an electrolysis experiment performed in acetonitrile solution saturated with CO_2 . The two peaks centered around 2143 cm⁻¹ correspond to the infrared active rotational-vibrations of the P and R branch of gaseous CO.

For a detailed analysis on the efficiency of the CO_2 reduction process demonstrated by our new compounds 2-3 and 2-2 controlled potential electrolysis were carried out for compound 2-3 and are assumed to be similar for compound 2-2 respectively. Different to the



Figure 5.16: Production of CO vs. time plot for potentionstatic CO₂-electrolysis experiment of 2-3 at constant -1850 mV(vs.NHE) performed in acetonitrile solution saturated with CO₂ (black triangles) and acetonitrile solution saturated with CO₂ with 2 % H₂O added (black squares) for an electrolysis time of 10000 s. Additionally the corresponding Faradaic efficiencies are shown in blue symbols (triangles for pure ACN and squares for ACN with 2 % H₂O).

cyclovoltammograms, controlled potential electrolysis experiments were performed using an H-cell setup with separated anode and cathode compartment in order to avoid re-oxidation of the formed products on the counter electrode.

Figure 5.16 shows the production of CO by the catalytic reduction of CO₂ of compound 2-3 over an electrolysis period of approximately 10000 seconds for a pure CO₂ saturated acetonitrile solution (black triangles) and a CO₂ saturated acetonitrile solution containing 2 % of H₂O (black squares). Furthermore, the calculated Faradaic efficiencies for the CO formation are depicted for the water free (blue slashed triangles) and water containing (blue slashed squares) CO₂ electrolysis measurements. In either case the CO production increases over the measurement period of 10000 seconds. However, as already indicated in the cyclovoltammograms of Figure 5.13(b), in the presence of H₂O the formation of CO is greatly enhanced.

Faradaic efficiencies for the water free system range from around 31 % after 6000 seconds to 24 % after 10000 seconds of electrolysis time. In the water containing system Faradaic efficiencies are noticeably less ranging from approximately 24 % after 4000 seconds electrolysis time to 22 % after 10000 seconds of electrolysis time. This significant difference for the faradaic efficiencies of CO formation can be readily understood by the production of H₂ as competing reaction in the water containing system. A similar behavior is known for the CO₂ reduction to CO of Re-bipy based catalysts like (2,2)-bipyridyl)Re(CO)₃Cl. For this type of systems it has been reported that with an addition of 10 % H₂O to the acetonitrile solution a maximum of CO formation can be reached decreasing again with higher amounts of H₂O added.[78] In summary, the electrocatalytic properties of rhenium(I) tricarbonyl complexes carrying bis(arylimino)acenaphthene (BIAN) ligands have been tested and characterized for the selective two-electron reduction of CO_2 to CO in homogeneous solution. It could also be demonstrated that a variation of the ligand substitution pattern in close proximity to the metal center has a very significant influence on the catalytic performance of these systems. This results are intended for publication. Further studies on the suitability of this deeply colored and readily tunable class of compounds[53, 25] as functional components of photocatalytic CO_2 -reduction cycles are currently underway.

5.3 Pyridinium and pyridazinium as catalyst

As one more example of homogeneous catalysis the pyridinium-catalyzed reduction of CO_2 to methanol reported in this context first by Bocarsly et.al. [30] is investigated in this section. Bocarsly and his group reported the reduction of carbon dioxide to methanol and formic acid on a platinum electrode in aqueous solutions containing pyridinium ions with faradaic efficiencies up to 20 % according to the mechanism presented in Scheme 5.17.

$$+3$$

$$+ 2H^{+} H^{+}$$

$$+ 2H^{+} H^{+}$$

$$+ 1e^{-}$$

$$+ 1e^{-}$$

$$+ 5e^{-}$$

$$+ H^{+} OH$$

$$+ 4 N^{+} + H^{0}$$

$$+ H^{0}$$

Figure 5.17: Proposed mechanism for the pyridinium-catalyzed reduction of CO_2 to methanol by Bocarsly et.al. [30]

The study proposed a detailed mechanism of the reduction proceeding through various coordinative interactions between the pyridinium radical and carbon dioxide, formaldehyde, and additional related species. In the ongoing work several studies have been reported where pyridinium ions were successfully used as catalyst materials towards CO_2 reduction.[90, 91, 92] Additionally a comparative study between pyridine and imidazole was reported which further explored the chemistry of the electrocatalytic reduction of CO_2 using nitrogen containing heteroaromatic systems.[93] Following this reports the proposed mechanism and the role of pyridinium as an active catalyst material lead to an ongoing discussion in chemistry. Especially quantum chemical calculations were carried out to investigate the

5.3. PYRIDINIUM AND PYRIDAZINIUM AS CATALYST

proposed mechanism and showed that the calculated acidities and redox potentials indicate that pyridinium cations behave differently than previously reported.[94] In a very recent study Saveant et. al. reported that no trace of methanol or formate could be detected upon preparative-scale electrolysis of CO_2 on the same system using pyridinium ions as active catalyst materials.[95]

Following the discussion electrochemical studies using the initially reported system with pyridinium ions as catalyst material in a homogenous aqueous solution and platinum as working electrode material was carried out. The obtained results from cyclic voltammetry studies were compared to a similar heteroaromatic system, pyridazine, containing two nitrogen atoms in the aromatic ring. Although apparently similar in structure, the two systems inherit a strong difference in their pKa value with 5.14 for pyridine and 2.10 for pyridazine.[96] The different pKa values should result in a significant shift of the acid dissociation equilibrium to regenerate the hydrated protons for the two systems under investigation.



Figure 5.18: Schematic chemical structures of the two different catalyst materials pyridine (1) and pyridazine (2) in pristine and protonated form as pyridinium and pyridazinium

Figure 5.18 shows the schematic chemical structures of the two different catalyst materials pyridine (1) and pyridazine (2) in pristine and protonated form as pyridinium and pyridazinium. Additionally bulk CO_2 electrolysis experiments and product analysis were carried out for both substances. A comparative study for the electrochemical characterization of pyridine and pyridazine and its application towards the reduction of CO_2 to methanol by bulk electrolysis experiments of CO_2 and product analysis by liquid gas and ion chromatography was carried out.

In previous studies mainly NMR spectroscopy with water suppression was used for the detection of methanol as reduction product. Reports showed different results.[30, 95, 32] In this study liquid gas chromatography of the bulk electrolyte solution was used for methanol detection and ion chromatography for the detection of formic acid during bulk electrolysis experiments at constant potential.

Figure 5.19 shows in (a) the cyclic voltammograms of 50 mM pyridine in an aqueous solution of 0.5 M KCl at pH 5.3 and in (b) CVs of 50 mM pyridazine in an aqueous solution of 0.5 M KCl at pH 4.7. recorded under a N_2 atmosphere at a Pt working electrode. The experiments within the potential range between 0 and -850 mVvs. SCE revealed a one



(a) Cyclic voltammograms of 50 mM pyridinium



(b) Cyclic voltammograms of 50 mM pyridazinium

Figure 5.19: (a) Cyclic voltammograms of 50 mM pyridine in an aqueous solution of 0.5 M KCl at pH 5.3 and (b) CVs of 50mM pyridazine in an aqueous solution of 0.5 M KCl at pH 4.7. Voltammograms are recorded under a N₂ atmosphere at a Pt working electrode. The scan rates shown are 5, 10, 25, 50, and 100 mVs⁻¹. Inset: Linear dependence of the cathodic and anodic peak current vs. the square root of the scan rate from 5 to 100 mVs^{-1} . [Measurements were done by C. Enengl and S. Enengl]

quasi-reversible reduction wave centered at -600 mVvs. SCE. The linear dependence of the cathodic and anodic peak current with the square root of the scan rate from 5 to 100 mVs^{-1} (R^2 cathodic 0.995, R^2 anodic 0.993), as can be seen in the inset of Figure 5.19(a) and (b), indicates a diffusion limited electrochemical reaction following the Randles-Sevcik equation.[38]

Although both experiments were carried out with identical catalyst concentrations, the electrochemical current response for pyridinium is found to be 75 times higher compared to pyridazinium. This would be in agreement with the mechanism suggested by Saveant et. al. where the reduction of pyridinium is following a reduction of the hydrated protons generated by the rapid dissociation of the pyridinium ions. Since the pKa value of pyridazine is 2.10, the acid dissociation to remain at equilibrium for the regeneration of hydrated protons is less dominant in the cyclic voltammetry measurements, compared to pyridine with a pKa of 5.14.

Figure 5.20 shows the cyclic voltammograms of 50 mM pyridine in an aqueous solution of 0.5 M KCl at pH 5.3 (a) and CVs of 50 mM pyridazine in an aqueous solution of 0.5 M KCl at pH 4.7 (b). The voltammograms are recorded under CO₂ atmosphere for scan rates of 10 and 25 mVs⁻¹ respectively. Compared to the situation under N₂ saturation a clear current enhancement in the presents of CO₂ is observed for both systems. For the experiment with pyridinium, the current density increased by a factor of 1.3, from initially -3.8 mA cm⁻² under N₂ to -5 mA cm⁻² under CO₂ saturation. For the experiment with pyridazinium, the current density increased by a factor of 5, from initially -0.05 mA cm⁻² under N₂ to -0.25 mA cm⁻² under CO₂ saturation. This current enhancement is either attributed to the reduction of CO₂ to methanol by a chain mechanism over several pyridinum radicals, as proposed by Bocarsly et. al.[30] and/or, as Saveant et. al. concluded [95], is simply due to the superposition of the contributions of the two acids present, namely the pyridinium and CO₂ in water.

Similar experiments were carried out with different working electrode materials changing from platinum to glassy carbon, gold and copper, however none of the later showed any noticeable electrochemical response in the applied potential range from 0 to - 800 mV vs. SCE. This characteristic is in agreement with previously reported results showing the important role of platinum in the overall reaction mechanism.[30, 94] In a recent work Musgrave et. al.[97] employed quantum chemical calculations to investigate the role and mechanism of pyridinium based CO_2 reduction. Results indicate a strong binding interaction of pyridinium with the electrode surface of platinum, resulting in an adsorption energy of 1.0 eV/molecule on Pt(111). It was further concluded that this strong binding interaction of pyridinium with Pt(111) significantly lowers its heterogeneous reduction potential.

Figure 5.21 shows the dependence of the catalytic peak current under CO_2 saturation for different pyridinium and pyridazinium concentrations of 5, 10, 25, 50, 70 and 100 mM respectively. For both catalyst materials the peak current increases with increasing catalyst concentration. For the case of pyridinium as catalyst however, the peak current increases significantly stronger, namely by a factor of 9.2 between a concentration of 5 mM and 100 mM. For the same concentration increase, under otherwise identical conditions, the peak



(a) Cyclic voltammograms pyridinium



(b) Cyclic voltammograms pyridazinium

Figure 5.20: (a) Cyclic voltammograms of 50 mM pyridinium in an aqueous solution of 0.5 M KCl at pH 5.3 recorded under N_2 (black line with squares) and CO_2 (red line with circles) atmosphere and (b) 50mM pyridazine in an aqueous solution of 0.5 M KCl at pH 4.7. Measurements are recorded at a Pt working electrode and a scan rate of 25 mVs⁻¹. [Measurements were done by C. Enengl and S. Enengl]



(a) Catalytic peak current under CO_2 for pyridinium



(b) Catalytic peak current under CO_2 for pyridazinium



(c) Ratio of current measured under a CO_2 to N_2 for pyridazinium

Figure 5.21: Dependence of the catalytic peak current under CO_2 saturation on different pyridinium and pyridazinium concentrations (5, 10, 25, 50, 70 and 100 mM). All measurements were taken at 100 mV s⁻¹ in an aqueous solution of 0.5 M KCl and a pH 5.3 for the measurements with pyridinium (a) and pH 4.7 (b) for the measurements with pyridazinium. (c) Dependence of the catalytic peak current, depicted as the ratio of current measured under a CO_2 atmosphere normalized to the current measured under an N₂ atmosphere in a pH-adjusted solution and increasing pyridazinium concentrations. current of the pyridazinium catalyst increases only 1.6 fold, showing that the material is less active towards catalytic CO_2 reduction. When the peak current of pyridazinium under CO_2 saturation is normalized to the peak current under N_2 , the peak current ratio decreases with increasing pyridazinium concentration reaching a quasi-constant current ratio of about 3.4 at about 50 mM, compare Figure 5.21(c) in the supplementary information. This is different to the reported behavior of the concentration dependence measured for pyridinium and imidazole, where the current ratio increased, with increasing concentration until the current ratio plateaus. In literature it was concluded that the plateau in current is due to a saturation of active surface-sites.[91, 93] In the case of pyridazinium this characteristic is more indicative of a CO_2 independent increase in base current due to pyridazinium reduction.

A critical experiment to decide on the catalytic reduction of CO_2 is bulk electrolysis followed by product analysis. Several electrolysis experiments for a 50 mM Pyridinum and Pyridazine solution were carried out with initial saturation of the solution by bubbling with CO_2 . In both cases controlled potential electrolysis were carried out over an extended period of 30 hours.

Figure 5.22 shows the current-time curve for the constant potential electrolysis experiment of 50 mM pyridine in an aqueous solution of 0.5 M KCl at pH 5.3 (a) and for comparison of 50mM pyridazine in an aqueous solution of 0.5 M KCl at pH 4.7 (b) over an electrolysis time of 16 hours. The data shown in Figure 5.22 correspond to the experimental data shown in the product analysis for methanol depicted in Figure 5.23 in the subsequent information. Current time measurements under CO_2 saturation (red solid line) and N_2 saturation (black solid line) are shown for both compounds. The experiment reveals, that there are only minute differences between the current under CO₂ and N₂ saturation for both catalyst materials respectively, which leads to the conclusion that a substantial amount of current is attributed to side reactions despite CO_2 reduction. Such a system is expected to demonstrate only low faradaic efficiencies. This experiment has been repeated for both compounds several times showing similar results. (The initial current increase in the case of pyridinium under N_2 saturation and pyridazinium under CO_2 saturation at the beginning of the measurement is not understood up to know. It is expected to be a characteristic of the experimental setup however, rather than of the catalyst material.) The noise in the current-time characteristics is attributed to the formation of hydrogen bubbles on the working electrode.

Figure 5.23 shows the liquid GC analysis of the electrolyte solution during constant potential electrolysis. The figure on the left side shows measurements of a 50 mM and 10 mM pyridinium concentrated solution in an aqueous 0.5 M KCl at pH 5.3 (a). For both concentrations, samples were taken after 30 hours of electrolysis time at - 800 mV vs. SCE. The measurements show, that for increasing pyridinium concentrations, the production of methanol increases going from 1.7 ppm CH₃OH for the 10 mM concentration to 1.9 ppm for the 50 mM concentration. The corresponding Faraday efficiencies are $9(\pm 1)$ and $14(\pm 1.5)$ % respectively and are hence lower than originally reported Faraday efficiencies for this system of about 22 %.[30] A standard for 12.5 ppm CH₃OH in 0.5 M KCl is also shown in Figure 5.23(a), black solid line.

In comparison on the right side of Figure 5.23, liquid GC analysis of a 50 mM pyri-


(a) Current-time measurements pyridinium



(b) Current-time measurements pyridazinium

Figure 5.22: Current-time measurements for the constant potential electrolysis experiment of 50 mM pyridine at - 750 mV vs. SCE in an aqueous solution of 0.5 M KCl at pH 5.3 (a) and of 50mM pyridazine at - 650 mV vs. SCE in an aqueous solution of 0.5 M KCl at pH 4.7 (b). Current time measurements under CO_2 saturation (red line) and N_2 saturation (black line). [Measurements were done by C. Energl and S. Energl]



(a) GC analysis for pyridinium electrolysis



(b) GC analysis for pyridazinium electrolysis



(c) GC analysis for pyridazinium kept at 6°C

Figure 5.23: GC analysis of the electrolyte solution during constant potential electrolysis for pyridinium and pyridazinium. (a) Measurements after 30 hours of CO_2 electrolysis at - 800 mV vs. SCE in an aqueous solution of 0.5 M KCl with 50 (red solid line) and a 10 mM (red dashed line) pyridinium concentration at pH 5.3. (b) GC analysis of 50 mM pyridazine in an aqueous solution of 0.5 M KCl at pH 4.7 for 19 and 30 hours of electrolysis time at constant - 650 mV vs. SCE. (c) Samples from the experiment in (b) taken during electrolysis and kept at 6°C for 24 hours before the measurement

dazinium solution in an aqueous 0.5 M KCl at pH 4.7 are shown for 19 and 30 hours of electrolysis time at constant - 650 mV vs. SCE. The corresponding methanol concentrations are 0.2 ppm and 0.3 ppm respectively, corresponding to Faraday efficiencies of about $2(\pm 0.5)$ and $3.6(\pm 0.5)$ %. For comparison a 1 ppm methanol standard in water is also shown (Figure 5.23(b), black line). The retention time for the methanol peak maximum was in all measurements typically at 2.07 min. If one compares this low faradaic efficiencies with the strong current enhancement in the cyclic voltammetry studies between N₂ and CO₂ saturated systems it is noticeable that CO₂ reduction to methanol is only partly responsible for the observed current increase as proposed by Bocarsly et. al.[30]. The additional current increase is expected to come from a superposition of the contributions of the two acids present, namely the pyridinium and CO₂ in water, or more dominant, the pyridazinium and CO₂ in water, as Saveant et. al. [95] concluded. The difference in the current densities can then be understood by the different pKa values of the two materials with 5.14 for pyridine and 2.10 for pyridazine.

Interestingly it was found that when the samples were stored at 6° C over several hours (e.g. 24 h for the experiment shown in Figure 5.23(c)) and measured again in GC analysis, the methanol concentration increased in all samples significantly and with it, the Faraday efficiency, compare Table 5.1 and Figure 5.23(c) in the presented information. The reason for this increase is not understood by now. Samples that were taken before the electrolysis experiment was started and held under otherwise identical conditions did not yield any methanol signal in the GC analysis. Additionally, the calibration measurement for low methanol concentrations shows excellent linearity from 1 to 50 ppm, compare Figure 2.15(b) in the experimental chapter. A detailed analysis of these measurements and the corresponding calculation of the Faraday efficiencies for methanol formation can be found in Table 5.1. Conclusions

Pyridinium				
Time	Conc. Cat.	Conc. CH ₃ OH	Coulomb	Faraday eff.
h	mM	ppm	-	%
30	50	1.93	17.3	14.3
30	10	1.79	25.1	9.2
Pyridazinium				
19	50	0.16	3.82	2.4
30	50	0.33	5.29	3.6
Pyridazinium	stored at 6°C			
24	50	0.29	4.57	3.6
28	50	0.33	5.06	3.8
44	50	0.73	6.36	6.6

Table 5.1: Summary of controlled potential electrolysis experiments shown in Figure 5.23 and the corresponding calculated Faraday efficiencies.

In this work the electrocatalytic reduction of CO_2 to methanol and formic acid is explored by the direct comparison of protonated pyridazine and pyridine. Cyclovoltammetric studies for both materials revealed a strong current increase upon CO_2 saturation. The formation of CH₃OH by bulk controlled potential electrolysis experiments could be verified by GC analysis. Faradaic efficiencies were measured with $14(\pm 1.5)$ % for the pyrdinium, and $3.6(\pm 0.5)$ % for the pyridazinium system respectively. The fact that only low faradaic efficiencies were measured although strong current enhancement in cyclic voltammetry studies from N₂ to CO₂ saturated systems were observed lead to the conclusion that CO₂ reduction to methanol is only partly responsible for the observed current increase, as proposed by Bocarsly et. al.[30]. The additional current increase, which is the dominant one, is expected to come from a superposition of the contributions of the two acids present, namely the pyridinium and CO₂ in water, or more dominant, the pyridazinium and CO₂ in water, as Saveant et. al. [95] concluded.

Chapter 6

Homogeneous photo catalysis

The fac-(2,2)-bipyridyl)Re(CO)₃Cl (1-1) is known to be an efficient photo catalyst for the reduction of CO₂ producing mainly CO with the aid of a sacrificial electron donor as for example triethanolamine (TEOA). Figure 6.1 depicts a schematic representation of such a photocatalytic CO₂ reduction system with the catalyst material indecated as (C) and the donor material (D).



Figure 6.1: Schematic representation of photocatalytic CO_2 reduction with the catalyst material (C) and the donor (D).

The quantum yield (Φ_{CO}) for CO₂ reduction of this compound 1-1 has been reported with 0.14 almost 30 years ago when first published in this context by Lehn et. al. in 1984.[43, 77] Subsequent modifications of the bipyridine ligand system of 1-1 lead to the development of superior catalysts with Φ_{CO} up to 0.59, making these type of materials the most efficient CO₂ photo-catalyst among known homogeneous catalyst materials by now.[46, 98]

In this work, the results obtained for the novel compounds (1-3) and (1-5) are compared to our previous findings for (1-1), schematic drawings of all three compounds are depicted in Figure 6.3, showing the modification of additional phenylethynyl substituents at the acceptor ligand 4,4'-position and 5,5'-position. It is expected that this substitution demonstrate an extended conjugation from the bipyridyl acceptor moiety to the central rhenium atom and



Figure 6.2: Illustration of the photochemical CO_2 reduction experiment with the light source (A), the gas tight reaction cell (B) and the FTIR measurement cell (C).

hence influence the catalyst activity towards electro- and photocatlytic CO_2 reduction.



Figure 6.3: Schematic chemical structures of three different rhenium compounds $(2,2'-bipyridyl)Re(CO)_3Cl$ (1-1), $(5,5'-bipphenylethynyl-2,2'-bipyridyl)Re(CO)_3Cl$ (1-3) and $(4,4'-bipphenylethynyl-2,2'-bipyridyl)Re(CO)_3Cl$ (1-5) investigated for photocatalytic CO₂ reduction.

For photocatalysis, it is important to extend the absorption of the catalyst compounds in the visible region. One way to address this is to covalently bind the catalyst to a photosensitizer with high absorption in the visible region. One of the best results concerning quantum yield and turnover numbers was achieved by bridging a Re-based catalyst with a Ru-based photosensitizer reported by Ishitani and coworkers. [48, 99, 100]

A important quantity for photocatalytic systems is the turn over number (TON). It is a dimensionless number and defined as the total number of turnovers the catalyst can achieve until its total decay, independent of the time involved.[101] As such it is an important



Figure 6.4: Comparison of normalized UV-Visible absorption spectra of three different rheniumcarbonyl-complexes in acetonitrile solution. (2,2'-bipyridyl)Re(CO)₃Cl (1-1), (5,5'-bisphenylethynyl-2,2'-bipyridyl)Re(CO)₃Cl (1-3) and (4,4'-bisphenylethynyl-2,2'-bipyridyl)Re(CO)₃Cl (1-5).

measure to evaluate the catalyst lifetime and robustness. Experimentally it can be found by the ratio between the amounts of products formed, if there is no limit in substrate (CO₂), divided by the amount of catalyst material in the system (mol reduced product of CO₂/mol catalyst). Typical TON for Re(bipy)(CO)₃X (X=Cl, Br) compounds are in the order of 300.[42, 43, 102]

Scheme 6.2 depicts an illustration of the photochemical CO_2 reduction experiment with the light source (A), the gas tight reaction cell (B) and the FTIR measurement cell (C). Gas samples were taken with a gas tight syringe and transferred to the specially designed FTIR gas cell for recording an IR difference absorption spectrum before and after light irradiation in transmission mode.

Figure 6.5 shows FTIR gas analysis of a photocatalytic reduction experiment of a DMF / TEOA (5:1/v:v) solution containing 2.6 mM of compound 1-1 or 1-3, respectively. The results were compared to a control experiment of the same solution kept in the dark. Headspace samples (5 ml) were taken after an irradiation time of 18 hours and analysed by FTIR spectroscopy. The spectra, as can be seen in Figure 6.5, correspond to a CO gas concentration of A 22.38 vol% and B 0.98 vol% in 5 ml sample gas. The irradiation time was 18 h under 26900 lux with an Osram 400 W Xenophot xenon lamp.

Comparing now photocatalytic CO₂ reduction experiments applying compound 1-1 and 1-3 it was found that the reduction in DMF/TEOA (5:1/v:v), similar to previous works of Koike and coworkers [46], shows big differences in reaction efficiency. As has been reported by other groups before, compound 1-1 showed a good photocatalytic activity with a quantum yield in the range of $\varphi = 0.167$. In later experiments with the new catalyst 1-3, a significantly



Figure 6.5: IR difference absorption spectra (transmission mode) of headspace samples after illumination (red line with circles) of a DMF:TEOA (5:1/v:v) solution with 2.6 mM catalyst concentration. Control dark experiments are also shown (black line with squares). A, compound 1 and B, compound 2. Light intensity 26900 lux, 360 nm low pass cutoff filter, irradiation time 18 hours.

lower performance in the generation of CO was reported under similar conditions. In our experiment the new catalyst 1-3 showed a 22.8 fold lesser generation of CO under the same conditions as 1-1. Taking this into account, our best estimate for the quantum yield of catalyst 1-3 (above 360 nm irradiation) is in the order of 0.4 %.[39] These findings can be interpreted by analyzing the above described spectrophotometric measurements, considering the assumption that a long lived ³MLCT^{*} state is a necessary requirement for the successful application of the catalyst in a photochemical system for the reduction on CO_2 to CO.

Although the new catalysts 1-3 and 1-5 show significantly higher absorption in the visible range (compare Figure 6.4), which was assumed to be a clear benefit for photocatalytic application, however, it was shown that the experiments over several hours of irradiation yielded only very low CO formation and under identical conditions, the unmodified compound 1-1 still performs better for photocatalytic CO_2 reduction. To the best of our understanding, following quantum mechanical DFT calculations, this different behaviour might be attributed to an inversion of the lowest-lying excited state properties of compound 1-3 and 1-5 compared to the situation in compound 1-1, which is crucial for the photochemical reactivity of such systems. Such an inversion from the typical metal-to-ligand charge transfer (MLCT) character present in 1-1 to an intraligand (IL) situation was already indicated in a detailed photophysical study of the excited state deactivation pathways of complex 1-3.[50] Further efforts should therefore focus on a systematic tuning of the excited state manifold of compounds such as 1-3 in order to better control the photocatalytic performance while at the same time improving the long-wavelength sensitization of the CO_2 reduction process.[25]

Chapter 7

Heterogeneous electro catalysis

While homogeneous catalysis is easier to characterize and mechanistically better understood than heterogeneous catalysis, it also has several disadvantages. High amounts of expensive catalyst material are necessary for efficient CO_2 reduction and the system is limited to the solubility properties of the active species, which often allows only a small variety of different solvents that do not necessarily match desired high CO_2 solubility properties. Furthermore homogeneous catalysts may sometimes face solution deactivation pathways, as for example a dimer formation of Re-compounds with bipyridine ligands in non-aqueous solution systems.[47] One way to overcome these problems is to immobilize the catalyst on the electrode and thereby change from homogeneous to heterogeneous catalysis. In the past, the most frequently reported ways to immobilize Re type catalysts onto a solid electrode were either the insertion of the molecule in a polymer matrix [78, 103, 104] or the chemical modification of the ligand-molecule with a functional group allowing polymerization.

7.1 (2,2)-bipy.)Re(CO)₃Cl incorporation into a polymer matrix

A versatile technique for the immobilization of an active catalyst species is the incorporation of the catalyst material in a host polymer matrix. Yoshida et. al. successfully incorporated the $(2,2'-bipyridyl)Re(CO)_3Br$ and $(terpyridine)Re(CO)_3Br$ into a coated Nafion membrane for the reduction of CO₂ to formic acid and CO in a water based environment.[105]



Figure 7.1: Schematic representation of the electrochemical polymerization of pyrrole to polypyrrole uppon oxidation.



(c) Polypyrrole film on Pt

Figure 7.2: (a) Potentiodynamic electropolymerisation of pure Pyrrol over 70 cycles on a Pt foil by sweeping the potential between 1053 mV and -647 mVvs. NHE over 70 cycles with a scan rate of 100 mVs^{-1} . With ongoing film formation the current density increases up to a maximum until the film formation ceased. Characteristic peaks for the oxidation at 350 mVvs. NHE and at 50 mVvs. NHE for the reduction are observed. (b) Film characterization at 50 mVs^{-1} in N₂ (black line with squares) and CO₂ (red line with circles) saturated electrolyte solution. (c) Picture of the electropolymerized polypyrrole film on a Pt foil supported working electrode. [Measurements were done by S. Schlager]

7.1. (2,2'-BIPY.)RE(CO)₃CL INCORPORATION INTO A POLYMER MATRIX 83

In our approach the aim was to immobilize the catalyst material (2,2'-bipyridyl) $\text{Re}(\text{CO})_3\text{Cl}$ (1-1) into a polypyrrole matrix by electrochemical polymerization of pyrrole in a homogeneous mixture of pyrrole and the catalyst material. Figure 7.1 shows a schematic representation of the electrochemical polymerization of pyrrole to polypyrrole by oxidation. Pyrrole was electropolymerized on a Pt foil serving as supporting working electrode for the polypyrrole film. Pyrrole was used as received. 625 μ l of pyrrole were added to 18 ml of acetonitrile with TBAPF₆ (0.1 M) as supporting electrolyte to receive a monomer concentration of 0.5 M. The electropolymerisation was performed by sweeping the potential between 1053 mV and -647 mVvs. NHE over 70 cycles with a scan rate of 100 mVs⁻¹.

Figure 7.2(a) shows the potentiodynamic film formation of a pure polypyrrole film without compound 1-1 present. The successive film formation is indicated by an increase in the current density of each cycle. The film formation ceased after approximately 70 cycles when no additional current increase could be observed. After electropolymerization the Pt working electrode was fully covered with a continuous dark black film of polypyrrole, compare Figure 7.2(c). In Figure 7.2(b) the pure polypyrrole electrode on Pt was tested upon CO_2 reduction. Cyclic Voltammograms of a polypyrrole covered Pt electrode in N₂ (black line with squares) and CO_2 (red line with circles) saturated electrolyte solution are shown. The scan with CO_2 saturation shows no significant reductive current enhancement.



Figure 7.3: Cyclic Voltammograms of a polypyrole covered Pt electrode and incoporated catalyst compound 1-1 in N₂ (black line with squares) and CO₂ (red line with circles) saturated electrolyte solution. Scan with CO₂ saturation shows a significant reductive current enhancement attributed to a catalytic reduction of CO₂ to CO by the catalyst. Measurements are taken at a scan rate of $100 \,\mathrm{mVs^{-1}}$ in acetonitrile with TBAPF₆ (0.1 M) and a Pt counter electrode. Upon sequential N₂ purging the original cyclic voltammetry curve is restored (black dashed line).

In a subsequent similar experiment compound 1-1 was dissolved in the pyrrole monomer electrolyte solution with a concentration of 2 mM and used for electro polymerization. After electropolymerization at constant current of 0.1 mA the formed film was removed from the system and washed with pure acetonitrile solution to remove any initial monomer and catalyst material not incorporated into the polymer matrix. Then the polymer film was used as working electrode for heterogeneous CO_2 reduction.

Figure 7.3 shows the cyclic voltammograms of the polypyrrole covered Pt electrode and the incorporated catalyst compound 1-1 in N₂ (black line with squares) and CO₂ (red line with circles) saturated electrolyte solution. The scan with CO₂ saturation shows a significant reductive current enhancement which is assumed to be due to a catalytic reduction of CO₂ to CO by the catalyst 1-1. Measurements are taken at a scan rate of 100 mVs⁻¹ in acetonitrile with TBAPF₆ (0.1 M) and a Pt counter electrode. Upon sequential N₂ purging the original cyclic voltammetry curve is restored (black dashed line). The reduction peak at about -600 mVvs. NHE is not present in the cyclic voltammogram of the pristine film depicted in Figure 7.2(b) before and is hence attributed to the first, bipyridyl based reduction of the catalyst 1-1, compare Figure 5.6 in chapter 5.

Similar results have been reported by Chen et. al. where Cobalt-Phthalocyanine was successfully incorporated into a polypyrrole matrix for CO_2 reduction.[106]

It has to be pointed out, that in this experiments no product gas analysis was performed to independently verify the CO_2 reduction and confirm the expected CO formation. Subsequent experiments failed in reproducing this data and further studies on this effect are under current investigations.

7.2 (5,5)-bisphen.-2,2'-bipy.)Re(CO)₃Cl polymerization

This chapter investigates the electropolymerization of compound 1-3 onto the electrode and determines its potential for heterogeneous catalysis towards CO_2 reduction. The film growth on a Pt working electrode was performed by potentiodynamic reductive scanning in nitrogen saturated acetonitrile solution containing 0.1 M TBAPF₆ and the catalyst monomer with a concentration of 2 mM. The films were electrochemically characterized using cyclic voltammetry. As done before, the catalytic properties for CO_2 reduction were studied via cyclic voltammetry in carbon dioxide saturated acetonitrile solution containing also 0.1 M TBAPF₆.

Figure 7.5 shows the potentiodynamic formation of the rhenium catalyst film by electropolymerization of the rhenium catalyst monomer 1-3 on a Pt working electrode from a 2 mM monomer solution. Changes in the voltammogram with increasing number of cycles are indicated by the numbers 1 to 5 in Figure 7.5. In the first scan (red line with circles), two distinct reduction waves of the monomer 1-3 are still visible. The peak at (-850 mVvs.NHE) can be attributed to a ligand based reduction, and the reduction wave at (-1300 mVvs.NHE) can be assigned to a reduction at the metal centre. The first reduction wave is partly reversible and the re-oxidation peak appears at (-750 mVvs.NHE). Both peaks 1 and 4, attributed to the monomer ligand, decrease with increasing number of scans, which suggests a ligand-based polymerisation of the monomer 1-3. The polymerization is assumed to proceed via radical coupling between two electro-generated radical species as was reported previously for simi-



Figure 7.4: Schematic representation of the electrochemical polymerization of the monomer compound (1-3) and the resulting possible chemical substructure of the rhenium sites within the polymer film in which X represents a chloride or a substituted ligand from the reaction medium.

lar systems, [43, 107] although alternative routes cannot be excluded due to the presence of metal carbonyl species. [108] Furthermore, the maximum of the first reduction wave 1 shifts towards more negative potentials with increasing number of scans. An oxidative peak 5 at around (-100 mVvs.NHE) initially appears and disappears after continuous scanning which may be attributed to a temporary dimer formation as it is described for similar systems. After approximately 25 cycles, the voltammogram doesn't change any further and shows a distinct background current below (-700 mVvs.NHE) (blue line with triangles). This background current is present over continuous scans and indicated by 2 and 3. After formation, the polymer film shows an intense violet colour on the part of the electrode that was in contact with the monomer solution (compare Figure 7.9).

Figure 7.6 shows the electroactivity of the rhenium catalyst film on a platinum plate electrode at various scan rates from $200 \,\mathrm{mVs^{-1}}$ (blue line with triangles) to $10 \,\mathrm{mVs^{-1}}$ (red line with circles). A plot of peak current vs. scan rate reveals a linear dependence suggesting that the redox process is not any more diffusion controlled as predicted by the Randles-Sevcik equation.[37] This further confirms the formation of an electroactive film immobilized on the Pt electrode surface.[109] Additionally, the maximum reduction peak position is independent of the scan rate within the measured cycling times. This shows that the electron transfer kinetics is fast with respect to the cycling time scales suggesting a Nernst like behaviour.[38]



Figure 7.5: Potentiodynamic formation of rhenium catalyst film on Pt from a catalyst monomer solution of 1-3. First scan (red line with circles) and last scan (blue line with triangles). Voltammograms are recorded at $50 \,\mathrm{mVs^{-1}}$ in nitrogen-saturated acetonitrile solution containing 0.1 M TBAPF₆ and a monomer catalyst concentration of $2 \,\mathrm{mM}$.

Figure 7.7 shows cyclic voltammetry measurements of the rhenium catalyst film on a Pt plate electrode in N₂- and CO₂-saturated electrolyte solution. The measurement of the potential window with two Pt electrodes as WE and CE, respectively, and an electrolyte solution under N₂ does not show any reductive current in the potential range from 0 mVvs.NHE to -2000 mVvs.NHE. When the solution is purged with CO₂ for 10 min and no catalyst is present, a reductive current starts to flow at a potential lower than about -1700 mVvs.NHE (blue dashed line). When the Pt working electrode is replaced by the Pt electrode with the rhenium catalyst film and measured in the electrolyte solution under N₂ atmosphere, the typical reduction curve as shown in Figure 7.6 is measured again (Figure 7.6, black line with squares). If however the electrolyte solution is at CO₂ saturation, a high non-reversible reductive current enhancement is observed (Figure 7.6, red line with circles). The reductive current begins to increase at about -1150 mVvs.NHE and can be attributed to the reduction of CO₂ to CO.

According to previous studies on active electrodes with rhenium based catalysts, the pathway for CO_2 reduction is similar to the homogeneous system. The catalytic mechanism proceeds via coordination of a CO_2 molecule to a rhenium atom, which allows the reduction of CO_2 to CO.[47, 107, 72, 110, 111] As a result, the catalytic current per area depends on the number of active redox sites per surface area.

A comparison between the catalyst monomer 1-3 in solution (green line with triangles) and the polymerized rhenium catalyst film on a Pt plate electrode (red line with circles)



Figure 7.6: Cyclic voltammograms of the rhenium catalyst film on Pt in nitrogen saturated acetonitrile solution containing 0.1 M TBAPF_6 at different scan rates from 200 mVs^{-1} (blue line with triangles) 10 mVs^{-1} (red line with circles).

in CO₂-saturated electrolyte is presented in Figure 7.8. The measurement shows that the electrochemical potential onset for the CO₂ reduction with the rhenium catalyst film on the Pt electrode has a similar value as the onset for CO₂ reduction using the monomer substance 1-3 in solution, which is at about -1150 mVvs.NHE. The reductive current increases initially more rapidly for the homogeneous monomer system. With increasing negative potential, however, the current density at the catalyst film electrode increases significantly faster, surpassing the reductive current of the 1 mM monomer solution at about -1450 mVvs.NHE.

In contrast to the cyclic voltammogram of the rhenium catalyst film on a Pt electrode (red line with circles), the cyclic voltammogram of the catalyst monomer 1-3 in a CO₂-saturated electrolyte solution (green line with triangles) still shows the quasireversible first reduction wave at about -850 mVvs.NHE. This reduction wave is attributed to the ligand of the monomer 1-3. As known from previous experiments, this reductive peak does not show any current enhancement under CO₂- saturation compared to saturation under N₂.[72, 39]

 CO_2 -electrolysis experiments at constant -1600 mVvs.NHE of a pure platinum plate electrode and of the rhenium catalyst film was performed in acetonitrile solution saturated with CO_2 . The experiment was carried out in a sealed cell over 60 minutes of electrolysis time. During this period no film degradation was observed. Current-time plots can be found in the *Experimental techniques* section compare Figure 2.5.

As a direct proof of the catalytic CO_2 -reduction capability of the rhenium catalyst film, headspace gas samples were taken and analyzed with regard to the CO-concentration



Figure 7.7: Cyclic voltammograms of the rhenium catalyst film on a Pt plate electrode in nitrogen- (black line with squares) and CO₂- saturated electrolyte solution (red line with circles), respectively. The scan in the presence of CO₂ shows a large current enhancement due to the catalytic reduction of CO₂ to CO. A scan with no catalyst film present under CO₂ (blue dashed line) shows little to no reductive current. Voltammograms were recorded at 100 mVs^{-1} in acetonitrile with a Pt counter electrode.

using GC and FTIR measurements. Knowing the partial pressure of the CO formed, the number of molecules of CO dissolved in the electrolyte solution was estimated using Henry's Law following Equation 2.4. The Faradaic efficiency (η_F) was then calculated according to Equation 2.3.

With this approach, a Faradaic efficiency for the reduction of CO_2 to CO by the rhenium catalyst film of about 33% was calculated. The Faradaic efficiency of a 1 mM solution of the monomer catalyst 1-3 was measured to be around 43%. The control experiment with a pure platinum plate electrode under otherwise identical conditions did not yield detectable amounts of CO. Similar to the homogeneous catalysis it is likely that under these conditions (ACN:TBAPF₆) also small amounts of formate and oxalate can be formed, however with typical Faradaic efficiencies below 1%.[41]

Further characterization to determine turn over number (TON) and turn over frequency (TOF) is important. These parameters will help in determining stability and lifetime of the novel catalyst film and should be further investigated. Typical TON for $\text{Re(bipy)(CO)}_3\text{X}$ (X=Cl, Br) compounds are in the order of 300.[77, 102, 42] To determine the TON of the catalyst film, specific information on the catalytic active rhenium sites on the film would be necessary. This data however is not available at the current stage of investigation and is very difficult to obtain experimentally. As a first approximation one can assume a single homogeneous active monolayer of the catalyst film on the electrode surface. This would



Figure 7.8: Cyclic voltammograms of the rhenium catalyst film on a Pt plate electrode (red line with circles) and a 1 mM solution of the monomer 1-3 (green line with triangles) in CO₂-saturated electrolyte solution. The scan in the presence of CO₂ shows large current enhancement for both systems due to a catalytic reduction of CO₂ to CO. Voltammograms were recorded at $100 \,\mathrm{mVs^{-1}}$ in acetonitrile and a Pt counter electrode. A scan with no catalyst film present under CO₂ (blue dashed line) shows little to no reductive current.

result in a surface coverage of about $1.5x10^{-10}$ mol active rhenium-sites per cm² and is in the order of similar reported catalyst films by B.P. Sullivan and T.J. Meyer et al. in 1989.[72] Dividing now the amount of CO formed during the electrolysis experiment over 60 min by the number of estimated active rhenium sites would result in about 1400 turn overs per active site and a frequency of about 0.4 turn overs per second. These values seem to be reasonable, since it is known from literature that electro-polymerized rhenium catalysts execute about 30 times more turnovers per site than their monomer counterparts in solution.

Figure 7.9(b) shows a comparison of the absorption spectra of a dilute solution of the monomer 1-3 in acetonitrile and of the rhenium catalyst film on a platinum plate electrode. In acetonitrile, the spectrum of the monomer compound 1-3 is dominated by an intense absorption maximum at around 375 nm resulting from a strong intraligand band with additional metal to ligand charge transfer contributions. Other weaker UV-bands of intraligand origin occur between 280 nm and 320 nm. A detailed study on the nature of the electronic transitions and the photophysical behaviour of the monomer compound was published by K. Oppelt et al.[50]

After electropolymerization, the rhenium catalyst film shows a red shift in the absorption band with a maximum at around 425 nm. Compared to 1-3, this red-shift of the absorption maximum in the film of the rhenium catalyst can probably be attributed to an increased delocalization of the conjugated π -electron system upon polymerization. Though, the red shift is not as significant as observed in other conjugated polymers. Therefore the effective conjugation is probably limited to a few monomer units.



(b) UV-Vis absorption spectra

Figure 7.9: (a) Current time curve for the potentiostatic film formation in nitrogen saturated acetonitrile solution containing 0.1 M TBAPF₆ initial monomer1-3 concentration of 2 mM at a constant potential of -1550 mVvs.NHE. (b) Comparison of the UV-Vis absorption spectra of the rhenium catalyst film on a platinum plate electrode (red solid line) and of a $6.25 \cdot 10^{-5}$ M solution of the monomer 1-3 in acetonitrile (298 K, 1 cm cell, black dots) (left side). On the right side a picture of the rhenium catalyst film electropolymerized onto a Pt-plate electrode is shown.

7.2. (5,5'-BISPHEN.-2,2'-BIPY.)RE(CO)₃CL POLYMERIZATION

The polymer growth process was also investigated with an ex-situ ATR-FTIR technique. For this measurement, a ZnSe reflection element covered with a thin (10 nm) sputtered film of platinum was used as working electrode, and a 150 nm layer of the rhenium catalyst film was potentiostatically electropolymerized on the Pt-surface of the modified ZnSe ATR crystal. The experiment was performed in a one compartment electrochemical cell as depicted in the *Experimental section* in Scheme 2.13(A). The electrolyte solution contained 0.1 M TBAPF₆ initial monomer1-3 concentration of 2 mM in acetonitrile. The electrochemical cell was connected to the potentiostat and a constant potential of -1550 mVvs.NHE was applied for 500 seconds. The electrochemical current measured as function of time is presented in Figure 7.9(a). As can be seen, during film formation, the current dropped from initially -0.3 mA to approx. -0.12 mA after 400 sec. and stayed constant afterwards. This indicates that the film formation ceased at that time.

After electropolymerization, the ZnSe/Pt electrode with the 150 nm thick catalyst film was mounted into an ATR-FTIR setup between two PTFE spacers (see in the *Experimental section* in Scheme 2.13(B)) and the ATR-FTIR difference absorption spectra between a pure ZnSe/Pt electrode and the ZnSe/Pt electrode with the catalyst film were recorded.

Figure 7.10 shows the ATR-FTIR difference absorption spectrum of the 150 nm thick film of the rhenium catalyst vs. a pure ZnSe/Pt electrode and of the monomer 1-3 dissolved in dichloromethane and drop cast on a ZnSe ATR crystal vs. the pure ZnSe ATR crystal. In the spectrum of the rhenium catalyst film distinctive new peaks are observed and their peak positions are indicated by the numbers 1 to 10 in the absorption spectrum of Figure 7.10. These positions are connected with characteristic vibrations of the polymerized film. As compared to the infrared spectrum of the monomer (bottom, black solid line) there is a noticeable decrease in the intensity of the monomer main peaks 3 and 4 positioned at around 1900 cm⁻¹ and 2000 cm⁻¹ which are characteristic signals connected to the C \equiv O vibrations.[50] The number of peaks and their relative intensities, however, do not change, which indicates that the incorporated catalytic centers of the monomer 1-3 are not decomposed upon polymerization, and that a facial arrangement (fac-isomeric form) of the carbonyl ligands is obviously retained at the rhenium atom.

In contrast, the IR-signal positioned at $2200 \,\mathrm{cm}^{-1}$ that is characteristic for the C \equiv O vibrations almost vanishes completely, while the appearance of a new sharp peak 8, centered at around $848 \,\mathrm{cm}^{-1}$, indicates the asymmetric stretching band of PF_6^- . It is assumed that the vanishing of the peak at $2200 \,\mathrm{cm}^{-1}$ might be directly connected to a loss of the C \equiv O signal in the course of the polymerization process. The fact that no solvent bands from acetonitrile at 2293, 2252, 1442, 1035 and 917 cm⁻¹,[112] are present in the spectrum suggests that the 848 cm⁻¹ band can be attributed to the presence of PF_6^- anion containing species in the polymer phase. The strong increase of this peak could then be explained by a substitution of the Cl⁻ in 1-3 by PF_6^- from the electrolyte during polymerization to retain charge neutality,[113] or because of the rather high relative intensity of the signal, by an uptake of a certain amount of the alkylammonium electrolyte. The two peaks 1 and 2, at 2972 and $2877 \,\mathrm{cm}^{-1}$, are attributed to the valence vibrations of additionally aliphatic C-H bonds formed either during polymerization, or due to the presence of the alkylammonium salt. The peak 5, at 1640 cm⁻¹, is characteristic for aryl-conjugated C=C bonds. The two smaller peaks 9 and 10, at 750 and 690 cm⁻¹, are typical for out-of-plane C-H bending vibra-

tions of monosubstituted benzene.[114] Additionally the peak 7 at 1065 cm^{-1} might originate from not well defined C-H vibrations along the main chain of the polymer film, which would explain the relative broadness of this absorption peak.



Figure 7.10: ATR-FTIR difference absorption spectra of a 150 nm thick rhenium catalyst film on 10 nm Pt sputtered onto a ZnSe ATR crystal to the pure 10 nm Pt/ZnSe ATR crystal (top, red line) and of the monomer 1-3 dissolved in DCM and drop cast on a ZnSe ATR crystal to the pure ZnSe ATR crystal (bottom black line).

Following this argumentation, it is assumed that the polymerization proceeds via radical addition similar to the mechanism published by Canadas et al.[114] Still, due to the strong negative potential necessary for electro-polymerization of the monomer 1-3, it is likely that additional side reactions take place that account for the unassigned peak 6 at 1280 cm^{-1} in the IR-spectrum of Figure 7.10. As a result, at this time it is not yet possible to determine the exact structure of the rhenium catalyst film. For the catalytically active centres of the rhenium catalyst film however, we propose a structural motif similar to the one depicted in Scheme 7.4.

The film morphology was studied using SEM and AFM technique. For this purpose the film surface was scratched to see the difference between the rhenium catalyst film formed (and the ZnSe/Pt substrate. As was reported in a published paper,[115] a highly ordered granular structure is observed and attributed to the granular structure is characteristic for sputtered platinum. However, the type of structure observed for the catalyst film is significantly different from the metallic substrate. The lack of clearly visible structures on the surface of the film suggests a lack of order in the film, which is expected for polymeric films. From a measurement of the tilted substrate by an angle of 54.0°, the film thickness of 150 nm could be measured. The roughness of the film was studied by atomic force microscopy (AFM). A close look on the film surface reveals the existence of particles that probably remain from

the film formation process. The RMS roughness in the regions without particles was found to be $5.4 \,\mathrm{nm}$.

Concluding the electropolymerisation of the monomer 1-3 it appears to be a promising way to change from homogeneous to heterogeneous catalysis for CO_2 -reduction, reducing the amount of required catalyst material needed and overcoming the limitations regarding solubility of homogeneous catalysts in general. The novel catalyst film furthermore demonstrates high selectivity for the CO_2 -reduction to CO at relatively low reduction potentials and high current densities. A detailed study on the polymerization of 5,5'-bisphenylethynyl-2,2'-bipyridyl)Re(CO)₃Cl and its characterization has been published.[115]

7.3 (4,4)-dicarboxyl-2,2'-bipy.)Re(CO)₃Cl immobilization at a zinc oxide layer

A different approach was used at the very beginning of the thesis when the rhenium catalyst 1-2 with the dicaboxylic side group at the ligand system was used to attach to a binding metal oxide layer with the aim of moving from a homogeneous to a heterogeneous catalysis (compare Figure 5.8). Zn was chosen as working electrode due to its high overpotential for hydrogen evolution and its native oxide layer. Scheme 7.11 illustrates the idea of anchoring the rhenium catalyst 1-2 onto an ZnO layer with the purpose of going from homogeneous to heterogeneous catalysis. Additionally in Scheme 7.11 the series from a to c depicts the expected, subsequent CO_2 reduction mechanism upon negative bias of the electrode in aqueous solution saturated with CO_2 . The mechanism was expected to proceed similar to the homogenous system, namely a two electron, proton coupled CO_2 reduction according to reaction 1.4 described in the introduction chapter 1, leading to CO and H₂O as reduction products.



Figure 7.11: Schematic representation of (4,4)-dicarboxyl-2,2'-bipyridyl)Re(CO)₃Cl (1-2) attached to an electrode by the metal native ZnO layer and the expected, subsequent CO₂ reduction mechanism a to c.

Figure 7.12 shows the cyclic voltammograms of $(4,4'-\text{dicarboxyl-2,2'-bipyridyl})\text{Re}(\text{CO})_3\text{Cl}$ immobilized at a zinc oxide layer in aqueous, N₂ purged solution with a KHPO₄ buffer at pH 7. Below a potential of approx. -1200 mV vs. Ag/AgCl in 3M KCl a reductive wave is observed attributed to the reduction of the metaloxide-catalyst bond. Below a potential of $-1400 \,\mathrm{mV}$ vs. Ag/AgCl substantial reductive current is observed due to hydrogen (H₂) evolution.



Figure 7.12: Cyclic voltammograms of (4,4)-dicarboxyl-2,2'-bipyridyl)Re(CO)₃Cl immobilized at a zinc oxide layer in aqueous, N₂ purged solution with a KHPO₄ buffer at pH 7

It can be concluded, that in this experiments the anchoring to the oxide layer was successfully achieved, however it tourned out that the film was not stabel uppon electrochemical reduction. The cyclicvoltammetry experients showed, that below a potential of -1200 mVvs. Ag/AgCl or equivalent -1000 mVvs. NHE (compare Figure 7.12) the layer was irreversibly destroyed and rinsed of the electrode as a black precipitate. Similar experiments have been reported where the anchoring to the oxide layer of TiO₂ was successfully achieved [111] showing the working principle of the idea, however up to now no application for CO₂ reduction was reported. This work has not been carried further within the frame of this thesis.

Chapter 8

Organic semiconductors for \mathbf{CO}_2 reduction

As described in the introduction chapter under 1.4, a very promising approach in the last decade was the combination of catalysts with inorganic semiconductor materials. In this work the approach is different in a way that an organic semiconductor is used as light absorbing donor material in combination with an acceptor catalyst, as for example Pyridinium or (2,2)-bipyridyl)Re(CO)₃Cl, for the actual CO₂ reduction. The advantage lies in the unique properties of organic semiconductors as they are flexible, light weight, bio-degradable and bio-compatible, abundant and hold hence the promising perspective to be cheap in production. Figure 8.1 shows the general idea of a photoinduced charge transfer from a biased organic semiconductor onto a catalyst redox mediator for CO₂ reduction.

The schematic drawing in Figure 1.5 shows an organic p-type semiconductor, as for example poly(3-hexylthiophene) (P3HT) on indium tin oxide (ITO), which serves as a transparent conducting electrode (TCE). The whole system is in contact with an electrolyte solution forming a Schottky type of contact.[33] The electrolyte solution contains a catalyst acceptor molecule as for example pyridinium. Upon light irradiation an electron-hole pair is generated in the organic semiconductor. The electron-hole pair generated can not be treated as individual charge carriers since the positive hole (h^+) and the negative electron (e^-) are initially still bound in the material by their Coulomb attraction.[34] The electron-hole pair, also known as exciton, moves as a quasi particle in the bulk of the material until the two charge carriers recombine or hit an interface where the driving force is strong enough for both charges to separate. In the ideal case the exciton will reach the semiconductor-electrolyte interface where the electron transfers to the catalyst acceptor molecule and the hole, now free to move in the bulk material, travels back to the biased ITO contact where it recombines with an electron. The catalyst material loaded with the negative charge is then capable of transferring this charge to the substrate, namely CO₂, and reducing it to the desired product.



Figure 8.1: Suggested mechanism for photoinduced charge transfer from a biased organic p-type semiconductor onto pyridinium as a catalyst redox mediator for CO_2 reduction.

8.1 Poly(3-hexylthiophene) electrodes with pyridinium as homogeneous catalyst

In this section poly(3-hexylthiophene) (P3HT) is used as the organic semiconducting polymer which serves as donor material and Pyridinium, already described in chapter 5, as a homogeneous electrocatalyst in solution. Figure 8.2(a) shows the schematic chemical structure of poly(3-hexylthiophene) (P3HT). Initially it is important to determine the reductive potential window of such a system in order to know up to what negative potential the working electrode can be reversibly biased without damage of the electrode or the electrolyte and is usually defined by the potential range (window) were no significant current is observed.

Figure 8.2(b) shows the cyclic voltammograms of a P3HT (black line with squares) and a blend of P3HT:PCBM (blue line with triangles, PCBM = Phenyl-C61-butyric acid methyl ester) covered ITO working electrode. It is known that a mixture of P3HT and PCBM is beneficial in a way that the PCBM works as an efficient acceptor molecule for electrons in a P3HT:PCBM blend and hence increasing the photocurrent supported by those bulk-heterojunction layers significantly.[116] For electrochemistry and photoelectrochemistry experiments it was found however, that a blended P3HT:PCBM as working electrode on ITO demonstrate a substantial smaller reductive potential window as can be seen in Figure 8.2(b) (blue line with triangles) which makes this combination not suitable for electrochemical applications. Therefore, in the following experiments a pure P3HT film on ITO/glass substrate was used.

Figure 8.3 shows cyclic voltammograms of a 100 mM pyridine (green lines with trian-



(a) Poly(3-hexylthiophene) (P3HT)

(b) Cyclic voltammograms of P3HT on ITO

Figure 8.2: (a) Schematic chemical structure of poly(3-hexylthiophene) (P3HT) (b) Cyclic voltammograms of a P3HT (black line with squares) and a blend of P3HT:PCBM (blue line with triangles) covered ITO working electrode. Experiments with a blended P3HT:PCBM working electrode demonstrate a substantial smaller reductive potential window. Voltammograms are recorded in a nitrogen saturated acetonitrile solution containing 0.1 M TBAPF_6 and a scan speed of 50 mVs^{-1} .

gles) and pyridinium (red lines with circles) electrolyte solution under dark and white light illumination with an approximately 120 nm thick P3HT film covered on ITO as working electrode. The experiment shows the effect upon protonation and light. It can be seen that the experiments under illumination show a significant current increase compared to the corresponding experiment in dark. Already when pyridine is present, the current increases significantly, which leads to the conclusion that pyridine acts as an acceptor molecule for charge transport. When the pyridine is converted to pyridinium, by the addition of small amounts of diluted sulfuric acid, the dark current increases which can be attributed to proton reduction. Upon light irradiation there is again a clear increase in the reductive current especially in the potential range where no current could be observed under dark conditions. For comparison a scan with a pure ITO electrode under otherwise identical conditions is also shown (black dashed line).

To investigate this effect further, potentiostatic experiments were performed where the semiconducting working electrode was biased to a constant potential of -800 mVvs. SCE and the light was repeatedly turned on an off.

Figure 8.4(a) shows the photoresponce of a P3HT covered ITO electrode at constant potential of -800 mVvs. SCE upon white light irradiation and a varying the pyridinium concentration from 10 to 100 mM. Upon light irradiation the current jumps immediately to more negative values and returns to the initial value when the light is turned off again. When the catalyst concentration is increased, the corresponding current photo-response is enhanced, which is expected when pyridinium acts as an efficient acceptor molecule. In Figure 8.4(b) the photocurrent of the data shown in Figure 8.4(a) is plotted as $\Delta j_{light-dark}$. It can be seen that the photocurrent increases linearly with the pyridinium concentration between 10 mM and 100 mM (black dashed line).



Figure 8.3: Cyclic voltammetry of a 100 mM pyridine (green lines with triangles) and pyridinium (red lines with circles) electrolyte solution under dark and white light illumination with a 120 nm thick P3HT covered ITO working electrode. Experiments under illumination (open symbols) show a significant current increase compared to the corresponding experiment in dark. For comparison a scan with a pure ITO electrode under otherwise identical conditions is also shown (black dashed line). Voltammograms are recorded at $10 \,\mathrm{mVs^{-1}}$ in a nitrogen-saturated KCl solution (0.1 M) and a Pt counter electrode.

In Figure 8.5 a similar experiment is shown where the photocurrent (as $\Delta j_{light-dark}$) from the photoresponse experiments of a P3HT covered ITO electrode at constant potential of -800 mVvs. SCE upon white light irradiation is plotted at different light intensities. The experiment was performed for two different pyridinium concentrations, namely a 10 mM and a 100 mM concentration. It was found that the photocurrent increases with increasing light intensity for both concentrations of the catalyst acceptor molecule.

One potential error of importance is the temperature effect upon light irradiation. As the solvent and electrode absorb some portion of the white light irradiation it can not be excluded that a temperature effect is observed. By taking a look into the theory of electrochemistry it appears to be very difficult describing mathematically the dependence of the diffusion limited current density of an electrochemical cell on the electrochemical reaction are not only determined by the electron transfer process, but also by transport processes like diffusion, ad-and desorption of reactants and reactions in the homogeneous solution preceding or following the charge transfer. A very good description of the complexity of such a system is described in reference nr. [117]. To estimate this error an additional experiment was performed where a thermocouple was attached to a blank ITO electrode in an otherwise identical system. It is expected that the ITO serves as a good heat conductor giving an almost homogeneous heat distribution within the electrode area of approximately 4 cm².

Figure 8.6 shows the temperature increase upon white light irradiation on a ITO electrode in a nitrogen-saturated KCl solution (0.1 M) (blue triangles). As can be seen the tem-



(a) Photoresponce of P3HT:Pyridinium



(b) Photocurrent plotted as $\Delta j_{light-dark}$

Figure 8.4: (a) Photoresponce of a P3HT covered ITO electrode at constant potential of -800 mVvs. SCE upon white light irradiation and a varying pyridinium concentration from 10 to 100 mM. The measurements are recorded in a nitrogen-saturated KCl solution (0.1 M) and a Pt counter electrode. (b) Photocurrent plotted as $\Delta j_{light-dark}$ from the photoresponse experiments depicted in (a). The photocurrent increases linearly with the pyridinium concentration between 10 mM and 100 mM (black dashed line).



Figure 8.5: Photocurrent plotted as $\Delta j_{light-dark}$ from the photoresponse experiments of a P3HT covered ITO electrode at constant potential of -800 mVvs. SCE upon white light irradiation at different light intensities. The photocurrent increases with increasing light intensity for a pyridinium concentration of 10 mM (black squares) and 100 mM (red circles).

perature increase follows an exponentially increasing behavior according to a fitting curve of $y(t) = 26.66 \cdot (1 - e^{-0.0034 \cdot (t+296.7)})$ (black line). It can be seen that within an illumination time of 20 min. the temperature increased by about 6.6 °C. Analyzing this behavior the electrode temperature has a time constant (τ) of about 294.12 s which represents the time it takes the system's response to reach 1 - 1/e (about 63.2 %) of its final (asymptotic) value.

In a very detailed study on the temperature effect of the working electrode on the limiting current of a 2 mM solution of $\text{Ru}(\text{NH}_3)_6^{3+}$ in aqueous 0.1 M KCl it was shown that upon a temperature increase of 6.7°C from 303.9 K to 310.6 K (about the same temperature range as in the experiment in Figure 8.3) the relative increase in the limiting current density was about 16.8 %.[118] Since in the cyclic voltammetry experiments depicted in Figure 8.3, the scan speed was 10 mVs⁻¹ and the return potential is - 850 mV, reaching peak current takes 85 s. At this return potential the relative increase in current density between dark and light measurement is about 133 %. Following this argumentations it can be safely concluded that a temperature effect can not be responsible for the change in the cyclic voltammetry current densities upon light irradiation depicted in Figure 8.3, nor for the immediate photoresponse observed in the measurements shown in Figure 8.4 and Figure 8.5.

Bulk electrolysis experiments using the P3HT/pyridinium system were performed, however no products in form of methanol could be detected. This is not surprising since the lifetime of this type of electrodes is rather low and the photocurrent is in the μ A regime. If one has a look back to chapter 5 where the pyridinium catalyst was described, one finds for example in Figure 5.22(a) that the current densities were in the order of mA for electrolysis experiments of 30 hrs and only then it was possible to detect methanol in the electrolyte solution with concentrations in the ppm level. This concentrations are close to the detection limit of the GC system. In the case with the P3HT covered ITO electrodes the electrodes corroded within 2 to 3 hrs of electrolysis time. As a resulting conclusion, this system has



(a) Temperature increase measurement



(b) Experiment foto

Figure 8.6: (a) Temperature increase upon white light irradiation on a ITO electrode in a nitrogen-saturated KCl solution (0.1 M) (blue triangles). The temperature increase follows $y(t) = 26.66 \cdot (1 - e^{-0.0034 \cdot (t+296.7)})$ (black line). (b) Foto of the corresponding experimental setup.

to be improved significantly in terms of electrode stability and current densities which is subject to ongoing research.

8.2 Polyvinylcarbazole electrodes with (2,2)-bipy.)Re(CO)₃Cl as homogeneous catalyst

It has been mentioned in chapter 6, Homogeneous photo catalysis, that the fac-(2,2'-bipyridyl) Re(CO)₃Cl (1-1) is an efficient photo catalyst for the reduction of CO₂ producing mainly CO with the aid of a sacrificial electron donor as for example triethanolamine (TEOA). The quantum yield (Φ_{CO}) for CO₂ reduction of this compound 1-1 has been reported with 0.14 almost 30 years ago and subsequent modifications of the bipyridine ligand system of 1-1 lead to the development of superior catalysts with Φ_{CO} up to 0.59, making these type of materials the most efficient CO₂ photo-catalyst among known homogeneous catalyst materials by now.[43, 46, 77, 98]

Unfortunately rhenium tricarbonyl complexes have several disadvantages when it comes to practical applications, stating their poor absorption in the visible region of the solar spectra and the low abundance of rhenium as the most prominent ones. One promising solution to overcome this disadvantages of rhenium based catalysts is to use poly(N-vinylcarbazole) (PVK) as a decent an cheap absorber to serve as redox photosensitizer in combination with fac-(2,2'-bipyridyl)Re(CO)₃Cl (1-1) as catalyst acceptor.





Figure 8.7: (a) Chemical structure of $(2,2'-bipyridyl)Re(CO)_3Cl$ and its corresponding highest occupied molecular orbital (HOMO) and lowest unoccupied molecular orbital (LUMO) level in electron volt (eV), and Poly(N-vinylcarbazole) (PVK) and its corresponding energy values for valence (VB) and conduction band (CB). (b) Schematic drawing of frontier orbital energy levels comparing PVK as donor and $(2,2'-bipyridyl)Re(CO)_3C$ (1-1) as acceptor molecule.

Figure 8.12(a) shows the chemical structure of $(2,2'-bipyridyl)Re(CO)_3Cl$ and its corresponding highest occupied molecular orbital (HOMO) and lowest unoccupied molecular

orbital (LUMO) level determined with -6.3 eV vs. vacuum for the HOMO and -3.6 eV vs. vacuum for the LUMO respectively. The values are determined from electrochemical and UV-Vis absorption measurements as well as quantum mechanical calculations on the DFT-level compare chapter 3 and chapter 5 of the thesis. Additionally Figure 8.12(a) shows the chemical structure of poly(N-vinylcarbazole) (PVK) and its corresponding energy values for valence (VB) and conduction band (CB) with -5.8 eV vs. vacuum and -2.2 eV vs. vacuum respectively, taken from literature values.[119, 120] Figure 8.12(b) shows the schematic drawing of the material frontier orbital energy levels comparing PVK as donor and $(2,2'-bipyridyl)Re(CO)_3Cl$ as acceptor molecule versus the vacuum energy. For the electrochemical consideration of frontier orbital energy levels an offset of the normal hydrogen electrode (NHE) potential vs. the vacuum leve with -4.75 eV is used (blue dashed line).[36] As can be seen in the schematic of Figure 8.12(b) the energy levels of the donor polymer and acceptor catalyst are aligned in a favorable situation for photo-excited charge and/or energy transfer. Subsequent photoluminescence (PL) quenching and light induced ESR experiments were carried out to study this system in bulk, solid phase mixtures of donor and acceptor, and at a donor-acceptor solid-liquid interface.

8.2.1 Photoluminescence quenching in solid films



Figure 8.8: PVK and (2,2'-bipyridyl)Re(CO)₃Cl (1-1) excitation and photoluminescence spectra. Excitation spectra for a pure, approx. 60 nm thick film of PVK (black solid line with squares), photoluminescence of the same PVK film on glass substrate excited at 350 nm (dashed gray line with squares), excitation spectra for a pure, approx. 40 nm thick film of 1-1 (blue line with circles) and photoluminescence of the same film of 1-1 on glass substrate excited at 350 nm (dashed dark blue line with circles).

Figure 8.8 shows the excitation and photoluminescence spectra of PVK and catalyst 1-1. The excitation spectra for a pure, approx. 60 nm thick film of PVK (black solid line with squares) shows the detector signal at 410 nm of the photoluminescence while the excitation wavelength is scanned from 250 to 380 nm. The spectra shows clear separated maxima

at approximately 340 and 300 nm with a distinct shoulder at 330 nm. The dashed gray line with squares give the corresponding photoluminescence of the same PVK film on glass substrate excited at 350 nm with a maximum at 410 nm. Additionally Figure 8.8 shows the excitation spectra for a pure, approx. 40 nm thick film of $(2,2' \text{ bipy})\text{Re}(\text{CO})_3\text{Cl}$ (blue line with circles) which gives the detector signal at 540 nm of the photoluminescence while the excitation wavelength is scanned from 300 to 520 nm. The spectra shows the typical strong electronic ${}^1\pi\pi^*$ intraligand transitions of the diimine ligands in the higher energetic region, at wavelengths shorter than 330 nm and MLCT signatures at lower energies with a maximum at about 370 nm.[121, 50] The dashed dark blue line with circles give the photoluminescence of the same $(2,2' \text{ bipy})\text{Re}(\text{CO})_3\text{Cl}$ film on glass substrate excited at 350 nm. The broad emission of the ${}^3\text{MLCT}$ to the ground state of the compound 1-1 is covering a typical wide spectral region including blue, green and yellow light with its maximum at around 540 nm. The excitation spectra are normalized to the spectra of the excitation lamp (photons per wavelength) measured by an internal, calibrated silicon diode.

Figure 8.9(a) shows PL quenching experiments with PVK as donor polymer and (2.2)bipy)Re(CO)₃Cl catalyst as quenching material on glass/ITO substrate. The materials were dropcast from dichloromethane (DCM) solution. The PL spectra are corrected by the absorption of each film taking an average value of 10% for the contribution due to light scattering into account. The amount of PVK is in all samples $5 \cdot 10^{-4}$ g. In Figure 8.9(a), the solid line with black squares give the photoluminescence of a pure, approx. 1.8 μ m thick, PVK film on glass substrate excited at 350 nm. It shows a clear PL maximum at about 410 nm. As soon as some catalyst material is present the photoluminescence of the PVK polymer is reduced and the typical catalyst photoluminescence with its maximum at 553 nm appears. At a quencher concentration of approx. $15 \cdot 10^{-6}$ g (about 3% of the total material in the film) the PL signal of the PVK donor polymer disappeared completely and only the PL signal of the acceptor catalyst at 550 nm is present. In Figure 8.9(b) the PL signal of the data in (a) is subtracted by the PL of the pure PVK. This plot reveals a clear isosbestic point at 485 nm as indicated in the graph. This indicates that the change in the PL signal scales equally to lower and higher wavelengths of the isosbestic point which also suggests that there is little to no degradation during the measurement.

Figure 8.9(c) shows the Stern-Volmer Plot of the data represented in the Figure 8.9(a) before where PL^0 is the photoluminescence intensity of the pure PVK polymer without quencher at its maximum at approx. 410 nm and PL is the photoluminescence intensity when a certain concentration of the quencher is added. The last curve from Figure 8.9(a) with an amount of quencher material of $15 \cdot 10^{-6}$ g is not represented since the PL signal is almost negligible and hence difficult to evaluate. Furthermore, the inhomogeneity of the film increases with increasing rhenium catalyst concentration leading to lower PL signal of the catalyst acceptor at high concentrations.



(a) PL quenching experiments with PVK



(c) Stern-Volmer Plot

Figure 8.9: (a) PL quenching experiments with PVK as donor polymer and different concentrations of (2,2)bipyridyl)Re(CO)₃Cl (1-1) catalyst as quenching material added on glass/ITO substrate. (b) PL signal subtracted by the PL of the pure PVK reveals an isosbestic point at 485 nm (c) Stern-Volmer Plot of the data represented in (a) where PL⁰ is the photoluminescence intensity of the pure PVK polymer without quencher and PL is the photoluminescence when a certain concentration of the quencher is added.

According to the Stern-Volmer equation 8.1, a plot of (PL^0/PL) -1 vs. quencher concentration should give a straight line which is observed for this system to a high degree (R-square value of 0.9967).[122]

$$\frac{P^0}{P} = 1 + K_{SV}[Q] \tag{8.1}$$

In equation 8.1, K_{SV} is the Stern-Volmer constant and Q is the quencher concentration. Evaluating equation 8.1 for the data represented in Figure 8.9(c) results in a quenching constant K_{SV} of $2.06(\pm 0.08) \cdot 10^6 \text{ g}^{-1}$. In the case of dynamic quenching, in e.g. Förster resonance energy or Dexter type electron transfer, the constant K_{SV} is the product of the true quenching constant k_q and the excited state lifetime τ in the absence of the quencher material, according to equation 8.2.

$$K_{SV}[Q] = k_q \cdot \tau_F \tag{8.2}$$

The fluorescence lifetime of PVK (τ_F) has been reported with 5.34(±0.03) ns.[123] Evaluating equation 8.2 for a K_{SV} of 2.06(±0.08) \cdot 10⁶ g⁻¹ and a τ_F of 5.34(±0.03) ns results in a quenching constant k_q of 3.85(±0.17) \cdot 10¹⁴ g⁻¹s⁻¹. This quenching constant k_q is then interpreted as the bimolecular reaction rate constant for the elementary reaction of the excited state with the quencher material Q.



Figure 8.10: PL spectra with PVK as donor polymer and $1 \cdot 10^{-6}$ g (solid lines) or $6 \cdot 10^{-6}$ g (dashed lines) of (2,2'-bipyridyl)Re(CO)₃Cl (1-1) catalyst as quenching material on glass/ITO substrate. The material was dropcast from solution, the spectra are corrected to their corresponding absorption. The PVK concentration in all samples is $5 \cdot 10^{-4}$ g. The solid films are excited at two different wavelength namely 350 (black lines) and 400 nm (red lines) respectively.

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Figure 8.10 shows PL quenching experiments with PVK as donor polymer and two different concentrations of $(2,2' \text{ bipy}) \text{Re}(\text{CO})_3 \text{Cl} (1-1)$ catalyst as quenching material added. The samples were dropcast from dichloromethane (DCM) solution. The PL spectra are corrected by the absorption of each film taking an average value of 10% for the contribution due to light scattering into account. The PVK concentration in all samples is $5 \cdot 10^{-4}$ g. The solid films are excited at two different wavelength namely 350 nm (black lines), which is the maximum of the PVK donor and relative minimum of the catalyst acceptor, and at 400 nm (red lines), which is the maximum of the ³MLCT catalyst acceptor absorption, respectively. The experiment is depicted for two different concentrations of the catalyst acceptor, $1 \cdot 10^{-6}$ g (solid lines) and $6 \cdot 10^{-6}$ g (dashed lines). In the experiment with the lower concentration, by exciting at the polymer absorption maximum at 350 nm, two luminescence peaks are observed, one characteristic for the PVK donor polymer at about 400 nm and the other at about 550 nm, characteristic for the luminescence of the catalyst acceptor 1-1. When the sample is excited at 400 nm, namely at the ³MLCT maximum o the acceptor 1-1, no PL signal of the donor polymer is present and only a weak PL signal of the catalyst material can be observed. At high catalyst quencher concentrations (dashed lines), independent of the excitation wavelength, no PL signal of the PVK donor polymer is present anymore, however for both wavelengths a strong PL signal of the acceptor catalyst 1-1 is observed. Following the argumentation of this results, together with the fact that for this system no light induced ESR signal could be observed, the process seems to follow a Förster- and/or Dexter type of energy transfer from PVK to (2,2') bipy)Re(CO)₃Cl (1-1) with only a minor contribution of charge transfer involved.

8.2.2 Photoluminescence quenching in ACN solution

For the potential application of CO_2 reduction to a synthetic fuel by a photoinduced energy transfer from PVK as donor material to $(2,2' \text{ bipy})\text{Re}(CO)_3\text{Cl}$ (1-1) as catalyst acceptor, bulk solid donor-acceptor mixtures are not applicable. In typical applications reported in literature, the CO_2 substrate is provided by purging an organic solvent (DCM, ACN, etc.) until gas saturation and dissolving the catalyst material to form a homogeneous solution mixture.[45, 100, 124]

Figure 8.11(a) shows PL quenching experiments with a solid, approx. 9nm thick film of PVK on ITO/glass substrate as donor polymer immersed into an acetonitrile (ACN) solution. The black solid line with squares shows the PL signal of the pure PVK substrate in ACN excited at 350 nm. In the subsequent spectra $(2,2' \text{ bipy})\text{Re}(\text{CO})_3\text{Cl}$ catalyst was added as quenching material into the ACN solution. Following the increasing concentration of the catalyst material, clear quenching is observed with a similar behavior as previously shown for the bulk, solid donor-acceptor mixtures. The catalyst photoluminescence with its maximum at 553 nm appears, while the PVK luminescence with its maximum at about 410 nm vanishes almost completely once a catalyst concentration of 0.56 mgm^{-1} is reached (violet curve with circles). The gray dashed line shows the PL signal at the end of the quenching experiment when the PVK film was removed from the ACN solution. By looking at the spectra recorded in Figure 8.11(a) one has to take into account that only a few surface mono layers of donor



(a) PL quenching experiments with PVK



(c) Stern-Volmer Plot

Figure 8.11: (a) PL quenching experiments with a solid, approx. 9nm thick film of PVK on ITO/glass substrate as donor polymer and different concentrations of (2,2'-bipyridyl)Re(CO)₃Cl (1-1) catalyst as quenching acceptor added into the ACN solution. (b) PL signal subtracted by the PL of the pure PVK reveals an isosbestic point at 530 nm (c) Stern-Volmer Plot of the data represented in (a) where PL⁰ is the photoluminescence intensity of the pure PVK polymer film without quencher present, and PL is the photoluminescence when a certain concentration of the quencher is added into the ACN solution.
and acceptor molecules get the chance to interact, while the bulk of the material in the solid phase and dissolved in solution will not take part in the actual energy transfer reaction. Following this argumentation it is remarkable observing a strong PL quenching effect in this solid-liquid donor-acceptor system. In Figure 8.11(b) the PL signal of the data in (a) is subtracted by the PL of the pure PVK. This plot reveals a isosbestic point at 530 nm as indicated in the graph, which is less pronounced and shifted to longer wavelength compared to the solid-solid mixture shown before (Figure 8.9(b), isosbestic point at 485 nm).

In Figure 8.11(c) the data represented in the Figure 8.11(a) is depicted in a Stern-Volmer Plot, where PL⁰ is the photoluminescence intensity of the pure PVK polymer film without quencher present, and PL is the photoluminescence when a certain concentration of the quencher is added into the ACN solution. The plot of (PL⁰/PL)-1 vs. quencher concentration gives again an almost perfect straight line (R-square value of 0.999). Evaluating equation 8.1 for the data represented in Figure 8.11(b) results in a quenching constant K_{SV} of $10.17(\pm 0.13) \cdot 10^3 \text{ ml g}^{-1}$. Evaluating again equation 8.2 for K_{SV} of $10.17(\pm 0.13) \cdot 10^3 \text{ ml g}^{-1}$ and τ_F of $5.34(\pm 0.03)$ ns results in a quenching- or bimolecular reaction rate constant k_q of $1.90(\pm 0.04) \cdot 10^{12} \text{ ml g}^{-1}\text{s}^{-1}$.

Summarizing this work, the photoinduced energy transfer from poly(N-vinylcarbazole), as donor material, to fac-(2,2'-bipyridyl)Re(CO)₃Cl, as catalyst acceptor, could be shown for the first time. Photoluminescence quenching experiments revealed dynamic quenching due to resonance energy transfer in solid donor/acceptor mixtures and in solid/liquid systems. The bimolecular reaction rate constants for the elementary reaction of the excited state with the quencher material could be determined with $3.85(\pm 0.17)\times10^{14}$ g⁻¹s⁻¹ using Stern-Volmer analysis. This work shows that poly(N-vinylcarbazole) (PVK) as a decent an cheap absorber material can act efficiently as redox photosensitizer in combination with fac-(2,2'-bipyridyl)Re(CO)₃Cl as catalyst acceptor, which might lead to possible applications in photocatalytic CO₂ reduction.

8.3 Functionalized Poly(3-hexylthiophene)

During the last 20 years electrically conducting and semiconducting polymers have received a great deal of attention due to their interesting properties and potential applications.20 Among a number of conducting polymers, polythiophene (PT) has attracted excessive interest since it is relative stable to both oxygen and moisture and can readily be used in electrochemistry.[125, 126, 127]

Therefore, the aim of this work is to functionalize poly (3-hexylthiophenes) (P3HT) with fac-(2,2'-bipyridyl)Re(CO)₃Cl (1-1) for its potential application of electro- and photochemical CO₂ reduction. The monomer is deposited by electro-polymerization onto the electrode and used to determine its potential for heterogeneous catalysis towards CO₂ reduction. This interesting approach lead to the formation of a conducting polymer with functionalised rhenium bipyridine catalysts attached to the polymer backbone via alkyl bridges.



Figure 8.12: Schematic representation of three different conducting polymers investigated in this study, polythiophene (8-1), poly (3-hexylthiophene) (8-2) and fac- $(2,2'-bipyridyl)Re(CO)_3Cl$ functionalized poly 3- $(7-(4, 4'-methyl-(2,2'-bipyridil)ReCO_3Cl)heptyl)$ thiophene (8-3). (Materials were prepared by G. Aufischer.)

Figure 8.12 shows the schematic representation of three different conducting polymers investigated in this study, namely polythiophene (8-1), poly (3-hexylthiophene) (8-2) and fac-(2,2'-bipyridyl)Re(CO)₃Cl functionalized poly 3-(7-(4, 4'-methyl-(2,2'-bipyridil)ReCO₃Cl) heptyl) thiophene (8-3). This three different type of polymers are what is described in literature as three different generations of conducting polymers. Polythiophene (8-1) is a conjugated polymer with good conductivity, but with the disadvantage of low processability and solubility. To overcome this disadvantages P3HT (2) is a polyconjugated material with additional hexyl substitutions leading to a high solubility and processability without losing the interesting physical and chemical properties of the material. Finally the novel fac-(2,2'-bipyridyl)Re(CO)₃Cl functionalized P3HT (8-3) is a fully functionalized polyconjugated material with improved and new physical and chemical properties for the specific applications of electro- and photochemical CO₂ reduction. (The monomer synthesis is described in detail in the Bachelor thesis of G. Aufischer.)

8.3.1 Electropolymerisation and characterization

Electroactive monomers such as the monomer thiophene unit can polymerize to form conducting or semi conducting polymers. Such conducting polymers can be synthesized either chemically by using an external reactant or electrochemically by electropolymerization. The later has several advantages for deposition on conducting supporting electrodes compared to chemical polymerization and was the matter of choice in this work.

Electropolymerization is a well-known technique and the method mainly used for deposition of organic conducting or semiconducting films on conducting substrate electrodes like platinum. The procedure has several advantages, the most important ones are the possibility to control the rate of polymer nucleation and hence the growth of the film by proper selection of the electropolymerization parameters. This allows also the control of film thickness by the amount of charge that passed during the deposition process. Furthermore a suitable selection of solvent and supporting electrolyte allow to a certain degree control over the film morphology.[128] In this work, electropolymerization is performed under potentiodynamic conditions which was shown to result in the formation of electrochemically conducting polymer matrixes forming disordered spatial chains.[129]



Figure 8.13: (a) Potentiodynamic electropolymerization of 0.1 M thiophene to polythiophene (8-1) in ACN solution containing 0.1 M TBAPF₆ as supporting electrolyte. First scan (red line with circles) and last scan (blue line with triangles). The cyclic voltammograms were recorded at a scan rate of $100 \,\mathrm{mVs^{-1}}$ inside the glove box using a Pt working electrode (WE), a Pt counter electrode (CE) and a Ag/AgCl quasi reference electrode. (b) Picture of the electropolymerized polythiophene on a Pt foil supporting working electrode.[Prepared by G. Aufischer]

Figure 8.13 shows the potentiodynamic electropolymerization of 0.1 M thiophene to polythiophene (8-1) in ACN solution containing 0.1 M TBAPF₆ as supporting electrolyte. The successive film formation is indicated by an increase in the current density of each cycle. The first scan is depicted in red line with circles and the last scan in blue line with triangles respectively. After electropolymerization the Pt working electrode was fully covered with a continuous shiny red to brown film as can be seen in the picture in Figure 8.13(b).

The mechanism for the polymerization has been reported to proceed via a radical coupling mechanism resulting in α - α linkages. Following the progress of the polymerization in Figure 8.13 one can observe a shift to lower oxidation potentials upon increasing scan numbers. This trend can be understood by the fact that the α - α linkages are a combination of monomer and oligomer radicals where the polymerization reaction occurs at lower potential on existing polymer than on a bare metal surface.[130] The cyclic voltammograms were recorded at a scan rate of $100 \,\mathrm{mVs^{-1}}$ inside the glove box using a Pt working electrode (WE).



(a) Poly(3-hexylthiophene) electropolymerization



(b) Picture of the electropolymerized film

Figure 8.14: (a) Potentiodynamic electropolymerization of 0.056 M 3-hexylthiophene to poly (3-hexylthiophene) (8-2) in propylene carbonate solution containing 0.1 M TBAPF₆ as supporting electrolyte. First scan (red line with circles) and last scan (blue line with triangles). The cyclic voltammograms were recorded at a scan rate of $50 \,\mathrm{mVs^{-1}}$ inside the glove box using a Pt working electrode (WE), a Pt counter electrode (CE) and a Ag/AgCl quasi reference electrode. (b) Picture of the electropolymerized poly (3-hexylthiophene) on a Pt foil supporting working electrode. [Prepared by G. Aufischer]

Figure 8.14 shows the potentiodynamic electropolymerization of 0.056 M 3-hexylthiophene to poly (3-hexylthiophene) (2) in propylene carbonate solution containing 0.1 M TBAPF₆ as supporting electrolyte. The successive film formation is indicated by an increase in the current density of each cycle. The first scan is depicted in red line with circles and the last scan in blue line with triangles respectively. After electropolymerization the Pt working electrode was fully covered with a continuous dull brownish film as can be seen in the picture in Figure 8.14(b).

The mechanism for the polymerization has been reported to proceed via a radical coupling similar to the case of the polythiophene described before. Also, following the progress of the polymerization in Figure 8.14 one can observe again a shift to lower oxidation potentials upon increasing scan numbers. The cyclic voltammograms were recorded at a scan rate of $50 \,\mathrm{mVs^{-1}}$ inside the glove box using a Pt working electrode (WE), a Pt counter electrode (CE) and a Ag/AgCl quasi reference electrode.

Comparing the electrochemical polymerization of poly (3-hexylthiophene) (8-2) in Fig-

ure 8.14 to the polythiophene (8-1) in Figure 8.13, it can be stated that the conductivity of the film does not appear to be influenced significantly by the presence of the alkyl substituents on the 3-position although one might expect a structural change in the film due to steric interactions which could result in lower conductivities. Generally it has been reported, that for polythiophene (8-1) as well as for poly (3-hexylthiophene) (8-2) conductivities are in the order of 1-100 S cm⁻¹.[128, 131, 132]



(a) Electropolymerization of $(2,2'-bipyridyl)Re(CO)_3Cl$ functionalized poly (3-hexylthiophene)



(b) Picture of the electropolymerized film

Figure 8.15: (a) Potentiodynamic electropolymerization of approx. 0.015 M Re(4-methyl-4'-(7-thienylheptyl)-2,2'-bypyridene(CO)₃Cl to fac-(2,2'-bipyridyl)Re(CO)₃Cl functionalized poly (3hexylthiophene) (8-3) in in BFEE solution. First scan (red line with circles) and last scan (blue line with triangles). The cyclic voltammograms were recorded at a scan rate of 50 mVs⁻¹ outside the glove box using a Pt working electrode (WE), a Pt counter electrode (CE) and a Ag/AgCl quasi reference electrode. (b) Picture of a different, very thick electropolymerized fac-(2,2'-bipyridyl)Re(CO)₃Cl functionalized poly (3-hexylthiophene) (8-3) on a Pt foil supSporting working electrode. [Prepared by G. Aufischer]

Electropolymerization of Re(4-methyl-4'-(7-thienylheptyl)-2,2'-bypyridene(CO)₃Cl to fac-(2,2'-bipyridyl)Re(CO)₃Cl functionalized poly (3-hexylthiophene) (8-3) as the representative compound for the so called 3^{rd} generation type of conducting polymer was difficult in the sence that the substituent fac-(2,2'-bipyridyl)Re(CO)₃Cl groups undergo irreversible oxidation above a potential of 1500 mVvs.NHE compare Figure 5.4 in chapter 5. One possible way to overcome this problem is to use BF₃-diethyl ether (BFEE) which substantially lowers the required potential for electro polymerization.[133]

Figure 8.15 shows the potentiodynamic electropolymerization of approx. 0.015 M Re(4methyl-4'-(7-thienylheptyl)-2,2'-bypyridene(CO)₃Cl to fac-(2,2'-bipyridyl)Re(CO)₃Cl functionalized poly (3-hexylthiophene) (8-3) in in BFEE solution. The successive film formation is indicated by an increase in the current density of each cycle. The first scan is depicted in red line with circles and the last scan in blue line with triangles respectively. After electropolymerization as shown in Figure 8.15(a) the film on the Pt working electrode was barely visible. For illustrative purposes an additional, thick film has been grown in BFEE containing 5 vol.% PPC and otherwise identical conditions for the picture depicted in Figure 8.15(b). For the thick film formation in (b) it can be seen that the Pt working electrode was fully covered with a continuous, almost gold like, shiny film. For further electrochemical characterization and electrochemical CO_2 reduction experiments the film formed in the experiment shown in Figure 8.15(a) was used due to its superior performance.

8.3.2 Cyclic voltammetry studies on electrochemical CO₂ reduction

Once the electroactive polymer electrodes were grown the prepared electrodes could be transfered into a monomer free electrolyte solution for their characterization towards electrochemical CO_2 reduction. Figure 8.16(a) shows the electrochemical characterization of the electropolymerized poly (3-hexylthiophene) (8-2) electrode deposited in the experiment depicted in Figure 8.15 before. The characterization is carried out for negative bias in in nitrogen- (black line with squares) and CO_2 - saturated electrolyte solution (red line with circles), respectively. For the poly (3-hexylthiophene) (8-2) the reduction starts at about -1700 mVvs.Ag/AgCl and is partly reversible with the re-oxidation maximum occurring at about -1800 mVvs.Ag/AgCl.



(b) $fac-(2,2^{2}-bipyridyl)Re(CO)_{3}Cl$ functionalized poly (3-hexylthiophene) (8-3)

Figure 8.16: (a) Cyclic voltammograms of poly (3-hexylthiophene) (8-2) electropolymerized on a Pt plate electrode and in (b) cyclic voltammograms of a thin film of fac-(2,2'-bipyridyl)Re(CO)₃Cl functionalized poly (3-hexylthiophene) (8-3) electrochemically polymerized on Pt plate electrode in nitrogen- (black line with squares) and CO₂- saturated electrolyte solution (red line with circles), respectively. The scan in the presence of CO₂ shows a large current enhancement for the polymer 8-3 due to the catalytic reduction of CO₂. A scan with no catalyst film present under CO₂ (blue dashed line) shows little to no reductive current. Voltammograms were recorded at $50 \,\mathrm{mVs^{-1}}$ in a propylene carbonate solution with a concentration of 0.1 M TBAPF₆ as supporting electrolyte. A Pt working electrode (WE) with and without film, a Pt counter electrode (CE) and a Ag/AgCl quasi reference electrode. [Prepared by G. Aufischer]

It is important to notice, that in presence of CO_2 the magnitude of the reductive current is much lower compared to that of the curve obtained under inert N₂ saturated electrolyte solution with no characteristic features of the poly (3-hexylthiophene) (8-2) present any more. A similar behavior has been observed at our institute for a different class of organic semiconducting materials, namely Quinacridone (QNC). It was found that upon purging with CO₂ the characteristic reduction peak of QNC at -1480 mVvs.Ag/AgCl diminished and the cathodic current decreased substantially showing similar features than represented in Figure 8.16(a). This phenomenon was related to the formation of a QNC-carbonate salt and could be used for efficient and controlled CO₂ capture and release. In the case of QNC it was shown that 20 w% capture (20g CO₂/100g QNC) could be achieved using controlled electrochemical reduce-and-capture. Since controlled capture, storage and release of CO₂ is a key step for both sequestration and utilization approaches of CO₂ this findings about organic semiconducting materials may become particularly interesting in the near future.

Figure 8.16(b) shows cyclic voltammetry measurements of a thin film of fac-(2,2)bipyridyl) $\operatorname{Re}(\operatorname{CO})_3\operatorname{Cl}$ functionalized poly (3-hexylthiophene) (8-3) electrochemically polymerized on Pt plate electrode in nitrogen- (black line with squares) and CO_2 - saturated electrolyte solution (red line with circles), respectively. This measurement constitutes the same thin film as represented in the measurement depicted in Figure 8.15(a). The solutions were purged with N_2 (black curve) or CO_2 (red curves) under stirring for about 15 minutes before cyclic voltammograms were recorded inside the glove box having O₂ and H₂O levels in the ambient atmosphere below 10 ppm. The measurement of the potential window with two Pt electrodes as WE and CE, respectively, and an electrolyte solution under N_2 does not show any reductive current in the potential range from 0 to $-2000 \,\mathrm{mVvs.Ag/AgCl}$. When the solution is purged with CO_2 and no polymerized catalyst film is present, a minor reductive current starts to flow at a potential lower than about $-1800 \,\mathrm{mVvs.Ag/AgCl}$ (blue dashed line). When the Pt working electrode is replaced by the thin film of fac-(2,2)bipyridyl) $Re(CO)_3Cl$ functionalized poly (3-hexylthiophene) (8-3) however, and measured in the electrolyte solution under N_2 atmosphere, the typical reduction curve of the polymer (8-3) is measured showing low current densities upon a bias to $-2000 \,\mathrm{mVvs.Ag/AgCl}$ with current densities of about $-0.25 \,\mathrm{mAcm^{-2}}$. If however the electrolyte solution is at CO₂ saturation, a high, non-reversible reductive current enhancement is observed (Figure 8.16(b), red line with circles). The reductive current begins to increase at about $-1550 \,\mathrm{mVvs.Ag/AgCl}$ reaching current densities of about $-2 \,\mathrm{mAcm^{-2}}$ at potentials of $-2000 \,\mathrm{mVvs.Ag/AgCl}$. Although a direct proof of reduction products is still missing, the current enhancement can be understood by a catalytic reduction of CO_2 to CO by the functionalized (2,2'-bipyridyl)Re(CO)₃Cl catalyst on the alkyl substituents of the polythiophene. It is also interesting to mention that the voltammogram under CO_2 saturation shows peak crossing which is an inherent characteristic of the homogenous (2,2)-bipyridyl)Re(CO)₃Cl catalyst as discussed before, compare Figure 5.6 and 5.7 in chapter 5 of this thesis.

Concluding this work it was shown for the first time the possible application of a functionalized poly (3-hexylthiophenes) with fac-(2,2'-bipyridyl)Re(CO)₃Cl, as a so called third generation of conducting polymer, for its application of electrochemical CO₂ reduction. Upon CO₂ saturation the cyclic voltammograms showed a strong current enhancement which is a good evidence for a catalytic reduction of CO₂ to CO by the functionalized (2,2'-bipyridyl)Re(CO)₃Cl catalyst. Beside its apparent application for CO₂ reduction, simple poly (3-hexylthiophene) might have interesting properties for controlled CO₂ capture and release and will be investigated further.

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Chapter 9

Summary and future studies

In this work the photoinduced electron transfer from organic semiconductors onto redox mediator catalysts for CO_2 reduction has been investigated, starting with the identification, characterization and test of suitable catalyst materials. Once the catalyst redox mediators were found the next step was the immobilization of the catalyst on the electrode and thereby changing from homogeneous to heterogeneous catalysis. Finally, the combination of catalysts with organic semiconductor materials was investigated for energy and charge transfer from the donor polymer to the catalyst acceptor towards its possible applications in photocatlytic CO_2 reduction.

9.1 What has been accomplished

After the introduction chapter, where the scope and motivation of this work were defined, the thesis starts with an exhaustive experimental description in chapter 2,

"Experimental techniques", describing in detail the methods used for the experimental results obtained herein. The following chapter 3, "Photophysical results", studies in great depth the photophysical properties of the catalyst materials further investigated for CO_2 reduction within the thesis.

In the subsequent chapter 4 of this work, "Quantum chemical calculations", quantum chemical calculations were successfully used for the interpretation of experimental obtained data, such as infrared absorption spectra, and for the calculation of molecular orbital energy levels. Infrared spectroscopy allowed analytical characterization of molecular substances. However, since the vibrational degrees of freedom for non linear molecules scales with 3N-6, with N being the number of atoms in the molecule, infrared spectra are complicated for larger molecules making the spectra difficult to interpret. For this reason calculated IR absorption spectra by quantum mechanical DFT calculations were successfully used to correlate characteristic features in the measured spectra to their molecular origin. Experimentally observed data and quantum chemical predictions for the IR spectra of the novel compound

are in good agreement. For the prediction of measured infrared spectra it was sometimes necessary to scale the obtained calculated data by a constant factor to achieve good matching of calculated and measured spectra. Additionally quantum mechanical calculations were carried out for the determination of molecular orbital frontier energy levels. Calculations gave typically a lager band gap than band gaps estimated by UV-Vis absorption or cyclic voltammetry measurements with offsets of about 0.2 eV. It should be notice that quantum mechanical calculations are based on many approximations giving only an estimate of the real molecular properties.

In the following chapter 5 the materials investigated for homogeneous electro catalysis were Rhenium difference complexes with different ligand systems as well as the Pyridinium catalyst. In the three sections "*Rhenium compounds with bipyridine ligands*", "*Rhenium compounds with bian ligands*" and "*Pyridinium as catalyst*" the properties of these materials as homogeneous electro catalysts for CO_2 reduction were investigated. Figure 9.1 shows a summary of the materials investigated within this work and the obtained faraday and energy efficiencies for electrocatalytic CO_2 reduction and the quantum yield for photocatalytic CO_2 reduction.



Figure 9.1: Summary of the materials investigated within this work and the obtained efficiencies. Faraday efficiency $\eta_{Faraday}$, energy efficiency η_{Energy} and quantum yield Φ_{CO} for CO₂ reduction.

Several tricarbonylchlororhenium(I)pyridyl complexes (1-1 to 1-4) were studied regarding to their potential as catalysts for homogeneous electrochemical and photochemical reduction of CO_2 to CO. It was found that the CO_2 reduction potential, determined by cyclic voltammetry, can be positively influenced by a modified ligand system. A comparison between the catalyst material 1-3 with added phenylethynyl groups at the 5,5' position to the non-modified catalyst 1-1 showed a shift in the onset CO_2 reduction potential by about 300 mV (vs. NHE) to more positive values. Bulk CO_2 electrolysis experiments showed Faraday efficiencies around 45 to 50 % for the formation of CO. The best estimated rate constants

9.1. WHAT HAS BEEN ACCOMPLISHED

according to cyclic voltammetry data are in the order of $220 \,\mathrm{M^{-1}s^{-1}}$ for compound 1-3.

The electrocatalytic properties of rhenium(I) tricarbonyl complexes carrying bis(arylimino)acenaphthene (BIAN) ligands for the selective two-electron reduction of CO_2 to CO in homogeneous solution have been successfully tested and characterized. It could be demonstrated that a variation of the ligand substitution pattern in close proximity to the metal center has a very significant influence on the catalytic performance of these systems. Further studies on the suitability of this deeply colored and readily tunable class of compounds as functional components of photocatalytic CO_2 -reduction cycles are currently underway.

As a next step new and improved electro- and photocatalysts for CO_2 reduction have to be developed and characterized. The modification of the attached ligand system is a suitable way for systematic tuning of the excited state properties of such materials and hence their electro- and photocatalytic abilities. A clear demonstration of this was shown by the comparison of compound 1-1 and 1-3. Following this idea a modification where the phenylethynyl groups are attached to the 4,4' position might be highly interesting, assuming a better conjugation to the metal center of the complex. Although further catalyst improvements are crucial, finally, the two systems capable of catalytic CO_2 reduction and H_2O splitting could be combined in a photo- or photoelectrochemical cell. Such a system would be capable of solar powered production of syngas and its equivalents (CO and H_2 or NADH).

One more example of homogeneous catalysis investigated in chapter 5 was the pyridiniumcatalyzed reduction of CO_2 to methanol. Cyclic voltammetry experiments were used to proof the important role of platinum in the overall reaction mechanism. Additionally controlled potential electrolysis were carried out over a extended period of 30 hrs leading to the formation of methanol via the pyridinium-catalyzed reduction of CO_2 .

Additionally, some of these materials proofed to be efficient photo catalysts for the reduction of CO_2 producing mainly CO with the aid of a sacrificial electron donor as for example triethanolamine (TEOA). For photo-catalysis, it is important to extend the absorption of the catalyst compounds in the visible region. In this work new catalysts 1-3 and 1-5 were synthesized which show significantly higher absorption in the visible range, compare chapter 6. It was assumed to be a clear benefit for photocatalytic application, however, it was shown that the experiments over several hours of irradiation yielded only very low CO formation. Under identical conditions, the unmodified compound 1-1 still performs better for photocatalytic CO_2 reduction. To the best of our understanding, following quantum mechanical DFT calculations, this different behaviour might be attributed to an inversion of the lowest-lying excited state properties of the new compound compared to the situation in compound 1-1, which is crucial for the photochemical reactivity of such systems.

In chapter 7, "Heterogeneous electro catalysis", several ways to change from homogeneous to heterogeneous catalysis for CO_2 -reduction were studied. As one of the first trials, the rhenium catalyst 1-2, with dicaboxylic side groups at the ligand system, was used to attach to a binding metal oxide layer. Although in this experiments the anchoring to the oxide layer was successfully achieved, it tourned out that the film was not stable upon electrochemical reduction. The cyclic voltammetry experients showed, that below a potential of about $-1000\,\mathrm{mVvs}$. NHE the layer was irreversibly destroyed and rinsed of the electrode as a black precipitate.

The electropolymerization of the active catalyst compound 1-3 onto a Pt working electrode is investigated. The electropolymerization to the electrode surface and its potential for heterogeneous catalysis towards CO_2 reduction was successfully studied. The film growth on a Pt working electrode was performed by potentiodynamic reductive scanning in nitrogen saturated acetonitrile solution. The films were electrochemically characterized using cyclic voltammetry. The catalytic properties for CO_2 reduction were studied via cyclic voltammetry in carbon dioxide saturated acetonitrile solution. It was found that the electropolymerisation of the monomer 1-3 appears to be a promising way to change from homogeneous to heterogeneous catalysis for CO_2 -reduction, reducing the amount of required catalyst material needed and overcoming the limitations regarding solubility of homogeneous catalysts in general. The novel catalyst film furthermore demonstrates high selectivity for the CO_2 -reduction to CO at relatively low reduction potentials and high current densities. Figure 9.2 shows the schematic representation of the differences between a homogeneous and a heterogeneous process for catalytic CO_2 reduction



Figure 9.2: Schematic representation of the differences between a homogeneous and a heterogeneous process for catalytic CO_2 reduction

Finally, following a different approach, the catalyst material $(2,2'-bipyridyl)Re(CO)_3Cl$ (1-1) was immobilized into a polypyrrole matrix by electrochemical polymerization of pyrrole in a homogeneous mixture of pyrrole and the catalyst material. Pyrrole was electropolymerized on a Pt foil serving as supporting working electrode for the polypyrrole film. First experiments using cyclic voltammetry looked promising, however no product gas analysis was performed to independently verify the CO₂ reduction and confirm the expected CO formation. Subsequent experiments failed in reproducing this data and further studies on this effect are under current investigations.

9.1. WHAT HAS BEEN ACCOMPLISHED

In the last chapter 8, "Organic semiconductors for CO_2 reduction", the combination of catalysts with organic semiconductor materials were investigated. In the first part poly(3hexylthiophene) (P3HT) was used as the organic semiconducting polymer which served as donor material and Pyridinium as a homogeneous electrocatalyst in solution as acceptor. In the photoresponse of a P3HT covered ITO electrode at constant potential upon white light irradiation and a varying pyridinium concentration it was found, that when the catalyst concentration is increased, the corresponding current photo-response is enhanced. This is expected when pyridinium acts as an efficient acceptor molecule. Bulk electrolysis experiments were performed, however no products in form of methanol could be detected. This can be explained since the lifetime of this type of electrodes is rather low and the photocurrent is in the μ A regime. In the case with the P3HT electrodes the electrodes corroded within 2 to 3 hrs of electrolysis time. As a resulting conclusion, this system has to be improved significantly in terms of electrode stability and current densities which is subject to ongoing research.

In a different approach, poly(N-vinylcarbazole) (PVK) was used as absorber material acting as efficient redox photosensitizer in combination with fac- $(2,2'-bipyridyl)Re(CO)_3Cl$ (1-1) as catalyst acceptor. The energy levels of the donor polymer and acceptor catalyst are aligned in a favorable situation for photo-excited charge and/or energy transfer. Subsequent photoluminescence (PL) quenching and light induced ESR experiments were carried out to study this system in bulk, solid phase mixtures of donor and acceptor, and at a donor-acceptor solid-liquid interface. PL quenching experiments with PVK as donor polymer in solid film mixtures and in a solid-liquid interface between polymer and catalyst revealed strong quenching due to a Förster- and/or Dexter type of energy transfer from PVK to $(2,2' bipy)Re(CO)_3Cl$ (1-1) with only a minor contribution of charge transfer involved. This findings might leading to possible applications in photocatlytic CO₂ reduction.

The last part of this thesis investigated a method to functionalize poly (3-hexylthiophenes) (P3HT) with fac-(2,2'-bipyridyl)Re(CO)₃Cl (1-1) for its potential application of electroand photochemical CO₂ reduction. The monomer was deposited by electro-polymerization onto the electrode and used to determine its potential for heterogeneous catalysis towards CO₂ reduction. This interesting approach lead to the formation of a conducting polymer with functionalised rhenium bipyridine catalysts attached to the polymer backbone via alkyl bridges. It was shown for the first time the possible application of a functionalized poly (3hexylthiophenes) with fac-(2,2'-bipyridyl)Re(CO)₃Cl, as a so called third generation of conducting polymer, for its application of electrochemical CO₂ reduction. Upon CO₂ saturation the cyclic voltammograms showed a strong current enhancement which is a good evidence for a catalytic reduction of CO₂ to CO by the functionalized (2,2'-bipyridyl)Re(CO)₃Cl catalyst. Beside its apparent application for CO₂ reduction, simple poly (3-hexylthiophene) might have interesting properties for controlled CO₂ capture and release, which will be investigated further.

9.2 The need of novel catalysts

The fac-(2,2'-bipyridyl)Re(CO)₃Cl (1-1) is up to now one of the most efficient catalysts for the reduction of CO₂ with reported quantum yields (Φ_{CO}) for photocatalytic CO₂ reduction of 0.14. Subsequent modifications of the bipyridine ligand system of 1-1 lead to the development of superior catalysts with Φ_{CO} up to 0.59, making these type of materials the most efficient CO₂ photo-catalyst among known homogeneous catalyst materials by now.[46, 98] One substantial drawback of this type of materials is based on the central metal atom rhenium being extremely rare and hence expensive. Rhenium is with an abundance of 0.7 ppb in the earth's crust[134] one of the rarest materials available resulting in a rhenium metal pellet price of 4630 \$ per kilogram. [135]

Taking this into account, one of the major challenges for basic research is to find catalysts based on earth-abundant materials that have low over potentials for CO_2 reduction, water oxidation and a high turnover frequency (equivalten to the rate constants k). One very interesting approach has resently been published by Kubiak and others where rhenium was successfully substituted by manganese in the CO_2 reduction catalysts Mn(bpy-tBu)(CO)₃Br and Mn(bpy-tBu)(CO)₃(MeCN)(OTf).[136, 137] It is expected that this achievements will have substantial impact on the scientific field working on CO_2 reduction.

Another very interesting approach was presented by Bocarsly and his group as they've reported the reduction of carbon dioxide to methanol and formic acid on a platinum electrode in aqueous solutions containing pyridinium as active catalyst material.[30] Following ongoing scientific reports over the last two years, the proposed mechanism and the role of pyridinium as the catalyst material lead to a controversial discussion in the field,[95] the reported data is nonetheless impressive and deserves great attention by the scientific community.

It has been stated in the beginning of the introduction chapter 1 of the thesis that converting sunlight into synthetic chemical fuels by the direct reduction of CO_2 is probably the most elegant and sustainable way to overcome demanding problems related with the current energy supply of humanity. How important the role of high turnover frequencies in catalyst materials is, becomes apparent when we consider practical applications and look at photovoltaic current densities vs. turnover frequencies (TOF) of CO_2 reduction catalysts to date. The best photovoltaic materials can support current densities of 10 to 20 mA cm⁻² (or 100 to 200 A m⁻²). In contrast, for a two electron process, a monolayer of catalyst with a TOF of 1000 s⁻¹, will support a current density of only 0.1 mA cm⁻².

Figure 9.3 relates current densities to equivalent turnover frequencies of a monolayer of catalyst material. Given current technology in photovoltaic cells, typical photovoltaic current densities are in the order of 100 A m⁻². As indicated by the red circle in Figure 9.3, a monolayer of catalyst would need to achieve a TOF of about 100 000 s⁻¹ to support the corresponding current density. The best catalyst materials known by now have about 500 - 1000 s⁻¹.

Obtaining high photocurrent densities inalienably requires the use of molecular catalyst



Figure 9.3: Relation between current densities vs. turnover frequencies of a monolayer of catalyst material for the two electron reduction of CO_2 to CO.

with high TOFs. In theory one could push the system also by increasing the molecular catalyst concentration, however, higher catalyst concentrations in solution will lead to an increase in light absorption by the solution and the solubility of the catalyst is limited in any given solvent. Taking this into account, there is an apparent need to advance catalyst materials by identifying the rate limiting intermediate steps in CO_2 reduction and improve them.

9.3 A more elaborate view on CO_2 reduction to date

In this thesis the main focus was on the CO_2 reduction by the use of catalyst materials concentrating on the cathode reaction in the electrochemical setup only. Especially cyclic voltammetry experiments using a three electrode system were used in great depth to investigate the properties of various materials for CO_2 reduction. However, one must not forget that by using a three electrode setup only the potential drop on the working electrode is measured, which is one of the important parameters for determining the effectiveness of a catalyst material but not of the total cell. The question that remains is, how this potential is related to a fully working device capable of CO_2 reduction, a prototype electrolyser so to speak, being a device similar to the one depicted in the introduction chapter 1, compare scheme 1.4? In a real CO_2 electrolyser, if everything is hooked together, several potential losses have to be accounted for. Let's assume a CO_2 reduction following the reactions 9.1 on the cathode and 9.2 on the anode with CO and O_2 as main products.

$$CO_2 + 2H^+ + 2e^- \rightleftharpoons CO + H_2O \tag{9.1}$$

$$H_2 O \rightleftharpoons \frac{1}{2}O_2 + 2H^+ + 2e^- \tag{9.2}$$

There is the well-studied potential for CO_2 reduction on the cathode electrode E_C , the potential E_A , that has to be applied on the anode counter electrode for the O_2 evolution reaction, the potential drop due to ohmic losses in the electrolyte solution E_O and the junction potential E_J over the membrane separating anode and cathode compartment. Taking all this potential drops into account, the total voltage which has to be applied, E_{total} , can be calculated by the following equation 9.3.

$$E_{total} = E_C + E_A + E_O + E_J \tag{9.3}$$

The potential necessary for CO_2 reduction, E_C , is about -1.65 V vs. NHE taking the potential for the 2^{nd} reduction wave of the catalyst material $(2,2'-bipyridyl)Re(CO)_3Cl$ (1-1) as the standard catalyst and benchmark compound deeply investigated in this thesis, compare chapter 5.

For the oxygen evolution to occur, several catalyst materials have been reported in literature. One of the most promising and applicable is a cobalt–phosphate type of catalyst where the O₂ evolution is reported to occur at approximately +1.3 V vs NHE (E_A) in an aqueous phosphate buffer solution at pH 7. [138, 139]

The ohmic potential drop in the cell E_O depends mainly on the conductivity of the electrolyte solution used, the area of the electrodes and the distance between working and counter electrode. For a 0.1 M KCl solution in water the electrolyte conductivity is about 12.8 mS cm⁻¹ at 25°C.[140] A typical distance between working and counter electrode is 2 cm with current densities of 2 mA cm⁻². Taking these values for an electrode of 10 cm² one obtains an ohmic potential drop in the cell E_O of about 312.5 mV.

The specific conductivity of a cation exchange membrane of 0.56 mm thickness used to separate anode and cathode compartment is about 9.3 mS cm^{-1} in a 0.1 M NaCl solution, resulting in a membrane potential drop E_J that is in the order of 50 mV for a current density of 2 mA cm⁻² and hence almost negligible for low current densities.[141, 142, 143]

Scheme 9.4 depicts the apparent voltage necessary for a CO₂ electrolyser system with a E_C of -1.65 V for the CO₂ reduciton, E_A of 1.3 V for the oxygen evolution, E_O of 312.5 mV for the ohmic losses in the electrolyte and E_J of 50 mV for the membrane potential. The total voltage that needs to be applied given by equation 9.3 for the actual system sums up to 3.27 V. One has however to take into account that the reduction potential E_{red} for the CO₂ reduction following reaction 9.1 with CO and O₂ as main reduction products is E_{red} -0.53 V and for the reaction 9.2 is E_{ox} 0.82 V (at pH 7 and 25 °C).

The sum of both potentials results in a thermodynamically necessary electromotive force emf of 1.35 V for the formation of CO and O₂. Since the necessary applied voltage in our



Figure 9.4: Schematic representation of the characteristic potentials necessary for a CO_2 electrolyser system consisting of two electrodes with a membrane to separated anode and cathode compartment.

system is 3.27 V, the device efficiency can then be calculated by 1.35 V divided by 3.27 V giving an efficiency of about 41 %, assuming a Faraday efficiency of 100 %.

In the electrochemical CO_2 reduction process pure CO_2 is used. Capturing CO_2 from the air is particularly important since the atmospheric concentrations are relatively low with about 400 ppm or 0.04 % by the end of 2013.[3] If we assume a perfect mechanism for capturing of CO_2 , only the free energy of mixing has to be provided, which can be calculated by knowing the partial pressure difference upon concentration according to equation 9.4.[144]

$$\Delta G^{\circ} = R \cdot T \cdot \frac{P}{P^{\circ}} \tag{9.4}$$

Where P° is 1 bar atmospheric pressure, P is the partial pressure of CO₂ with $4 \cdot 10^{-4}$ bar, and T is the temperature taken at 300 K, which gives $-19.51 \text{ kJ mol}^{-1}$. One must not forget that this is for a perfect absorber, in reality however, the energy needed is expected to be substantially higher.

The theoretical energy that can be gained back by burning CO and O_2 again according to reaction 9.5

$$CO + \frac{1}{2}O_2 \rightleftharpoons CO_2$$
 (9.5)

has a change in the standard Gibbs energy of reaction ΔG of $-257 \,\mathrm{kJ} \,\mathrm{mol}^{-1}$. The Gibbs

energy of reaction is also related to the electromotive force according to equation 9.6.

$$\Delta G = -n \cdot F \cdot E \tag{9.6}$$

Taking now the total voltage applied in the CO_2 electrolysis system of 3.27 V, the change in Gibbs energy of reaction according to equation 9.6 is -631 kJ mol^{-1} , which has to be applied to the system for the CO_2 reduction reaction to occur, plus the free energy of mixing for concentrating the CO_2 in the system with minimal about $-19.51 \text{ kJ mol}^{-1}$, so in total about -651 kJ mol^{-1} . Based on these assumptions the overall CO_2 reduction to energy return efficiency would be -257 kJ mol^{-1} devided by -651 kJ mol^{-1} , or about 38 %. Gasoline has a specific volumetric energy density of about 35 MJ/l (9.7 kWh/l).[7] Taking the calculated efficiency value of 38 % and a price for electric energy with 7.5 cent/kWh, the production of an energy equivalent of 1 l gasoline by CO_2 reduction to CO would cost about 1.9 Euro and would remove $3.4 \text{ m}^3 \text{ CO}_2$ from the atmosphere, while the price for gasoline at a local gas station in Austria was about 1.4 Euro/l by the time this sentence was written.

Of course, these rough and quick calculations are by no means exhaustive and only schematic at best, but they might still give a glimpse that electro- and photochemical CO_2 reduction for artificial fuel synthesis might become at some point more to society than an interesting academic field of research only. I would like to finish this work with quoting the Nobel Laureate Wilhelm Ostwald (1853 - 1932), who was one of the first scientists that was deeply aware of the importance of energy storage and conversion and predicted many forthcoming developments [145]:

"When we ask for the general function of science, just as we do in the case of art, the answer is very straight forward: it consists of prophecies. All the manifold work driven by the sciences has the final goal to give us the potential to foresee future occurrences". [146]

Chapter 10

Appendix

List of abbreviations

AC = alternating current ACN = acetonitrile AFM = atomic force microscopy ATR = attenuated total reflectance a.u. = arbitrary unit BCB = benzocyclobutene BLZ = blazing angle CMS = charge modulation spectroscopy DCM = dichloromethane DFT = density functional theory DMF = dimethylformamid DTGS = triglycine sulfate FTIR = fourier transform infrared spectroscopyGC = gas chromatography

- HF = Hartree-FockIC = ion chromatographyIL = intra ligandITO = indium tin oxide $MCT = mercury \ cadmium \ telluride$ MeOH = methanolMIR = mid infraredMLCT = metal-to-ligand charge transferMO = molecular orbitalNADH = nicotinamide-adenine-dinucleotide NIR = near infraredNHE = normal hydrogen electrodeOER = one-electron-reducedP3HT = poly(3-hexylthiophen)PL = photoluminescence
- PVK = polyvinylcarbazol
- QRE = quasi reference electrode
- RMS = rout mean square
- SEM = scanning electron microscopy
- TEOA = triethanolamine
- TON = turn over number
- $TBAPF_6 = tetrabutylammonium hexafluorophosphate$
- UV = ultra violet

Vis = visible

WE = working electrode

ZnSe = zinc selenid

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Eidesstattliche Erklärung

Ich erkläre an Eides statt, dass ich die vorliegende Dissertation selbstständig und ohne fremde Hilfe verfasst, andere als die angegebenen Quellen und Hilfsmittel nicht benutzt bzw. die wörtlich oder sinngemäß entnommenen Stellen als solche kenntlich gemacht habe. Die vorliegende Dissertation ist mit dem elektronisch übermittelten Textdokument identisch.

Linz, am 24. Februar 2014

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